



# Solute transport in periodical heterogeneous porous media: Importance of observation scale and experimental sampling



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## SUMMARY

This paper focuses on the effects of the observation scale and sampling on the dispersion of tracers in periodical heterogeneous porous media. A Model Heterogeneous Porous Medium (MHPM) with a high degree of heterogeneity was built. It consists of a preferential flow path surrounded by glass beads. 44 tracer experiments were carried out on several series of periodic MHPM to investigate the effect of the observation scale on solute dispersion. Each series was replicated several times, allowing for a statistical description of the unit transfer function of the MHPM. No significant trend was found for the dispersion coefficient as a function of the size of the MHPM. However, given the variability of the breakthrough curves from one experiment replicate to another, under-sampling might easily lead to conclude that the dispersion coefficient is variable with distance. Depending on the samples used, it would be as easy to (wrongly) detect an increasing trend as to detect a decreasing one. A confidence interval analysis of the experimental breakthrough curves in the Laplace space shows that (i) there exists a model with scale independent parameters that can describe the experimental breakthrough curves within the limits of experimental uncertainty, (ii) this model is not the advection–dispersion (AD) model, (iii) the modelling error of the AD model decreases with the number of periods, (iv) the size of the Reference Elementary Volume for the dispersion coefficient is between 10 and 20 periods. The effects of sampling prove to override those of scaling. This, with the invalidity of the AD model, leads to question attempts to calibrate and/or identify trends in the dispersion coefficient at intermediate scales from a limited number of experiment replicates.

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## 1. Introduction

Understanding solute transport in porous media is important to predict the fate of contaminants in natural soils. Natural soils are highly heterogeneous and implicate various transport mechanisms. Tracer experiments on laboratory soil columns made a big contribution to identify these mechanisms. The most widespread transport model for inert solute is the advection–dispersion (AD) model. Fitting this model against real-world tracer tests has been reported to induce an increase in the dispersion coefficient with the travelled distance (see e.g. Dagan, 1989; Gelhar et al., 1992; Zhou and Selim, 2003). The variability of the dispersion coefficient with distance has motivated a strong interest for alternative models. Recently, laboratory tracer experiments have been used as a benchmarking basis to test the respective accuracy of a variety of

normal and anomalous transport models (see e.g. the review in Gao et al., 2009). It has also been suggested by some authors that the dispersion coefficient in Mobile–Immobile models should be made exponentially dependent on distance in order to accurately reproduce experimental breakthrough curves in laboratory column experiments (Gao et al., 2010).

A number of laboratory tracer experiments in porous media are available from the literature (Silliman et al., 1998). Laboratory experiments on heterogeneous porous media are very few in comparison to those done on homogeneous porous media. One cause might be the practical difficulty to conceive and construct heterogeneous porous media.

Silliman and Simpson (1987) used fine sand inclusions (small cubes) with coarse sand surrounding. They found a change in the shape of the breakthrough curve at each of five measurement sections, and inferred a continuous increase in dispersivity with distance. Saiers et al. (1994) used a coarse sand inclusion (tubule) with finer sand surrounding. The inclusion constituted a

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preferential flow path and contributed to more than 60% of the mass balance. The breakthrough curves exhibited multiple inflection points that cannot be accounted for by the classical advection dispersion (AD) model. In comparison to other studies, the work of [Saier et al. \(1994\)](#) is distinguished by the high degree of heterogeneity of the porous media. This fact is reflected in the shape of the breakthrough curves. Much more than a mere tailing effect, the breakthrough curves exhibited a clear two-step shape. [Li et al. \(1994\)](#) used coarse inclusions (polyethylene porous cylinders) with finer sand surrounding. The resulting breakthrough curves exhibited asymmetry. [Huang et al. \(1995\)](#) used a 12.5 m long column with a wide range of soil materials. Their breakthrough curves exhibited irregular and nonsigmoidal distributions and were in most cases poorly described by the AD model.

[Sternberg et al. \(1996\)](#), [Irwin et al. \(1996\)](#) were the first to use a periodical heterogeneous porous media, where the heterogeneity consisted of a succession of several glass bead sets tested in several serial orders. The breakthrough curves were used to infer the variation of the dispersion coefficient with distance. Unfortunately, the breakthrough curves are not shown in the publications and no estimate is provided for the goodness-of-fit of the AD model. It is thus impossible to determine whether fitting the coefficients of the AD model was meaningful. However, both studies present the results of dispersion estimations. [Sternberg et al. \(1996\)](#) found that dispersion does not necessarily increase with scale, but that it can increase and decrease depending on the particular arrangement of properties in the medium. They deduced that the system length was unimportant in observing the scale effect. Conversely, in the study of [Irwin et al. \(1996\)](#), dispersion appeared to be scale dependent up to a certain travel distance. But, quoting the authors' own words, "because of the scatter in the data, it could be argued that the apparent increase in longitudinal dispersion is simply a result of the variation in the data". This raises the issue of sampling effects.

[Greiner et al. \(1997\)](#) used aggregates of lower permeability in a surrounding of higher permeability. [Niehren and Kinzelbach \(1998\)](#) used cylindrical cellpore filters (less permeable) in a quartz-sand surrounding (more permeable). [Tran Ngoc et al. \(2011\)](#) used spherical clay inclusions (micro porosity) surrounded by sand (macro porosity). [Danquigny et al. \(2004\)](#) performed tracer tests on two kinds of heterogeneous porous material: a channel structured medium ( $5.6 \text{ m} \times 1 \text{ m} \times 1 \text{ m}$ ), with channels crossing the whole tank, and a statistically correlated random structure. They found that the breakthrough curves of the statistically correlated random structure could be fitted with the AD model (at least for long distances), but that the fit is quite poor for channel structured medium due to the non-Gaussian distribution of the concentration.

[Zin et al. \(2004\)](#) designed an artificial porous medium with several conductivity contrasts, using low conductivity inclusions (small beads) surrounded by a high conductivity matrix (large beads). They found that the breakthrough curves of the low-contrast medium showed no tailing, while those of high-contrast medium showed tailing. [Golfier et al. \(2011\)](#) used fine sand inclusions (lenses) with coarse sand surrounding. Their breakthrough curves showed asymmetry. The low degree of heterogeneity in the studies of [Sternberg et al. \(1996\)](#), [Irwin et al. \(1996\)](#) might have led to some contradictory conclusions concerning the dispersion scale dependence. As to the study of [Saier et al. \(1994\)](#), the authors were not mainly interested in the problematic of dispersion scale dependence, but rather in colloidal mobilization and transport in a structured porous media.

In the light of the abovementioned studies, it appears that studying the effect of heterogeneity on solute transport requires two conditions: (i) a high degree of heterogeneity of the porous media (as the experimental model of [Saier et al. \(1994\)](#)), and (ii) a periodical heterogeneous porous media (as the experimental protocol of [Sternberg et al. \(1996\)](#), [Irwin et al. \(1996\)](#)). The first

condition guarantees that the effects of material heterogeneity are clearly visible, while the second allows the influence of scale effects to be assessed. This also allows for a better quality of the experimental data, with easily replicable experiments yielding reliable statistics.

In this study, we conceived a Model Heterogeneous Porous Medium (MHPM) with a high degree of heterogeneity. The purpose is to (i) enrich the experimental database of laboratory tracer tests with high quality data, (ii) answer the following six questions.

- (Q1) Can a scaling trend be observed for the dispersion coefficient in this highly heterogeneous MHPM?
- (Q2) If this is not the case, can the variations of the dispersion with the observation scale be attributed to experimental artefacts such as sampling effects?
- (Q3) Does there exist a model with uniform coefficients (thus scale-independent) to describe adequately the present MHPM response?
- (Q4) Can the AD model be considered valid at the scale of this MHPM?
- (Q5) If it cannot, does a scale exist above which the AD model can be deemed a satisfactory approximation of the experimental response of the MHPM?
- (Q6) Can more advanced models such as the Mobile–Immobile (MI) or Continuous Time Random Walk (CTRW) models be considered as better candidates than the AD model to simulate small-distance and short-time MHPM behaviour?

The detailed characteristics of the experimental setup is described in Section 2 of the paper. The results of experimental breakthrough curves are shown in Section 3. Such experiments are usually termed Intermediate Scale Experiments (ISE) in that they involve a scale larger than the typical size of the heterogeneity but they do not achieve the size of the Reference Elementary Volume (REV) above which the continuous medium formalism should be expected to be valid ([Bear, 1972](#)).

Section 3 is also devoted to an analysis of the transfer function of the MHPM. Section 4 is devoted to discussion. A point-by-point answer to the six questions above is given throughout Section 3 and 4.

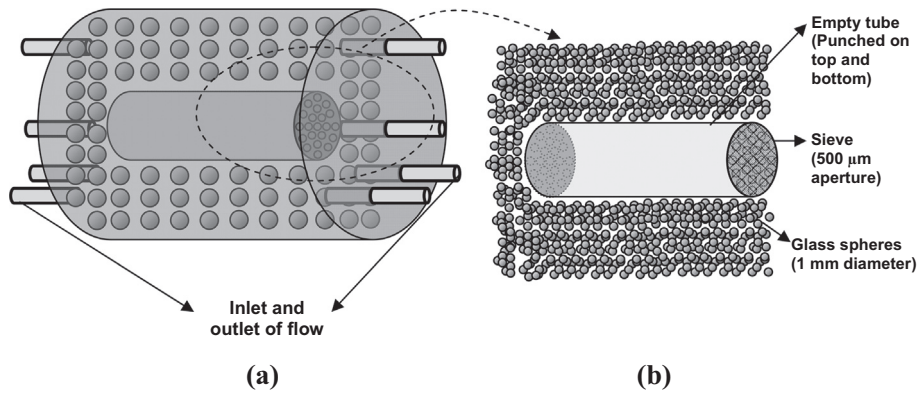
## 2. Materials and methods

### 2.1. Model heterogeneous porous media

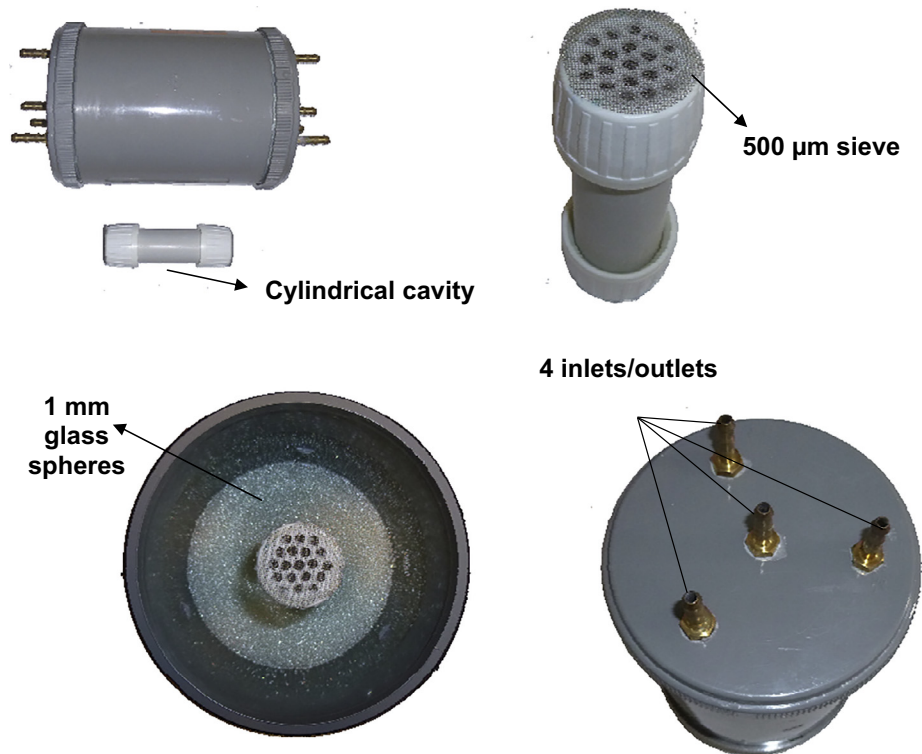
The MHPM consists of a set of PVC columns (10 cm in diameter, 15 cm in length each) containing 1 mm glass spheres (40% porosity) surrounding a cylindrical cavity (2.5 cm in diameter, 10 cm in length) placed in the centre of the column ([Fig. 1](#)). The cylindrical cavity has 100% porosity and thus acts as a wide pore that induces preferential water and solute transfer. The pore volume  $V_0$  of one MHPM period is about 461 ml.

The water and solute flow enters and leaves the column by 4 inlets and outlets (4 mm in diameter). A 500  $\mu\text{m}$  sieve prevents the glass spheres from clogging the inlets and outlets, possibly blocking the flow. [Fig. 2](#) shows real captures of the MHPM. The incoming discharge (imposed by a peristaltic pump) is equally distributed between the 4 inlets. It is expected that the flow of the central inlet will mainly transfer through the central cavity, while the flow of the three remaining inlets will mainly transfer through the surrounding glass beads.

After carrying out the series of experiments, four randomly chosen columns were disassembled. In each of them, the position of the sieve was compared to what it was before the experiment. No detectable displacement was noted.



**Fig. 1.** (a) A model heterogeneous porous media (MHPM) with 4 inlets and outlets that occupy the centre of gravity and the 3 vertices of an equilateral triangle. The centre of gravity is on the central axis of the column and the 3 vertices are 1 cm away from the column periphery. (b) The internal cavity is a tube that is punched on top and bottom and covered with a 500 µm sieve. The sieve impedes the glass spheres from entering inside the cavity and guaranties that only water (and solute) can transfer through the cavity.



**Fig. 2.** Real captures of a MHPM.

## 2.2. Experimental setup

Step tracing experiments are done by injecting salty water (deionised water supplemented with NaCl at  $C_0 = 0.1 \text{ Mol/l}$ ) in a study column initially containing deionised water. A flow of  $7.5 \text{ l h}^{-1}$  salty water is induced into the study column until the outlet concentration  $C$  stabilizes to  $C_0$ . In these experiments, the stable  $C_0$  level was generally reached after injecting three times the pore volume  $V_0$  of the study column. The outlet concentration is measured using a conductimeter (WTW TetraCon 325) and saved on a data logger (Campbell CR1000) every 5 s. The cumulated outlet volume  $V$  is measured by weighing the effluent every 5 s and saved on the data logger (Fig. 3).

The study column consists of a series of  $N$  connected MHPM. In this study, four series were investigated with  $N = 3, 5, 10$  and 15.

The series with  $N = 3$  corresponds to the smallest scale of periodical heterogeneity because the first MHPM has a divergent flow inlet and a parallel flow outlet while the last MHPM has a parallel flow inlet and a convergent flow outlet. Only the in-between MHPM have the same parallel flow inlets and outlets (Fig. 3). Therefore,  $N = 3, 5, 10$ , and 15 correspond to 1, 3, 8, and 13 periodical heterogeneities.

In this study, 15 MHPM columns were built, named A, B, C, ..., N, O. For each series, four replicates of the step tracing experiment were conducted for four 90° rotations of the study column, from which a mean breakthrough curve was deduced. The purpose of the 90° rotation is to eliminate biases resulting from a possible interaction between density-driven effects and the 120° spacing between the column inlets and outlets. The various column combinations used for the various experiments are summarized in Table 1.

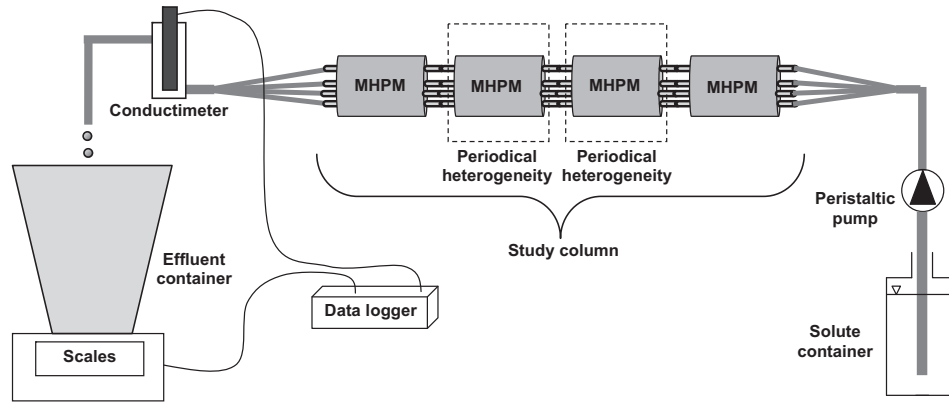


Fig. 3. Experimental setup with an example of a series of  $N = 4$  columns. Only the in-between column correspond to periodical heterogeneities.

### 3. Experimental results

#### 3.1. Experimental breakthrough curve

For each value of  $N$ , four experimental signals are computed: the average breakthrough concentration  $\bar{C}(t)$ , its standard deviation  $\sigma_C$ , the minimum and maximum breakthrough concentrations, defined as

$$\begin{aligned} \bar{C}(t) &= \frac{1}{R} \sum_{i=1}^R C_i(t), & \sigma_C^2 &= \frac{1}{R-1} \sum_{i=1}^R [C_i(t) - \bar{C}(t)]^2, \\ C_{\min}(t) &= \min_i C_i(t), & C_{\max}(t) &= \max_i C_i(t) \end{aligned} \quad (1)$$

where  $C_i(t)$  is the concentration at time  $t$  for the  $i$ th replicate and  $R$  is the number of replicates. The standard deviation and the difference between the minimum and maximum signals provide a measure of experiment variability.

Fig. 4 (top) shows the experimental signals obtained for the four values  $N = 3, 5, 10$  and  $15$ . As expected from previously published studies (Danquigny et al., 2004; Huang et al., 1995; Saiers et al., 1994), the breakthrough curve for small  $N$  strongly differs from the analytical S-shaped solution of the AD model (see the graphs for  $N = 3, N = 5$ ). As  $N$  increases, however, the breakthrough curves tend to behave similarly to a classical advection–dispersion model output ( $N = 10$  and  $N = 15$  in Fig. 4).

It is also worth stressing the strong variability of the breakthrough curve from one replicate to another for a given  $N$ . The amplitude of the standard deviation  $\sigma_C(t)$  shown in Fig. 4 is consistently about  $5 \times 10^{-2}$  regardless of  $N$ . The amplitude of the min–max interval seems to decrease for larger  $N$ , but this might be due only to the smaller number of experiments (the min and max indicators being biased contrarily to the standard deviation).

This experimental result has two main consequences. First, it clearly shows that the observed behaviour (atypical or typical breakthrough curve) depends on the observation scale. Second, it leads to question the use of the AD approach to model solute transfer in porous media for small spatial scales. Indeed, the AD is adequate to reproduce breakthrough curves with a typical ‘S’ shape but not those with atypical behaviour. Several studies on heterogeneous porous media have already shown that the AD model is

inadequate to describe the resulting breakthrough curves (Saiers et al., 1994; Huang et al., 1995; Danquigny et al., 2004; Li et al., 1994).

Additional information is brought by the Laplace transform of  $dC^*/dt(t)$

$$P(s) = s \int_0^{+\infty} C^*(t) \exp(-st) dt \quad (2)$$

where  $s$  is the Laplace variable. Since the input concentration is a unit step,  $P(s)$  is the Laplace transform of the response of the  $N$  columns to a concentration unit pulse. The graphs  $P(s)$  are shown in Fig. 4 (bottom). The graphs are drawn for  $s \leq 0.1$  Hz because the sampling time step is 5 s, thus making the numerical computation of (2) inaccurate for larger  $s$ . The response  $P(s)$  behaves as a decreasing exponential for large  $s$ , as indicated by the linear asymptote in the graphs ( $P$  is plotted using logarithmic coordinates). This is the typical signature of a delay. That the asymptotic linear behaviour is reached for smaller  $s$  as  $N$  increases indicates that advection phenomena become predominant as  $N$  increases, a well-known feature of the advection–dispersion model for increasing Peclet number values. This, however, is not sufficient to validate the AD model, an issue that is addressed in Section 4.1.

#### 3.2. Scaling trend for the dispersion coefficient

Questions (Q1) and (Q2) are answered assuming that the AD model is valid, with governing equations

$$\frac{\partial C}{\partial t} + u \frac{\partial C}{\partial x} - D \frac{\partial^2 C}{\partial x^2} = 0 \quad (3a)$$

$$C(x, 0) = 0 \quad \forall x \in [0, L] \quad (3b)$$

where  $D$  is the dispersion coefficient, and  $u$  the flow velocity. Analytical solutions are available for an upstream boundary condition in the form of a step flux function (Ogata and Banks, 1961)

$$\begin{aligned} C(0, t) &= C_0 \quad \forall t > 0 \Rightarrow C(x, t) \\ &= \left[ \operatorname{erfc} \left( \frac{x - ut}{2(Dt)^{1/2}} \right) + \exp \left( \frac{ux}{D} \right) \operatorname{erfc} \left( \frac{x + ut}{2(Dt)^{1/2}} \right) \right] \frac{C_0}{2} \end{aligned} \quad (4)$$

The unit response to a Dirac flux pulse is obtained as the derivative of (4) with respect to time

$$\begin{aligned} C(0, t) &= C_0 \delta(t) \Rightarrow C(x, t) = \frac{C_0}{4\pi^{1/2}(Dt)^{3/2}} \left[ (x + ut) \exp \left( -\frac{(x - ut)^2}{4Dt} \right) \right. \\ &\quad \left. + (x - ut) \exp \left( -\frac{(x + ut)^2}{4Dt} \right) \right] \end{aligned} \quad (5)$$

Table 1

Experimental configurations.  $L$  is the total length of the porous media.

$N$	$V_0$ (ml)	$L$ (m)	Column groups	Total replicates
3	1383	0.45	ABC, FGH, DEJ, KLM, INO	20
5	2305	0.75	ABCDE, FGHIJ, KLMNO	12
10	4610	1.50	A–J, F–O	8
15	6915	2.25	A–O	4



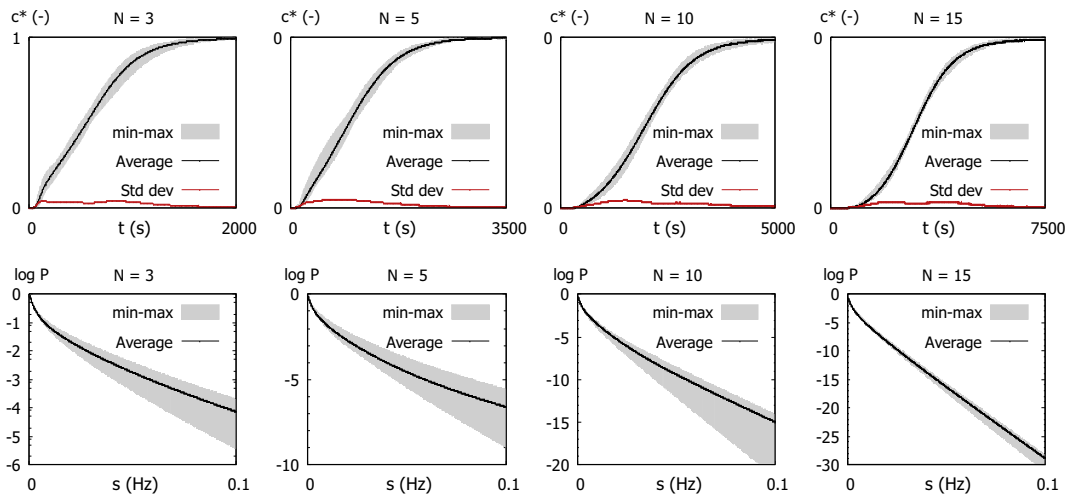


Fig. 4. Breakthrough curves and the Laplace transforms of their derivatives for  $N = 3, 5, 10$ , and  $15$  MHPM. Note the logarithmic coordinates for the Laplace transform.

The Laplace transform of the solution (5) can also be obtained by solving Eq. (3) in the space-Laplace domain:

$$\hat{C}(x, s) = \frac{2}{1+F} \exp\left(\frac{ux}{D} \frac{1-F}{2}\right), \quad F = \left(1 + \frac{4D}{u^2 s}\right)^{1/2} \quad (6)$$

The experimental dispersion coefficient  $D$  is computed using a formula derived from the analytical solution of the advection–dispersion equation (Bear, 1972):

$$D = 2 \left( \frac{t_{60} - t_{40}}{t_{50}} \right)^2 Lu = 2 \left( \frac{t_{60} - t_{40}}{t_{50}} \right)^2 \frac{L^2}{t_{50}} \quad (7)$$

used by e.g. Irwin et al. (1996), Sternberg et al. (1996).

Eq. (7) was applied to the experimental configurations shown in Table 1. The detailed results are given in the Appendix (Tables A1–A4), only statistics are presented here. For each value of  $N$ , the average, standard deviation, minimum and maximum of  $D$  obtained from the various possible configurations are provided in Table 2. Several remarks can be made at this stage.

Firstly, the variations in the average  $D$  with  $L$  are smaller than the standard deviation of  $D$  for any given  $L$ . Since the individual variations between the replicates for a given  $N$  override by far any visible trend, it can be concluded that no significant trend of distance-dependent dispersion  $D(L)$  is detected given the experimental uncertainty.

Secondly, given the range of variations between the minimum and maximum values, it is possible to find a sequence among all the experimental values in Tables A1–A4 such that an increasing trend  $D(L)$  is detected. An example of such a sequence is (ABC1, ABCDE2, A–J4, A–O4). But it would be just as easy to detect a decreasing trend  $D(L)$  by choosing the values in Tables A1–A4 appropriately, for instance the sequence (KLM4, FGHIJ3, K–O2, A–O3). Such trends, however, would only be sampling artefacts.

It can be concluded as an answer to question (Q1) that, in the limit of experimental uncertainty, no significant scaling trend can be identified for the dispersion coefficient in the present MHPM. As an answer to question (Q2), sampling artefacts may easily lead

to the conclusion that the dispersion coefficient is subjected to a scaling trend in this MHPM. It is stressed that only the systematic replication of the tracer experiments and a high-resolution sampling allows this question to be answered with a satisfactory degree of confidence.

### 3.3. Unit transfer function

The purpose of the present subsection is to answer question (Q3). Since the various replicates  $C_i(t)$  all give different time series for a given number  $N$  of columns, the unit transfer function is different for each replicate. The proposed approach consists in determining the envelope of all possible  $C(t)$  signals for a Dirac input. It is obvious from definition (1) that neither the lower bound  $C_{\min}$  nor the upper bound  $C_{\max}$  of this envelope do correspond to a single replicate signal  $C_i(t)$ , the purpose being only to determine the range of possible variations of  $C(t)$  for each time  $t$ .

For this, it is necessary to estimate the unit transfer function of a single MHPM period. Denote by  $P_{N,i}$  the Laplace transform of the  $i$ th replicate for a number  $N$  of columns. A minimum–maximum confidence interval is defined for  $P$  with the following lower and upper bounds:

$$P_{N,\min} = \min_{i=1,\dots,R} P_{N,i}, \quad P_{N,\max} = \max_{i=1,\dots,R} P_{N,i} \quad (8)$$

where  $N$  denotes the number of columns used in the experiment and  $i$  denotes the replicate. This allows a confidence interval to be defined for the unit Laplace transform of a single MHPM period. Let  $r$  be the Laplace transform of a single MHPM period for a Dirac concentration input. The lower and upper bounds defined in (8) yield a confidence interval  $[r_{\min}(M, N), r_{\max}(M, N)]$  for  $r$ . Indeed, the convolution property of the Laplace transform leads to

$$r_{\min}(M, N) \leq r \leq r_{\max}(M, N) \quad \forall (M, N), M < N \quad (9a)$$

$$r_{\min}(M, N) = \left( \frac{P_{N,\min}}{P_{M,\max}} \right)^{\frac{1}{N-M}}, \quad r_{\max}(M, N) = \left( \frac{P_{N,\max}}{P_{M,\min}} \right)^{\frac{1}{N-M}}, \quad M < N \quad (9b)$$

Table 2  
AD model. Dispersion coefficients obtained using Eq. (7). See the detailed results in the Appendix.

$L$ (m)	$N$	$D$ ( $\text{m}^2 \text{s}^{-1}$ ) average	$D$ ( $\text{m}^2 \text{s}^{-1}$ ) standard deviation	$D$ ( $\text{m}^2 \text{s}^{-1}$ ) minimum	$D$ ( $\text{m}^2 \text{s}^{-1}$ ) maximum
0.45	3	$1.08 \times 10^{-4}$	$3.65 \times 10^{-5}$	$5.60 \times 10^{-5}$	$1.69 \times 10^{-4}$
0.75	5	$1.36 \times 10^{-4}$	$6.37 \times 10^{-5}$	$7.40 \times 10^{-5}$	$3.29 \times 10^{-4}$
1.50	10	$1.18 \times 10^{-4}$	$3.38 \times 10^{-5}$	$6.58 \times 10^{-5}$	$1.81 \times 10^{-4}$
2.25	15	$1.18 \times 10^{-4}$	$3.00 \times 10^{-5}$	$8.43 \times 10^{-5}$	$1.67 \times 10^{-4}$

If a unit transfer function with scale-independent parameters exists, all the confidence intervals  $[r_{\min}(M, N), r_{\max}(M, N)]$  derived for all possible combinations  $(M, N)$  should overlap. Denoting respectively by  $r_1$  and  $r_2$  the lower and upper bounds of the intersection of all the confidence intervals, one has by definition

$$r_1 = \max_{M,N} r_{\min}(M, N), \quad r_2 = \min_{M,N} r_{\max}(M, N) \quad (10)$$

The confidence intervals overlap provided that  $r_1(s) < r_2(s) \forall s$ .

Fig. 5a–f shows the min–max confidence intervals derived from Eq. (9b) for all the possible  $(M, N)$  combinations. It is noted that the confidence interval becomes narrower as the number  $(M-N)$  of periods used to determine the unit transfer function increases, thus indicating the convergence of the estimates (9b).

The intersection of all the confidence intervals is shown in Fig. 5g. The non-zero width of the interval  $[r_1, r_2]$  indicates that a transfer function with scale-independent parameters can indeed be found within the range  $N = 3$  to  $N = 15$ . In other words, it is possible to find a scalar transport model with spatially uniform parameters that yields simulation results lying within the experimental uncertainty. This model, however, is not necessarily the classical AD model. This issue is explored in the next section.

## 4. Discussion

### 4.1. Validity of the AD model

The purpose of the present section is to answer questions (Q4 and Q5). If the AD model is valid at the scale of  $N$  MHPM periods, then there exists a combination  $(D, u)$  such that

$$r_1^N(s) \leq \hat{C}(Nl, s) \leq r_2^N(s) \forall s \quad (11)$$

where  $l = 15$  cm is the length of a single MHPM period. Clearly, this condition is not satisfied for  $N = 1$ . Indeed, for large  $s$ , the analytical solution (6) behaves as

$$F \approx \frac{2}{u} D^{1/2} s^{1/2} \Rightarrow \hat{C}(Nl, s) \approx \frac{u}{D^{1/2} s^{1/2}} \exp\left(-\frac{Nl}{D^{1/2}} s^{1/2}\right) \quad (12)$$

a function with a horizontal asymptotic direction in semi-logarithmic coordinates, while  $r_1(s)$  and  $r_2(s)$  take the form of straight lines for large  $s$  (see Fig. 5g). Consequently, the function  $\hat{C}(Nl, s)$  does not lie within the interval  $[r_1^N, r_2^N]$  for all  $s$  and the AD model is invalid to some extent. This is illustrated by Fig. 6a, where the confidence interval  $[r_1^N, r_2^N]$  and the function  $\hat{C}(Nl, s)$  are plotted for  $N = 1$ .

The degree of accuracy of the AD model is assessed by computing the  $L_2$ -norm of the difference between the experimental transfer function and the theoretical one in the Laplace space:

$$L_2 = \left[ \frac{1}{S} \int_0^S \varepsilon^2(s) ds \right]^{1/2} \quad (13a)$$

$$\varepsilon(s) = \begin{cases} \hat{C}(Nl, s) - r_1^N(s) & \text{if } \hat{C}(Nl, s) < r_1^N(s) \\ 0 & \text{if } r_1^N(s) \leq \hat{C}(Nl, s) \leq r_2^N(s) \\ \hat{C}(Nl, s) - r_2^N(s) & \text{if } \hat{C}(Nl, s) > r_2^N(s) \end{cases} \quad (13b)$$

where  $S = 0.1$  Hz is the upper bound of  $s$ . Eq. (13b) gives a zero error if the solution of the AD model lies between  $r_1$  and  $r_2$  in the Laplace space, that is, if the AD solution falls within the range of the experimental uncertainty.

Table 3 shows the combinations  $(D, u)$  that minimize the  $L_2$ -norm (13a) for various values of  $N$ . Fig. 6a–g shows the corresponding plots in the Laplace space. The  $L_2$ -norm for  $N = 1$  is large, indicating that the AD model provides a poor description of the transfer process at the scale of a single column. However, the  $L_2$ -norm decreases quickly with  $N$ , which is an indication that the AD model gains worth with the number of MHPM periods. The driving mechanism for this is interesting to notice. As shown by Fig. 6a–g, the AD transfer function lies outside the confidence interval for  $s > 3 \times 10^{-2}$  Hz in all graphs. In other words, in terms of relative error, the AD model is equally inaccurate for all values of  $N$ . However, the amplitude of the transfer function decreases quickly as  $N$  increases. The absolute value of the error thus becomes smaller as  $N$  increases.

Note that the value for  $D$  is found to be consistently about  $2 \times 10^{-4} \text{ m}^2 \text{ s}^{-1}$  (except for  $N = 3$ ), while formula (7) gives an average value of about  $1.2 \times 10^{-4} \text{ m}^2 \text{ s}^{-1}$  (see Table 2). This striking difference between the two sets of values can be explained by the calibration approach. The values given in Table 1 are computed separately for each individual experiment, under the assumption that the AD model provides an accurate description of the transport processes for each experiment. However, a  $(D, u)$  combination calibrated for a given replicate will fail totally to predict the behaviour of another replicate.

In contrast, the dispersion coefficient values in Table 3 account for the variability of experimental uncertainty. It is not requested that the AD model should satisfy each individual experiment as accurately as possible, but that its response should lie within the intersection of all the confidence intervals associated with

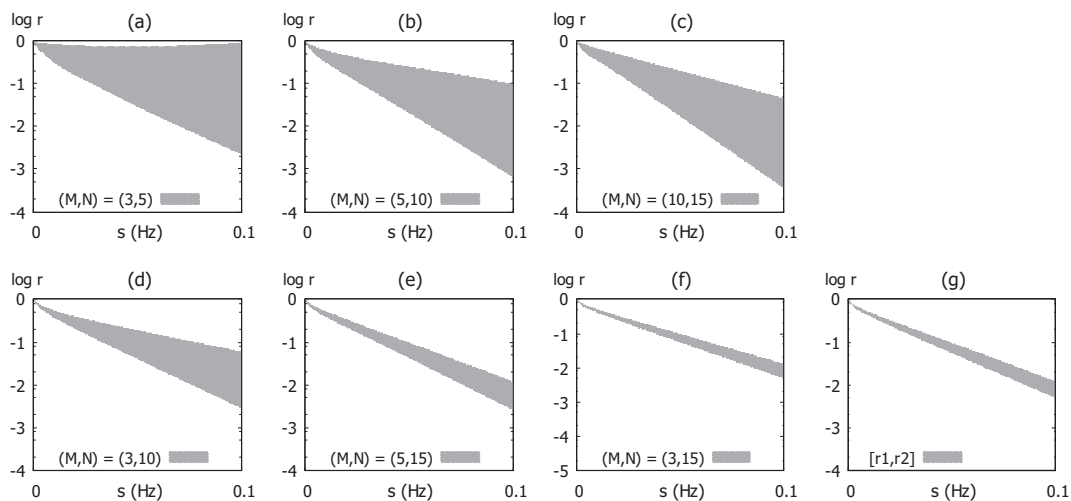


Fig. 5. Unit response of a column inferred from the Laplace transforms of the experimental signals.

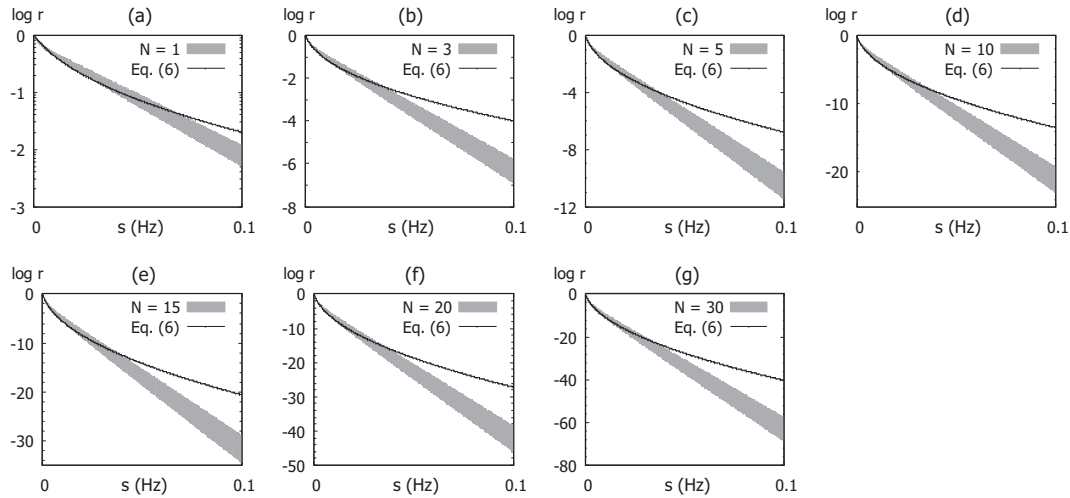


Fig. 6. Best AD model fits in the Laplace space for various values of  $N$ .

**Table 3**  
AD model. Optimal parameter set for the objective function (13a and b).

$N$	$D$	$u$	$L_2$	Figure
1	$1.57 \times 10^{-4}$	$1.98 \times 10^{-3}$	$2.13 \times 10^{-3}$	6a
3	$2.85 \times 10^{-4}$	$1.18 \times 10^{-3}$	$1.27 \times 10^{-4}$	6b
5	$2.36 \times 10^{-4}$	$9.98 \times 10^{-4}$	$1.70 \times 10^{-6}$	6c
10	$2.24 \times 10^{-4}$	$7.97 \times 10^{-4}$	$1.75 \times 10^{-10}$	6d
15	$2.07 \times 10^{-4}$	$7.71 \times 10^{-4}$	$6.51 \times 10^{-15}$	6e
20	$2.07 \times 10^{-4}$	$7.71 \times 10^{-4}$	$2.045 \times 10^{-18}$	6f
30	$2.07 \times 10^{-4}$	$7.71 \times 10^{-4}$	$2.66 \times 10^{-25}$	6g

different MHPM lengths. As a consequence, smoother unit responses (thus larger dispersion coefficient values) are allowed compared to the former approach. Moreover, both calibration approaches use different variables (pointwise  $C(t)$  values in the first approach,  $\hat{C}(Nl, s)$  over an interval in the second approach).

#### 4.2. Validity of alternate transport models

This section is motivated by Question (Q6). Since the classical AD model fails to reproduce the unit pulse response of the column, the question arises whether alternate transport models may be more successful. To start with, examining Fig. 5g indicates an asymptotically linear behaviour in semi-logarithmic coordinates. In other words, the unit transfer function is asymptotically equivalent to a decreasing exponential in the Laplace space. The experimental unit transfer function thus verifies the following property:

$$\hat{C}(x, s) \underset{s \rightarrow \infty}{\approx} A \exp(-Bxs) \Rightarrow C(x, t) \underset{t \rightarrow 0}{\approx} H(t - Bx)f(t) \quad (14)$$

where  $A$  and  $B$  are constants and  $H$  is Heaviside's step function. In other words, the signal propagates at a finite velocity  $B^{-1}$ , with a breakthrough concentration rising from 0 at  $t = Bx$  to 1 for  $t \rightarrow \infty$ . The inadequacy of the AD model for small times and distances precisely stems from the infinite front propagation speed associated with the Fickian flux model.

The Mobile-Immobile (MI) model (Van Genuchten and Wierenga, 1977) is one of the earliest and most probably best-known non-Fickian models for dispersion. Later on, generalizations such as the multirate model (Haggerty and Gorelick, 1995) have been proposed. The governing equations for the MI model are:

$$\frac{\partial C_m}{\partial t} + u \frac{\partial C_m}{\partial x} - D \frac{\partial^2 C_m}{\partial x^2} = \frac{k}{\theta} (C_i - C_m) \quad (15a)$$

$$\frac{\partial C_i}{\partial t} = \frac{k}{1 - \theta} (C_m - C_i) \quad (15b)$$

where  $C_i$  and  $C_m$  are respectively the concentrations in the immobile and mobile regions,  $k$  is an exchange rate constant and  $\theta$  is the relative volume fraction of the mobile region. Applying the Laplace transform in time, eliminating  $C_i$  yields

$$\frac{d^2 \hat{C}_m}{dx^2} - \frac{u}{D} \frac{d \hat{C}_m}{dx} - a \frac{s}{D} \hat{C}_m = 0, \quad a = \frac{k + (1 - \theta)\theta s}{[k + (1 - \theta)s]\theta} \quad (16a)$$

$$\hat{C}_m(x, s) = \hat{C}_m(0, s) \exp(-\lambda x), \quad \lambda = \left[ \left( \frac{u}{2D} \right)^2 + \frac{as}{D} \right]^{1/2} - \frac{u}{2D} \quad (16b)$$

For large  $s$ , the following equivalence is obtained:

$$a \underset{s \rightarrow \infty}{\approx} 1 \Rightarrow \hat{C}_m(x, s) \underset{s \rightarrow \infty}{\approx} A \exp \left( -\frac{s^{1/2}}{D^{1/2}} x \right) \quad (17)$$

leading to a horizontal asymptotic direction in the semi-logarithmic plots of Figs. 4–6. Consequently, the  $\hat{C}_m(x, s)$  curve (16) cannot remain between the min and max bounds of the experimental confidence interval for large  $s$ , thereby failing to account for the experimental MHPM behaviour for small times.

The modelling community's attention has been drawn over the past years to anomalous transport models (see e.g. Gao et al., 2009 for a review). Anomalous transport models use a non-Fickian model for dispersion. The underlying assumption is that the characteristic time scale and/or the characteristic length of the solute movement are infinite. Under such conditions, the assumption of Brownian movement is no longer valid and long-term memory effects appear. The general form for anomalous transport models is

$$\frac{\partial C}{\partial t} + u \frac{\partial C}{\partial x} - D \frac{\partial^{1-\alpha} C}{\partial t^{1-\alpha}} \frac{\partial^\gamma C}{\partial x^\gamma} = 0, \quad \begin{cases} 0 < \alpha \leq 1 \\ 0 < \gamma \leq 1 \\ \beta \in \{1 - \alpha, 1\} \end{cases} \quad (18)$$

where  $\partial^k / \partial t^k$  stands for the  $k$ th-order fractional time derivative (see e.g. Oldham and Spanier, 1974; Podlubny, 1999 for definitions). For  $\alpha < 1, \gamma < 1$ , Eq. (18) is obtained assuming that the probability density function  $w$  of the displacement time and  $d$  of displacement length obey the following asymptotic behaviours for large time and distances (Metzler and Klafter, 2000):

$$w(t) \underset{t \rightarrow +\infty}{\approx} \frac{A}{t^{1+\alpha}}, \quad d(x) \underset{x \rightarrow +\infty}{\approx} \frac{B}{x^{1+\gamma}} \quad (19)$$

The combinations  $(\beta = 1 - \alpha, \gamma = 1)$  and  $(\beta = 1, \gamma = 1)$  correspond respectively to the so-called Galilean-variant and Galilean-invariant fractional diffusion models presented in Metzler and Klafter (2000) under the Continuous Time Random Walk (CTRW) formalism. For  $\gamma < 1$ , so-called Levy walks are obtained. As shown in Klafter et al. (1987), that solute particles may cover arbitrary long distances within a displacement (thus leading to infinite velocities, a physical impossibility) may be balanced by a coupling between the pdfs  $w(t)$  and  $d(x)$ . Depending on the respective natures of  $w$  and  $d$ , any anomalous dispersive behaviour may be obtained, from subdiffusive to superdiffusive. Note that the case  $(\alpha = \beta = 1, \gamma < 1)$  has been investigated by Pachepsky et al. (2000) and applied to column experiment simulation by Gao et al. (2009). The behaviour of the analytical expression given by Pachepsky et al. (2000) is not easy to analyze, even in the Laplace space. However, a qualitative reasoning suffices to discard this option to model the present experiments. The Levy flight model yields infinite signal propagation velocities, just as does the standard, Fickian model. Consequently, for large  $s$ , this model also lies outside the experimental unit response of the MHPM in the Laplace space. The case  $\gamma < 1$  will therefore not be analyzed hereafter.

For  $\gamma = 1$ , applying the Laplace transform to (18) gives

$$\frac{d^2 \hat{C}}{dx^{12}} - \frac{u}{D} s^{1-\alpha-\beta} \frac{d^\beta \hat{C}}{dx^\beta} - \frac{s^\alpha}{D} \hat{C} = 0 \quad (20a)$$

$$\begin{aligned} \hat{C}(x, s) &= \hat{C}(0, s) \exp(-\lambda x), \quad \lambda \\ &= \left[ \left( \frac{u}{2D} \right)^2 s^{2-2\alpha-2\beta} + \frac{s^\alpha}{D} \right]^{1/2} - \frac{u}{2D} s^{1-\alpha-\beta} \end{aligned} \quad (20b)$$

which gives the following equivalences

$$\beta \in \{1 - \alpha, 1\} \Rightarrow \lambda \underset{s \rightarrow +\infty}{\approx} \frac{s^{\alpha/2}}{D^{1/2}} \Rightarrow \tilde{C}(x, s) \underset{s \rightarrow +\infty}{\approx} A \exp\left(-\frac{s^{\alpha/2}}{D^{1/2}} x\right) \quad (21)$$

As for the MI model, this model yields a horizontal asymptotic direction in semi-logarithmic coordinates and does not allow the experimental behaviour to be reproduced for large  $s$ .

Although attractive in theory, anomalous transport models may fail in a number of cases, not because they are not valid in general, but because they are not applied at the right space/time scales. Fractional derivatives are introduced in anomalous transport models under the assumption of heavy-tailed waiting time and travel distances probability density functions. The CTRW analysis (Klafter et al., 1987; Metzler and Klafter, 2000) shows that fractional derivatives stem naturally from this assumption as the Laplace variable  $s$  tends to zero. For the CTRW analysis to be valid, the observation time and/or travelled distance must be sufficient for a significantly large number of solute molecule jumps to occur. Moreover, the solute must cover a sufficient number of medium heterogeneities so that the ergodicity of the transport process be ensured. This underlying assumption is in contradiction with the present experimental setup, that obviously deals with space and time scales smaller than those required for ergodicity. As mentioned by Gao et al. (2009), the reason why anomalous transport models may succeed better to reproduce experimental column behaviour may simply be that they incorporate more degrees of freedom than classical transport models. As stressed by these authors, more degrees of freedom do not necessarily induce a better model.

## 5. Conclusions

This paper presents the results of intermediate scale tracer experiments carried out using a Model Heterogeneous Porous Medium with a variable length. The periodic character of the

medium allows the stationarity of the medium properties to be preserved. The large number of replicates (44 experiments for 4 different column lengths) allows sampling artefacts to be minimized and reliable statistics to be derived. A confidence interval for the unit transfer function of a single period of the model medium is derived from a Laplace transform analysis.

In the light of this work, the answers to questions (Q1–Q6) raised in the Introduction are the following.

- (A1) No clear scaling trend can be identified for the dispersion coefficient within the range of experimental uncertainty for the present MHPM.
- (A2) Given the strong individual variability observed from one replicate to another, sampling artefacts may lead to wrongly conclude that the dispersion coefficient is scale-dependent.
- (A3) There exists a model with scale-independent parameters that can provide a correct description of the solute transfer in the MHPM from  $N = 3$  to  $N = 15$ .
- (A4) This model is not the AD model, because it does not allow the experimental breakthrough curves to be reproduced accurately within the range of the experimental uncertainty.
- (A5) The AD model can be deemed to provide an accurate description of the present MHPM after the solute has been transported over at least 10 (and most probably 20) periods. The size of the REV for this MHPM is thus between 10 and 20 MHPM periods.
- (A6) The MI and CTRW models will fail to reproduce the small-time and short-distance experimental behaviour of the MHPM because of the second-order derivative used in the modelling of dispersion.

We should like to stress the strong variability of the experimental results, even in the case of the present artificial MHPM, that was intentionally made strictly periodic. This should make modellers extremely cautious when dealing with natural media, the geometry of which is often poorly known and does not exhibit the degree of determinism of the present MHPM. This makes the systematic replication of breakthrough experiments indispensable in seeking reliable conclusions on scaling effects, as well as in model calibration attempts. It is a useful reality check of the assumptions of stationarity and ergodicity (Kulasiri and Verwoerd, 2002) of the AD model. From a more general perspective, one might also question the relevance of investigating the scaling behaviour of the AD model for spatial scales where it is invalid. This questioning also holds for alternate models such as anomalous transport models.

Lastly, the present work shows the usefulness of a high resolution sampling in analyzing the MHPM transfer functions (each of the breakthrough curves used in this study is made of 500–1500 records).

Further research focuses on (i) an experimental design from which the boundary effects arising from the inlet distribution is absent, which would allow the unit response  $r$  to be derived directly for a single column, (ii) carrying out series of experiments at identical  $N$  for several discharge values, so as to analyze the dependence of the dispersion coefficient on the flow velocity, and (iii) developing and applying alternative transport models (among which variations of the multirate model) to better simulate the ISE using scale-independent parameters. The present experiments clearly indicate that such a model exists. However, it should most probably not be based on a Fickian description of dispersion.

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## Appendix A

Dispersion coefficient – detailed results.

See Appendix [Tables A1–A4](#).

**Table A1**

AD model. Dispersion coefficients obtained using Eq. (5) for  $N = 3$ .

Configuration	$t_{40}$ (s)	$t_{50}$ (s)	$t_{60}$ (s)	$D$ (m <sup>2</sup> s <sup>-1</sup> )
ABC1	495	585	680	$6.92 \times 10^{-5}$
ABC2	485	575	660	$6.52 \times 10^{-5}$
ABC3	485	580	660	$6.36 \times 10^{-5}$
ABC4	430	545	675	$1.50 \times 10^{-4}$
DEJ1	395	500	615	$1.57 \times 10^{-4}$
DEJ2	450	550	635	$8.33 \times 10^{-5}$
DEJ3	415	515	610	$1.13 \times 10^{-4}$
DEJ4	470	560	645	$7.06 \times 10^{-5}$
FGH1	515	605	690	$5.60 \times 10^{-5}$
FGH2	465	560	665	$9.22 \times 10^{-5}$
FGH3	480	600	725	$1.12 \times 10^{-4}$
FGH4	460	595	735	$1.45 \times 10^{-4}$
IHO1	425	555	665	$1.36 \times 10^{-4}$
IHO2	445	530	615	$7.86 \times 10^{-5}$
IHO3	400	510	620	$1.48 \times 10^{-4}$
IHO4	455	555	645	$8.55 \times 10^{-5}$
KLM1	435	545	675	$1.44 \times 10^{-4}$
KLM2	480	575	680	$8.52 \times 10^{-5}$
KLM3	435	550	680	$1.46 \times 10^{-4}$
KLM4	420	545	680	$1.69 \times 10^{-4}$

**Table A2**

AD model. Dispersion coefficients obtained using Eq. (5) for  $N = 5$ .

Configuration	$t_{40}$ (s)	$t_{50}$ (s)	$t_{60}$ (s)	$D$ (m <sup>2</sup> s <sup>-1</sup> )
ABCDE1	865	1005	1165	$9.97 \times 10^{-5}$
ABCDE2	900	1035	1170	$7.40 \times 10^{-5}$
ABCDE3	725	860	1010	$1.44 \times 10^{-4}$
ABCDE4	730	870	1020	$1.44 \times 10^{-4}$
FGHIJ1	890	1035	1185	$8.83 \times 10^{-5}$
FGHIJ2	840	970	1100	$8.33 \times 10^{-5}$
FGHIJ3	845	1035	1225	$1.46 \times 10^{-4}$
FGHIJ4	765	905	1065	$1.37 \times 10^{-4}$
KLMNO1	765	910	1065	$1.34 \times 10^{-4}$
KLMNO2	835	985	1140	$1.10 \times 10^{-4}$
KLMNO3	805	980	1165	$1.55 \times 10^{-4}$
KLMNO4	630	825	1035	$3.29 \times 10^{-4}$

**Table A3**

AD model. Dispersion coefficients obtained using Eq. (5) for  $N = 10$ .

Configuration	$t_{40}$ (s)	$t_{50}$ (s)	$t_{60}$ (s)	$D$ (m <sup>2</sup> s <sup>-1</sup> )
A-J1	1730	1965	2215	$1.40 \times 10^{-4}$
A-J2	1850	2090	2320	$1.09 \times 10^{-4}$
A-J3	1695	1960	2245	$1.81 \times 10^{-4}$
A-J4	1800	2035	2280	$1.23 \times 10^{-4}$
K-O1	1925	2125	2350	$8.47 \times 10^{-5}$
K-O2	1805	2015	2235	$1.02 \times 10^{-4}$
K-O3	1870	2050	2225	$6.58 \times 10^{-5}$
K-O4	1675	1905	2140	$1.41 \times 10^{-4}$

**Table A4**

AD model. Dispersion coefficients obtained using Eq. (5) for  $N = 15$ .

Configuration	$t_{40}$ (s)	$t_{50}$ (s)	$t_{60}$ (s)	$D$ (m <sup>2</sup> s <sup>-1</sup> )
A-O1	2800	3075	3360	$1.09 \times 10^{-4}$
A-O2	2655	2925	3185	$1.14 \times 10^{-4}$
A-O3	2785	3025	3265	$8.43 \times 10^{-5}$
A-O4	2680	3010	3350	$1.67 \times 10^{-4}$

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