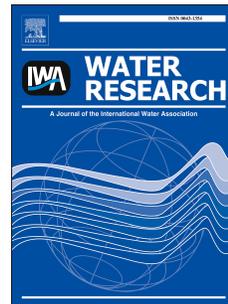


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Adsorption of Halogenated Aliphatic Contaminants by Graphene Nanomaterials

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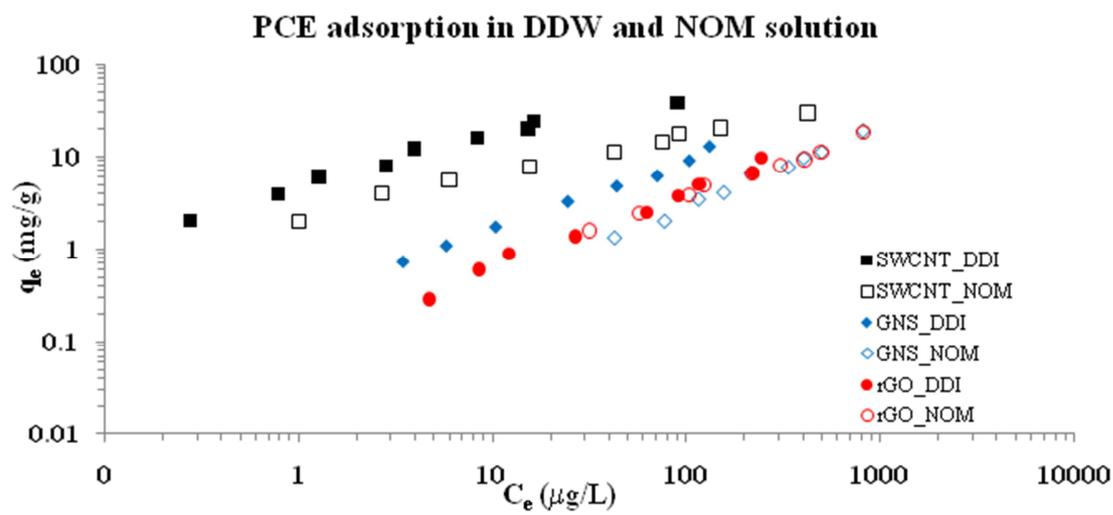
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**Adsorption of Halogenated Aliphatic Contaminants by Graphene  
Nanomaterials**

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24 **ABSTRACT**

25 In this study, adsorption of ten environmentally halogenated aliphatic synthetic organic  
26 compounds (SOCs) by a pristine graphene nanosheet (GNS) and a reduced graphene oxide (rGO)  
27 was examined, and their adsorption behaviors were compared with those of a single-walled  
28 carbon nanotube (SWCNT) and a granular activated carbon (GAC). In addition, the impacts of  
29 background water components (i.e., natural organic matter (NOM), ionic strength (IS) and pH)  
30 on the SOC adsorption behavior were investigated. The results indicated HD3000 and SWCNT  
31 with higher microporous volumes exhibited higher adsorption capacities for the selected  
32 aliphatic SOC than graphenes, demonstrating microporosity of carbonaceous adsorbents played  
33 an important role in the adsorption. Analysis of adsorption isotherms demonstrated that  
34 hydrophobic interactions were the dominant contributor to the adsorption of aliphatic SOC by  
35 graphenes. However,  $\pi$ - $\pi$  electron donor-acceptor and van der Waals interactions are likely the  
36 additional mechanisms contributing to the adsorption of aliphatic SOC on graphenes. Among  
37 the three background solution components examined, NOM showed the most influential effect  
38 on adsorption of the selected aliphatic SOC, while pH and ionic strength had a negligible effects.  
39 The NOM competition on aliphatic adsorption was less pronounced on graphenes than SWCNT.  
40 Overall, in terms of adsorption capacities, graphenes tested in this study did not exhibit a major  
41 advantage over SWCNT and GAC for the adsorption of aliphatic SOC.

42

43 **Keywords:** Adsorption, Aliphatic Synthetic Organic Compounds, Graphenes, Carbon  
44 Nanotubes, Activated Carbons, Natural Organic Matter

45

## 46 1. Introduction

47 Graphenes are two-dimensional single layered,  $sp^2$  hybridized carbon atoms densely  
48 packed as a hexagonal honeycomb lattice and they can be visualized as basic building blocks for  
49 fullerenes, carbon nanotubes (CNTs) and graphite [Novoselov et al., 2004]. The unique structure  
50 endows graphenes with outstanding mechanical, optical and electronic properties [Geim, 2009;  
51 Lee et al., 2008; Novoselov et al., 2005], which make them ideal candidates for a wide range of  
52 commercial applications. Commercial production and industrial scale application of graphenes  
53 are expected to grow exponentially over the next decades [Geim and Novoselov, 2007; Li and  
54 Kraner, 2008]. However, due to their mass production, the release of carbonaceous  
55 nanomaterials (such as graphenes) into environment possess various health and environmental  
56 risks for plants, animals and humans [Nowack et al. 2012; Upadhyayula et al. 2009; Yu et al.  
57 2014; Zhang et al., 2010; Zhao et al., 2014]. Furthermore, some of the negative impacts might be  
58 increased as a result of adsorbing synthetic organic compounds (SOCs) by these nanomaterials,  
59 and the fate and transport of SOCs in the environment can be altered.”

60 Graphenes are hydrophobic nanomaterials with large specific surface areas (SSA); and  
61 they have been evaluated as promising adsorbents to remove SOCs from water [Zhao et al et al.,  
62 2011; Ramesha et al., 2011; Ji et al., 2013; Sharma and Das, 2013; Zhao et al., 2011; Li et al.,  
63 2012; Gao et al., 2012; Li et al., 2013; Apul et al., 2013; Wu et al., 2011]. In our previous study  
64 [Apul et al., 2013], graphenes were shown to have higher or comparable adsorption capacities to selected  
65 carbon nanotubes and granular activated carbons. In addition, the impact of NOM competition on the  
66 adsorption capacity of graphenes was less severe. Therefore, from an engineering perspective, graphenes  
67 may serve as novel and alternative adsorbents in engineered treatment system in future [Yu et al. 2015].  
68 To date, the majority of the tested SOCs were aromatic compounds; and no study has examined

69 the adsorption of aliphatics by graphenes. Several aliphatic SOCs are common organic pollutants  
70 that were either regulated by United States Environmental Protection Agency (US EPA) under  
71 Priority Pollutants List (e.g., trichloroethylene, tetrachloroethylene, 1,1-dichloroethylene) or  
72 listed under Candidate Contaminant List 3 (CCL3) (e.g., 1,1,1,2-tetrachloroethane, 1,1-  
73 dichloroethane). Given the paucity of data on this topic in literature, it is important to understand  
74 adsorption of aliphatic SOCs by graphenes to adequately assess the environmental impact and  
75 engineering applications of graphenes. Therefore, the main objectives of this study were to (i)  
76 investigate the factors controlling adsorption of halogenated aliphatic SOCs by graphenes in  
77 terms of adsorbent characteristics, adsorbate properties and background solution chemistry, and  
78 to (ii) evaluate the application potential of graphenes as alternative adsorbents in treatment  
79 systems by comparing their adsorption capacities with those of single-walled carbon nanotubes  
80 (SWCNT) and granular activated carbon (GAC).

81

## 82 **2. Materials and methods**

### 83 **2.1. Adsorbents**

84 Four carbonaceous adsorbents: pristine graphene nanosheets (GNS, Angstrom Materials  
85 Inc.), reduced graphene oxide (rGO, Graphenea CO., Ltd.), SWCNT (Chengdu Organic  
86 Chemicals Co., Ltd.) and GAC (HD3000, Norit Inc.) were used. GNS, rGO, and SWCNT were  
87 used as received from the manufacturers, while HD3000 was ground to 200-325  $\mu\text{m}$  mesh size  
88 prior to use. Selected physicochemical properties of the four carbonaceous adsorbents are  
89 summarized in Table 1.

90

## 91 2.2. Adsorbates

92 Ten aliphatic SOCs with different properties were purchased from Acros (PCE, > 99%),  
93 Fluka (12DCP, > 99%; 12DBE, > 98%), Matrix Scientific (DBCP, > 98%), Alpha Easer (TCE, >  
94 99.5%), TCI (1112TeCA, > 99%), Baker Analytical (111TCA, > 96.7%) and Sigma Aldrich  
95 (112TCA, > 96%; 11DCE, > 99%; CCl<sub>4</sub>, > 99.9%). Both of these aliphatic SOCs represented  
96 common organic pollutants that were either listed under Priority Pollutants List or CCL3, and  
97 they differ in molecular size, hydrophobicity, number of double bonds, and polarizability.  
98 Therefore, they were employed as probe molecules to cover some typical adsorbate-adsorbent  
99 interactions. Abbreviations, properties and molecular structures of the aliphatic SOCs are  
100 summarized in Tables 2 and S1 in Supporting Information.

101

## 102 2.3. NOM solution

103 The natural organic matter (NOM) was isolated from the influent of Myrtle Beach  
104 drinking water treatment plant in South Carolina using a reverse osmosis and followed by resin  
105 fractionation, as described elsewhere [Song et al., 2009]. SUVA<sub>254</sub>, defined as the ratio of UV  
106 absorbance at 254 nm divided by the dissolved organic carbon (DOC) concentration, is a  
107 quantitative measurement of the aromatic content per unit concentration of organic carbon in  
108 water [Karanfil et al., 2003]. Natural waters with high SUVA<sub>254</sub> values (e.g., more than 4.0  
109 L/mg-m) have organic matter with relatively high contents of hydrophobic, aromatic, and high  
110 molecular weight components, whereas waters with low SUVA<sub>254</sub> values (e.g., less than 2.0  
111 L/mg-m) contain mostly non-humic, hydrophilic and low molecular weight material. The

112 SUVA<sub>254</sub> value of the NOM solution used was around 4.0 L/mg-m, indicating it was rich in  
113 aromatic components.

114

#### 115 **2.4. Characterization of adsorbents**

116 Several techniques were used for the characterization of carbonaceous adsorbents.  
117 Nitrogen gas adsorption at 77 K was performed with a physisorption analyzer (Micromeritics  
118 ASAP 2010) to determine the SSA, total pore volumes (PV) and pore size distributions (PSD) of  
119 the four adsorbents. The Brunauer-Emmett-Teller (BET) equation was used to calculate SSA.  
120 The total PV were obtained from the adsorbed volume of nitrogen near the saturation point ( $P/P_0$   
121 = 0.99). PSD of adsorbents were determined from the nitrogen isotherms using the Density  
122 Functional Theory (DFT) model. Oxygen contents of the carbonaceous adsorbents were  
123 measured using a Flash Elemental Analyzer 1112 series (Thermo Electron Corporation). In  
124 addition, pH of the point of zero charge ( $pH_{PZC}$ ) of adsorbents was determined using pH  
125 equilibration technique. The details about these characterization methods have been provided  
126 elsewhere [Dastgheib et al., 2004].

127

#### 128 **2.5. Adsorption experiments**

129 Constant carbon dose aqueous phase isotherm experiments were conducted using  
130 completely mixed batch reactors (125 mL glass bottles with Teflon-lined screw caps). Two types  
131 of isotherms were conducted at room temperature ( $20 \pm 3$  °C):

132 (1) Distilled and deionized water (DDW) experiments: Concentrated stock solution of  
133 each aliphatic SOC was prepared in methanol. Bottles containing about 5 mg of adsorbents were

134 first filled with DDW and no headspace, and spiked with predetermined volumes of aliphatic  
135 SOC<sub>s</sub> from their methanol stock solutions. For the graphene experiments, the bottles with  
136 adsorbents were initially half filled with DDW, sonicated for 20 min, and completely filled with  
137 DDW prior to spiking aliphatic SOC<sub>s</sub>. The volume percentage of the methanol spiked solution  
138 per bottle was kept below 0.4% (v/v) to minimize the co-solvent effect. Preliminary kinetic  
139 experiments were performed for TCE adsorption onto four carbonaceous adsorbents; and the  
140 results showed that a time period of seven days was sufficient to reach equilibrium (Figure S1).  
141 Thus, the bottles with no headspace were placed into a rotary tumbler for one week. The solution  
142 pH remained around 6.5 during the experiments. To investigate the effect of pH on adsorption,  
143 additional adsorption isotherm experiments were conducted at pH 3 and 11, where the solution  
144 pH was adjusted by 0.1 mol/L HCl and NaOH. For ionic strength (IS) effect experiments, the  
145 same experimental procedure was used, except the ionic strength was adjusted with NaCl to  
146 three levels (IS=0.001, 0.01, 0.1 M). The ranges for pH and ionic strength were kept wider than  
147 those typically used in water and wastewater treatment or found in natural water systems to  
148 examine their impact in a wider parametric range.

149 (2) Preloading experiments: The NOM effect on adsorption of aliphatic SOC<sub>s</sub> by  
150 different carbonaceous adsorbents was examined under preloading condition, giving an advantage  
151 to NOM adsorption prior to that of the SOC<sub>s</sub>, which represents the most severe NOM  
152 competition condition. For the preloading experiments, bottles containing about 5 mg adsorbents  
153 were first filled fully with 3 mg DOC/L NOM solution buffered with 1mM  
154 NaH<sub>2</sub>PO<sub>4</sub>·H<sub>2</sub>O/Na<sub>2</sub>HPO<sub>4</sub>·7H<sub>2</sub>O and adjusted to pH 7.0, then the bottles with zero headspace were  
155 placed into a rotary tumbler. After four days, predetermined volumes of aliphatic SOC stock  
156 solutions were directly spiked into the bottles, and then the headspace-free bottles were tumbled

157 again for an additional week. In NOM preloading experiments, 200 mg/L  $\text{NaN}_3$  was added to  
158 NOM solution to minimize any biological activity.

159 After the equilibrium period of isotherm experiments, bottles were placed on a bench  
160 overnight to allow settling of the adsorbents, and supernatants of samples in the bottles were  
161 transferred to 10 mL centrifuge tube for centrifugation to remove the remaining adsorbents. The  
162 supernatants were extracted with hexane by liquid: liquid extraction and analyzed using a gas  
163 chromatograph with a micro-electron capture detector (GC- $\mu$ ECD) equipped with a Rxi-624Sil  
164 MS Column (Restek, USA). Bottles without any adsorbents served as blanks to monitor the loss  
165 of adsorbates during the experiments, which were found to be negligible.

166

## 167 **2.6. Isotherm modeling**

168 Four common isotherm models, Freundlich (FM), Langmuir (LM), Langmuir-Freundlich  
169 (LFM) and Polanyi-Manes models (PMM), were employed to fit the experimental data. The  
170 modeling results showed that FM model resulted in good fits with meaningful parameter values  
171 for every case (Tables S2 to S5). Therefore, the FM model was selected to fit the adsorption data  
172 in this study:

$$173 \quad q_e = K_F C_e^n \quad (1)$$

174 where  $q_e$  and  $C_e$  represent the solid-phase equilibrium concentration (mg/g) and the liquid-phase  
175 equilibrium concentration ( $\mu\text{g/L}$  or  $\text{mg/L}$ ), respectively,  $K_F$  is the unit-capacity parameter  
176 ( $(\text{mg/g})/C_e^n$ ), equal to the amount adsorbed at a value of  $C_e$  equal to unity, and  $n$  is a  
177 dimensionless parameter related to the surface heterogeneity. Two  $K_F$  parameters ( $K_{F\mu}$  and  $K_{Fm}$ )

178 were examined for SOCs adsorption capacities at equilibrium concentrations of  $1\mu\text{g/L}$  and  
179  $1\text{mg/L}$ , respectively.

180

### 181 **3. Result and discussion**

#### 182 **3.1. Adsorbent characterization**

183 The results of SSA, total PV, PSD, oxygen content and  $\text{pH}_{\text{PZC}}$  of the four carbonaceous  
184 adsorbents are summarized in Table 1. The SSA of GNS and rGO were 666 and  $497\text{ m}^2/\text{g}$ ,  
185 respectively; and they were considerably smaller than the theoretically calculated SSA of single-  
186 layered graphene nanomaterials ( $2630\text{ m}^2/\text{g}$ ) [Stoller et al., 2008]. The much lower SSA  
187 indicated that graphenes were not present as exposed single-sheets, instead they formed bundles  
188 decreasing the SSA. Very high total PV ( $> 3\text{ cm}^3/\text{g}$ ) of GNS indicated aggregation may be  
189 confining large amounts of space within its 'house-of-cards' like bundle structure. GNS had six  
190 times higher total PV than rGO, indicating the oxygen content of rGO may be inhibiting the  
191 formation of bulky pores (especially macropores) within its bundle structure. The lacking  
192 macropores may also be attributed to tighter aggregation of rGO due to hydrogen bonding  
193 between the oxygen containing functional groups within the graphene bundle. When comparing  
194 the graphenes with SWCNT and HD3000, no major difference was observed in SSA, total PV  
195 and PSD besides the notably large macropore volume of GNS. In addition, rGO had higher  
196 oxygen content (17.5%) than other adsorbents as expected, which suggested that the surface of  
197 rGO is more hydrophilic. The low  $\text{pH}_{\text{PZC}}$  value of rGO indicated a net negative charge under  
198 neutral conditions due to the presence of oxygen-containing functional groups.

199

### 200 **3.2. The effect of adsorbent properties on adsorption of aliphatics**

201 Adsorption isotherms of PCE, TCE and 1,1-DCE by the four carbonaceous adsorbents in  
202 DDW are presented in Figure 1 and the Freundlich isotherm parameters were summarized in  
203 Table S6. Some major observations from the isotherms and isotherm parameters are as follow:  
204 HD3000 and SWCNT exhibited higher adsorption capacities than graphenes for all aliphatic  
205 SOCs tested. The adsorption isotherms were normalized according to the SSA and micropore  
206 volumes of adsorbents. However, after normalization, the adsorbed amount of aliphatic SOCs by  
207 HD3000 and SWCNT were still higher than those of GNS and rGO (Figures 1-D, E, F, G, H, I).  
208 Adsorbents with higher micropore volumes (HD3000 and SWCNT) showed higher adsorption  
209 capacities; however, SSA or micropore volume difference did not completely explain the  
210 adsorption capacity difference. Because, SSA, total PV and PSD parameters were obtained in the  
211 bulk phase of adsorbents via N<sub>2</sub> adsorption, the aggregation of CNTs and graphenes in aqueous  
212 phase may change the availability of sorption sites for aliphatic SOCs unlike rigid activated  
213 carbon pore structure.

214 Pristine GNS exhibited higher uptake for the aliphatic SOCs than rGO even after surface  
215 area normalization, which was attributed to its low surface polarity. Oxygen-containing  
216 functional groups on carbonaceous adsorbents can decrease the accessibility of adsorbents for  
217 aliphatic SOCs either through (i) a decrease due to increasing hydrophilicity (i.e. polarity) of the  
218 surface, or (ii) a decrease in the number of available adsorption sites due to water cluster  
219 formation around the oxygen-containing functional groups. Similar effect of oxygen content of  
220 graphenes was also observed on the adsorption of aromatic organic contaminants [Apul et al.,  
221 2013].

222

### 223 3.3. The effect of aliphatic SOC properties on adsorption

224 To investigate the effect of aliphatic SOC properties, adsorption isotherms of the  
225 aliphatic SOC<sub>s</sub> on GNS and rGO are compared in Figures 2-A, B. Hydrophobic interactions are  
226 important driving forces for adsorption of SOC<sub>s</sub> from aqueous solutions. To investigate the  
227 contribution of hydrophobicity of the aliphatic SOC<sub>s</sub> on adsorption, the adsorption isotherms  
228 were normalized according to their solubilities (Figures 2-C, D). After the solubility  
229 normalization, the separation in the adsorption isotherms on both GNS and rGO were greatly  
230 reduced but isotherms did not converge on a single line. This indicates that hydrophobicity of the  
231 aliphatic SOC<sub>s</sub> was an important driving force for adsorption, and there were other factors  
232 contributing to adsorption.

233 To further investigate the effect of the other SOC properties on adsorption, the PCE, TCE  
234 and 11DCE isotherms were compared. These compounds have similar molecular structures and  
235 configurations but different number of chlorine atoms. As shown in Figures 3-A, B, adsorption  
236 affinities of the three aliphatic SOC<sub>s</sub> by GNS and rGO followed the same order: PCE > TCE >  
237 11DCE. Solubility normalization greatly reduced the differences in the adsorption isotherms,  
238 although isotherms did not converge on a single line (Figures 3-C, D), and still followed the  
239 same order with smaller differences. The difference in the strengths of  $\pi$ - $\pi$  electron donor-  
240 acceptor (EDA) interactions of these three aliphatics with the graphenes might influence their  
241 adsorption. The highly polarizable graphene sheet can play an amphoteric role attracting both  $\pi$   
242 electron-acceptors and  $\pi$  electron-donors to the surface; and chlorine atoms on carbon double  
243 bonds of the three SOC<sub>s</sub> can serve as  $\pi$  electron acceptors, which can involve in adsorption  
244 interactions between the SOC<sub>s</sub> and graphenes through  $\pi$ - $\pi$  EDA complex formation. Therefore,  
245 adsorption affinities of the three aliphatic SOC<sub>s</sub> by graphenes increase with increasing number of

246 chlorine atoms. Another possibility influencing adsorption of these three compounds is the  
247 nonspecific interactions generally referred to as van der Waals forces. These interactions can  
248 exist between molecules regardless of their chemical structures; and they are proportional to the  
249 product of polarizability or dipole moment of adsorbates and adsorbents. Thus, stronger van der  
250 Waals interactions between PCE and graphenes might occur due to its higher polarizability. The  
251 separation in solubility-normalized isotherms of the three aliphatic SOCs on both GNS and rGO  
252 were further reduced after polarizability normalization (Figures 3-E, F). This additional  
253 reduction suggested that increasing polarizability of aliphatic SOCs may also have positive  
254 effects in their adsorption. To further examine the effect of polarizability, two isomer aliphatic  
255 SOCs (111TCA and 112TCA) with different polarizability were selected. Figure 4 compares  
256 their adsorption isotherms on GNS and rGO after solubility normalization to eliminate the  
257 difference in the hydrophobicity of these two compounds. The results showed both GNS and  
258 rGO showed higher adsorption capacities for 112TCA than 111TCA. As seen in Table 2,  
259 112TCA has higher polarizability than 111TCA (0.68 vs. 0.41); thus stronger van der Waals  
260 interactions between 112TCA and graphenes may be expected.

261         Presence of  $\pi$ -electrons in the structure of aliphatic SOCs may be another factor affecting  
262 their adsorption on graphenes. Aromatic SOCs have strong  $\pi$ - $\pi$  bonding interactions with  
263 graphene surface due to presence of resonating  $\pi$ -electrons in their benzene rings [Apul et al.,  
264 2013]. To investigate whether the  $\pi$ -electrons of aliphatic SOCs exert the effect on their  
265 adsorption, solubility-normalized adsorption isotherms of PCE vs. 1112TeCA and TCE vs.  
266 112TCA were compared (Figure 5) because they have similar molecular structures but different  
267 carbon bonds. After the solubility normalization, the separation between their adsorption  
268 isotherms was reduced greatly; and the isotherms almost converged on a single line, which

269 indicated the  $\pi$ -electrons of aliphatic SOCs might have positive effect on their adsorption by  
270 graphenes. Both 1112TeCA and 112TCA were expected to have stronger van der Waals  
271 interactions with graphenes than PCE and TCE, respectively due to their higher polarizabilities,  
272 which would enhance their adsorption on graphenes. However, after solubility normalization,  
273 1112TeCA and 112TCA did not show higher adsorption affinities to graphenes as compared to  
274 PCE and TCE, which therefore indicated that the  $\pi$ -electrons of PCE and TCE possibly  
275 contributed to their adsorption on graphenes through  $\pi$ - $\pi$  EDA complex to counterbalance the  
276 contribution of van der Waals interactions to 1112TeCA and 112TCA adsorption. In addition,  
277 their solubility-normalized adsorption isotherms once again demonstrated hydrophobic  
278 interactions were dominant contributor for the adsorption of aliphatic SOCs on graphenes.

279

### 280 **3.4. The effect of background water components on adsorption of aliphatics**

#### 281 **3.4.1. The effect of NOM**

282 To investigate the effect of NOM on adsorption of aliphatic SOCs by graphenes and  
283 compare NOM effects on adsorption capacities of GNS, rGO and SWCNT, adsorption of six  
284 SOCs (PCE, TCE, 11DCE, 112TCA, 1112TeCA, and DBCP) with different properties by GNS,  
285 rGO and SWCNT were tested in NOM solution. Their adsorption isotherms in DDW and NOM  
286 solutions are presented in Figure 6. Freundlich isotherm parameters in DDI and NOM solution  
287 are provided in Table S6 and S7 in Supporting Information, respectively. Two parameters,  $R_{\mu}$   
288 and  $R_m$ , as the ratios of  $K_{F\mu}$  and  $K_{Fm}$  in NOM preloading conditions to those in DDW,  
289 respectively, were calculated to quantify the effect of NOM on the adsorption of the six aliphatic

290 SOCs by different adsorbents. The lower  $R_{\mu}$  and  $R_m$  values indicate a greater reduction of  
291 adsorption capacity due to NOM preloading.

292 For GNS and rGO, the NOM effect on adsorption capacity of GNS were stronger  
293 than rGO, as indicated by lower  $R_m$  values of GNS; and rGO exhibited comparable adsorption  
294 capacity in the presence of NOM and in DDW as reflected by  $R_m$  values of rGO for the six SOCs  
295 ranging from 0.72 to 0.91, which can be attributed to electrostatic repulsion of negatively  
296 charged NOM molecules and rGO surface. Because the low  $pH_{PZC}$  value of rGO (Table 1), it had  
297 a net negative charge under neutral pH conditions; and NOM molecules generally carry a net  
298 negative charge at the same pH, which would result in less NOM coating on the rGO surface.  
299 Furthermore, adsorption of six SOCs by GNS and rGO under NOM preloading conditions was  
300 compared to SWCNT adsorption. As shown in Table S7,  $R_m$  values of SWCNT for all six SOCs  
301 were smaller than those of rGO and GNS, indicating that preloaded NOM exhibited stronger  
302 suppression on the adsorption of the aliphatic SOCs by SWCNT. This was attributed to more  
303 hindrance of the aliphatic SOC access to the adsorption sites on SWCNT due to the microporous  
304 structure of SWCNT bundles in water, in contrast to the flat sheet structure of GNS and rGO.  
305 These findings were similar to those of aromatic organic contaminant adsorption, where  
306 preloaded NOM exhibited much smaller impact on adsorption capacity of rGO than that of  
307 SWCNT [Apul et al., 2013]. However, although preloaded NOM exerted smaller effects on the  
308 adsorption capacities of GNS and rGO as compared to SWCNT, graphenes did not exhibit a  
309 major advantage, in terms of adsorption capacities, over SWCNT for the adsorption of aliphatic  
310 SOCs in the NOM solution (Figure S2).

311 The uptakes of all six SOCs decreased under NOM preloading conditions as reflected by  
312  $R_m$  values. However, there were no clear trends observed in  $R_m$  values for each SOC; and the  $R_m$

313 values did not correlate with the SOCs properties such as solubility, molecular size or  
314 polarizability. In fact, preloaded NOM did not exert significantly different effects on the six  
315 SOCs adsorption in terms of the  $R_m$  values. Therefore, for the six aliphatic SOCs, their different  
316 physicochemical properties did not cause large differences in NOM effects on their adsorption.

317

### 318 **3.4.2. The effect of pH and ionic strength**

319 Three aliphatic SOCs ( $\text{CCl}_4$ , TCE, and DBCP) with different molecular structure,  
320 molecular size and chain lengths were employed as probe molecules to explore the effect of  
321 solution pH on adsorption of aliphatic SOCs by graphenes. The adsorption isotherms of  $\text{CCl}_4$ ,  
322 TCE and DBCP on GNS and rGO under different pH conditions are presented in Figure S3 in  
323 the Supporting Information. The change in pH did not influence the adsorption of these three  
324 aliphatic SOCs on GNS and rGO (except for DBCP under pH 11 conditions). Since the tested  
325 compounds are non-ionic, their adsorption was independent from solution pH. However, as pH  
326 increased, the dissociation of oxygen-containing functional groups on graphene surfaces  
327 (especially rGO) also did not show any influence indicating that adsorption of these three  
328 aliphatic SOCs occurred on the hydrophobic sites of graphene surface where there were no  
329 oxygen-containing functional groups. For DBCP at pH 11, we observed a higher adsorption by  
330 graphenes, but actually this does not reflect its real adsorption affinity. Because degradation and  
331 transformation of DBCP at high pH might occur during the adsorption experiments indicated by  
332 the very low ratio (0.10-0.15) between measured blank concentrations and calculated ones.

333 To investigate the effect of ionic strength, the same aliphatic SOCs selected for pH  
334 experiments were used in the adsorption experiments. Two potential impacts can be observed:  
335 (1) increasing ionic strength enhances the activity coefficient of hydrophobic organic

336 compounds, leading to a decrease in their solubility (i.e. salting out effect), which is favorable  
337 for SOCs adsorption [Zhang et al., 2010]; and (2) the ions may penetrate into the diffuse double  
338 layer surrounding the graphene surfaces and eliminate the repulsive energy between the  
339 adsorbents, facilitating the formation of a more compact aggregation structure (i.e. squeezing-  
340 out), which is unfavorable for SOCs adsorption [Zhang et al., 2010]. Increasing ionic strength  
341 had negligible effect on adsorption of the aliphatic SOCs by both GNS and rGO (Figure S3).  
342 Therefore, the results indicated that either the contribution of salting-out effect to the adsorption  
343 of these aliphatic SOCs was equivalent to that of the squeezing-out effect or both the salting-out  
344 effect and squeezing-out effect were too weak to influence the adsorption of the SOCs on  
345 graphenes.

346

#### 347 **4. Conclusions**

348 Graphene nanomaterials adsorbed halogenated aliphatic SOCs, however the overall  
349 adsorption capacities of graphene nanomaterials were smaller than those of carbon nanotubes  
350 and activated carbon in the presence of NOM. Hydrophobicity was the dominant contributor for  
351 the adsorption of aliphatic SOCs on graphenes, but it was not the only mechanism controlling the  
352 adsorption,  $\pi$ - $\pi$  EDA interaction and van der Waals interaction appear to be the additional  
353 mechanisms contributing to the adsorption of aliphatic SOCs on graphenes. It should be noted that  
354 these adsorption interactions were observed for the selected halogenated aliphatic contaminants with  
355 comparable molecular configuration and sizes in this study. Further research is warranted to confirm and  
356 extend the findings to larger and more complex aliphatic molecules or different classes of contaminants.  
357 Among the three background water characteristics examined, NOM showed the most important  
358 effect on adsorption, whereas the changes in pH and ionic strength had a negligible effect on the

359 adsorption of selected halogenated aliphatic SOCs. NOM preloading exerted minimal effect on  
360 adsorption capacities of rGO for aliphatic SOCs, which was attributed to low degree of NOM  
361 coating on rGO surface due to electrostatic repulsion between negatively charged NOM  
362 molecules and rGO. NOM exhibited severe suppression on adsorption capacities of SWCNT  
363 than those of graphenes. This was attributed to microporous structure of SWCNT aggregates as  
364 compared with flat sheet structure of graphenes. In terms of adsorption capacities, graphenes did  
365 not exhibit a major advantage over SWCNT and HD3000 for the adsorption of aliphatic SOCs.  
366 Future studies also need to examine adsorption kinetics to assess whether graphenes exhibit  
367 advantages over other carbonaceous adsorbents for halogenated aliphatic SOCs.

368

### 369 **Acknowledgement**

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373

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**Table 1.** Physicochemical properties of adsorbents

Adsorbent	SSA <sub>BET</sub> <sup>a</sup> m <sup>2</sup> /g	V <sub>T</sub> <sup>b</sup> cm <sup>3</sup> /g	DFT Pore Volume Distribution <sup>c</sup>			Oxygen Content %	pH <sub>pzc</sub>
			V <sub>micro</sub> (< 2 nm) cm <sup>3</sup> /g, (%)	V <sub>meso</sub> (2-50nm) cm <sup>3</sup> /g, (%)	V <sub>macro</sub> (> 50nm) cm <sup>3</sup> /g, (%)		
GNS	666	3.138	0.065, (2.1)	1.196, (38.1)	1.877, (59.8)	0.8	9.8
rGO	497	0.530	0.081, (15.3)	0.377, (71.1)	0.072, (13.6)	17.5	4.1
SWCNT	537	1.240	0.117, (9.4)	0.581, (46.9)	0.542, (43.7)	0.9	7.5
HD3000	642	0.775	0.108, (13.9)	0.449, (57.9)	0.218, (28.1)	3.4	6.9

520 <sup>a</sup> Specific surface area calculated with the Brunauer-Emmett-Teller (BET) model, <sup>b</sup> Total pore volume calculated from single point adsorption at P/P<sub>0</sub> = 0.99, <sup>c</sup> Pore  
521 volume in each pore size range obtained from the density functional theory (DFT) analysis.

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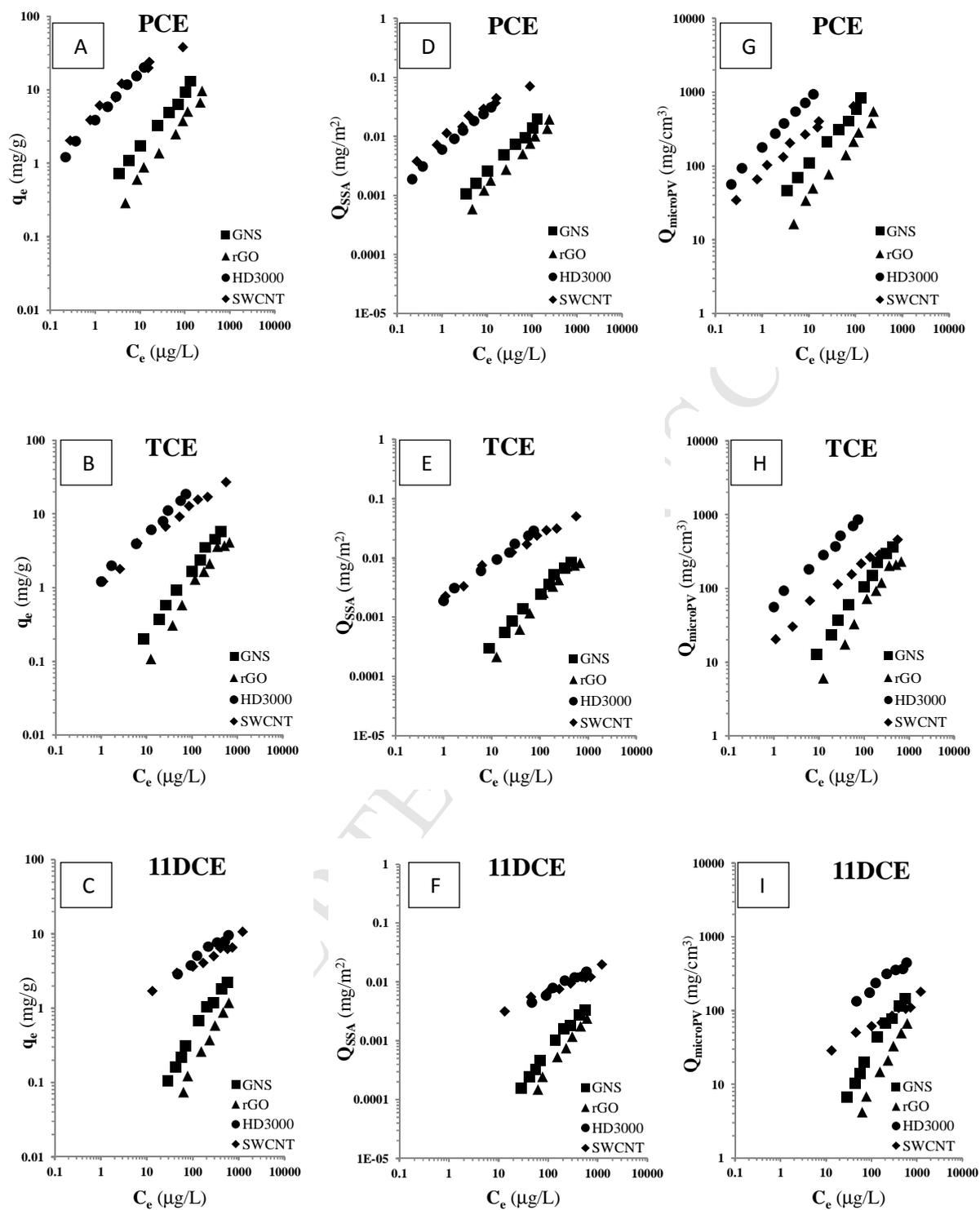
**Table 2.** Selected properties of aliphatic SOCs

SOC	Abbreviation	MW <sup>a</sup>	Density	MV <sup>b</sup>	C <sub>s</sub> <sup>c</sup>	LogK <sub>ow</sub> <sup>d</sup>	Polarizability <sup>e</sup>
		g/mol	g/cm <sup>3</sup>	cm <sup>3</sup> /mol	mg/L		
trichloroethylene	TCE	131	1.46	89.7	1183	2.42	0.37
tetrachloroethylene	PCE	166	1.62	102.5	224	3.40	0.44
1,1,1-trichloroethane	111TCA	133	1.32	100.8	1358	2.49	0.41
1,1,2-trichloroethane	112TCA	133	1.44	92.4	4483	1.89	0.68
carbon tetrachloride	CCl <sub>4</sub>	154	1.59	96.9	790	2.83	0.38
1,1-dichloroethylene	11DCE	97	1.21	80.2	2375	1.32	0.34
1,2-dichloropropane	12DCP	113	1.16	97.4	2819	2.28	0.68
1,2-dibromoethane	12DBE	188	2.17	86.6	4177	1.96	0.76
1,1,1,2-tetrachloroethane	1112TeCA	168	1.55	108.3	1103	2.93	0.63
1,2-dibromo-3-chloropropane	DBCP	236	2.08	113.5	985	2.43	0.78

523 <sup>a</sup> molecular weight; <sup>b</sup> molar volume; <sup>c</sup> water solubility at 25 °C obtained from the Material Safety Data Sheet of each compound; <sup>d</sup> octanol-water partitioning coefficient  
524 simulated with ACDLABS11.0 (ChemSketch and ACD/3D Viewer); <sup>e</sup> polarizability obtained from ACD/ADME Suite 5.0.

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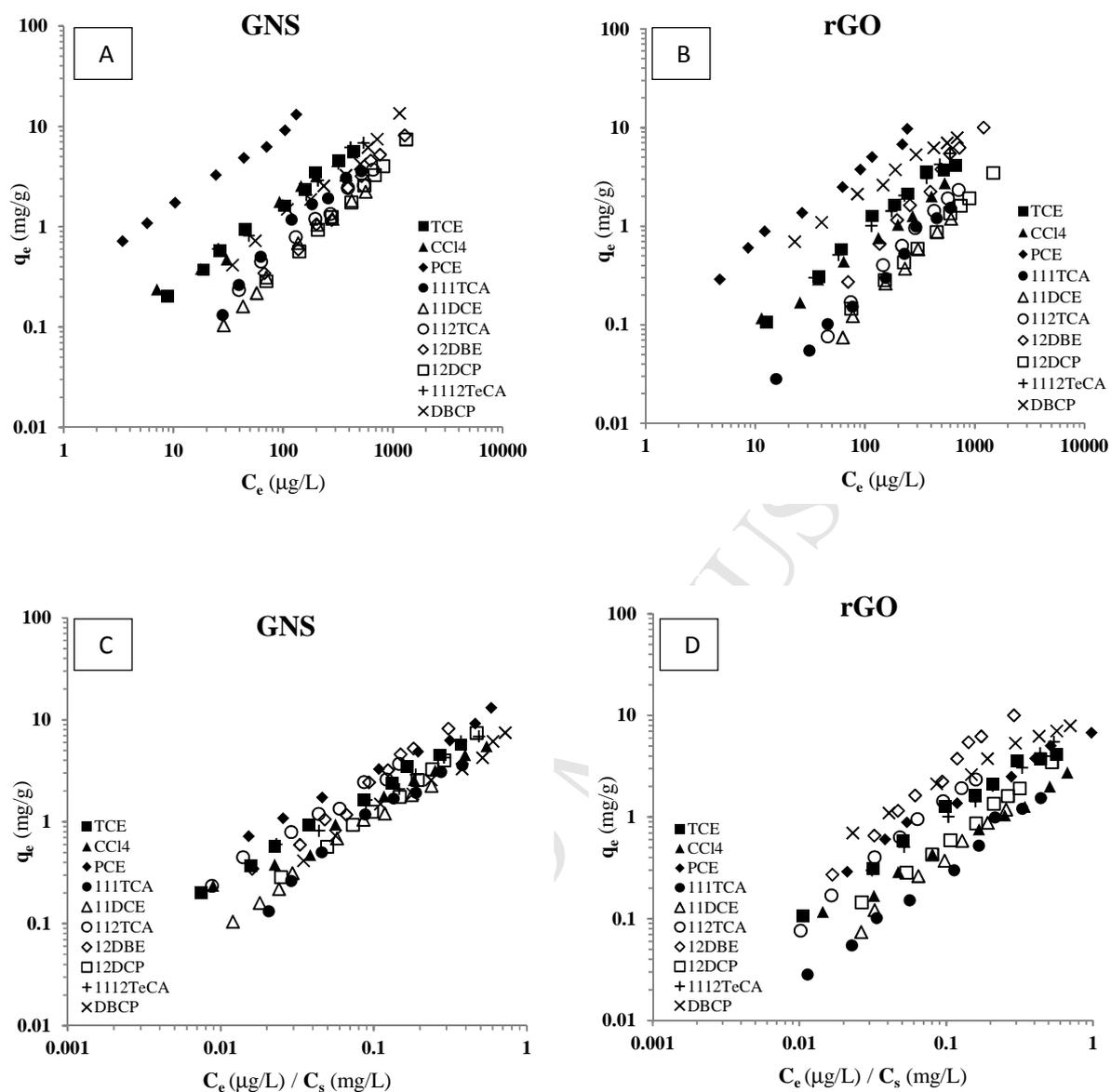
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532 **Figure 1.** Adsorption isotherms in DDW (A) PCE mass basis, (B) TCE mass basis, (C) 11DCE mass  
 533 basis, (D) PCE surface area normalized, (E) TCE surface area normalized, (F) 11DCE surface area  
 534 normalized, (G) PCE micropore volume normalized, (H) TCE micropore volume normalized, and (I)  
 535 11DCE micropore volume normalized.



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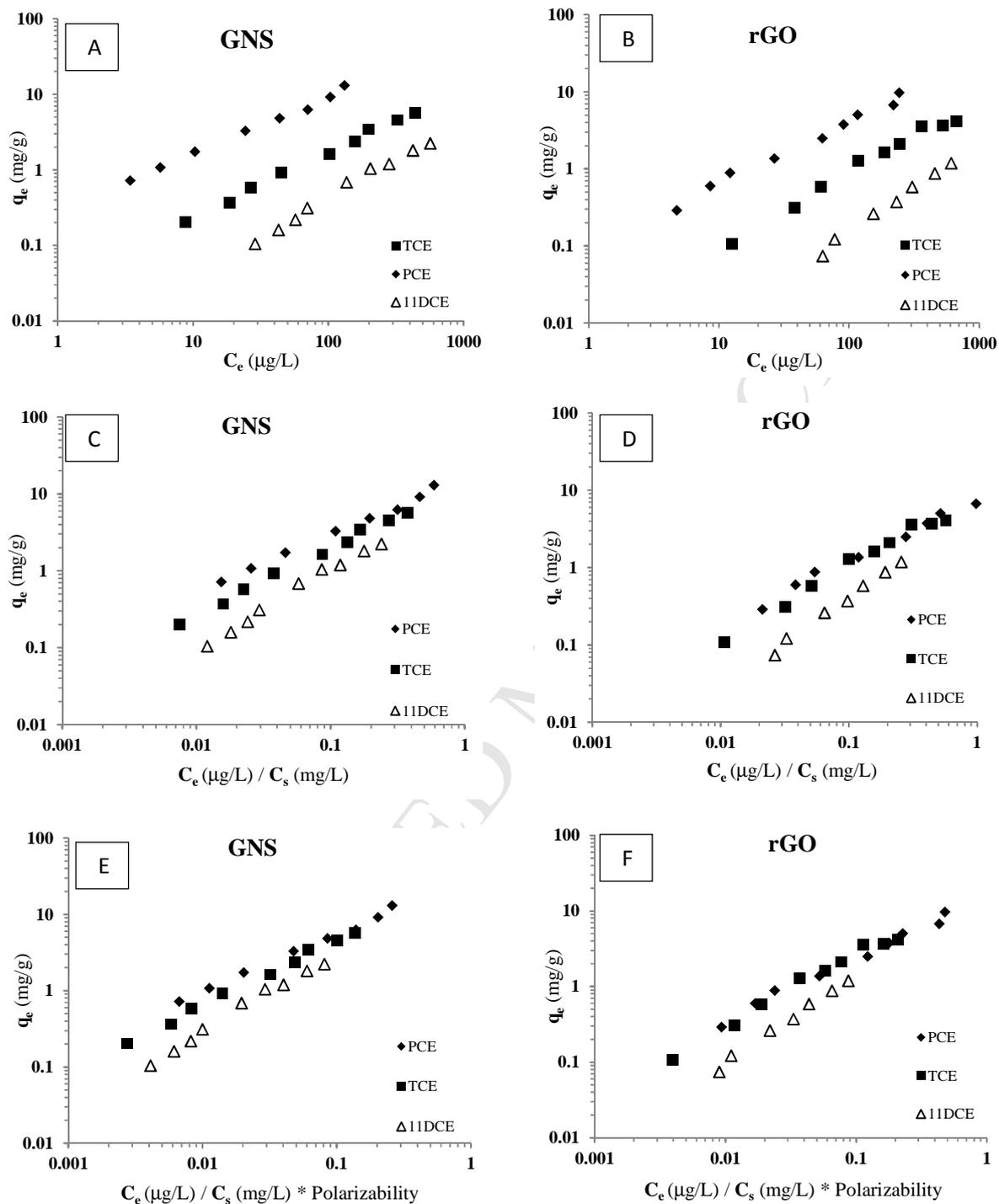
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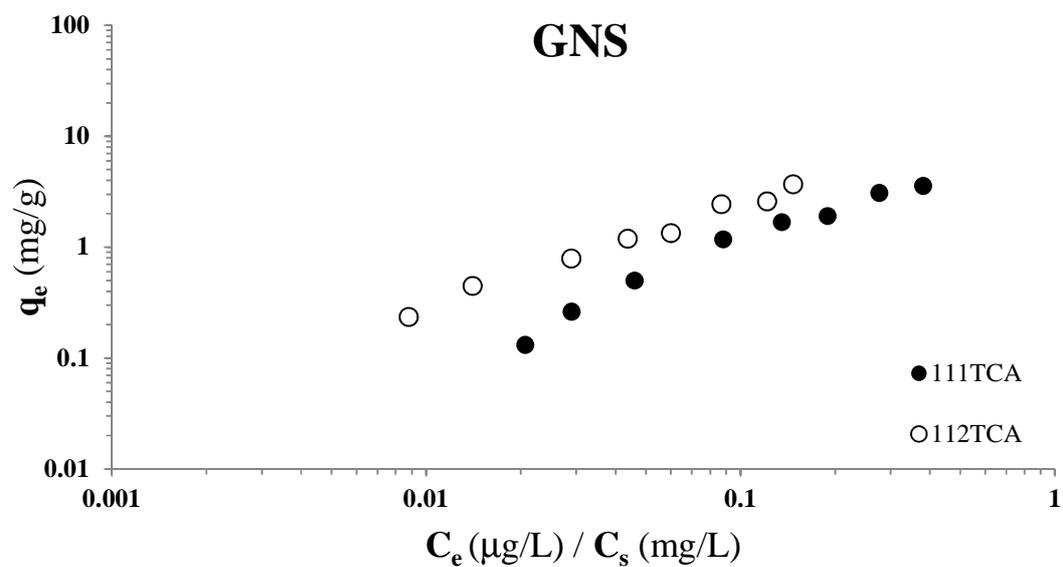
540 **Figure 2.** Adsorption isotherms of ten aliphatic SOCs by GNS and rGO in DDW (A) GNS mass basis,  
 541 (B) rGO mass basis, (C) GNS solubility normalized, (D) rGO solubility normalized .

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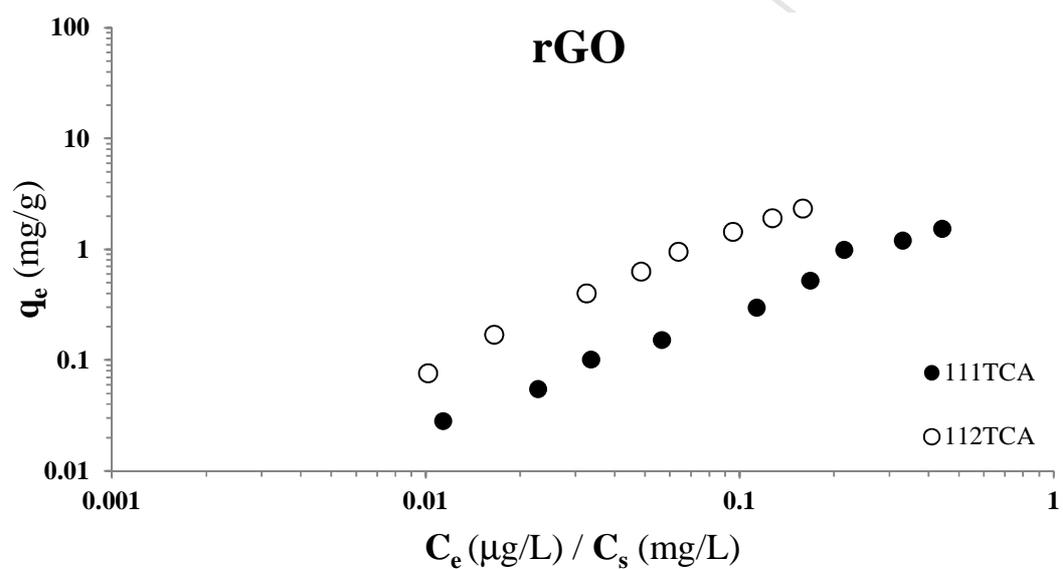
546 **Figure 3.** Adsorption isotherms of PCE, TCE and 11DCE in DDW (A) GNS mass basis, (B) rGO mass  
 547 basis, (C) GNS solubility normalized, (D) rGO solubility normalized, (E) GNS polarizability normalized,  
 548 and (F) rGO polarizability normalized.

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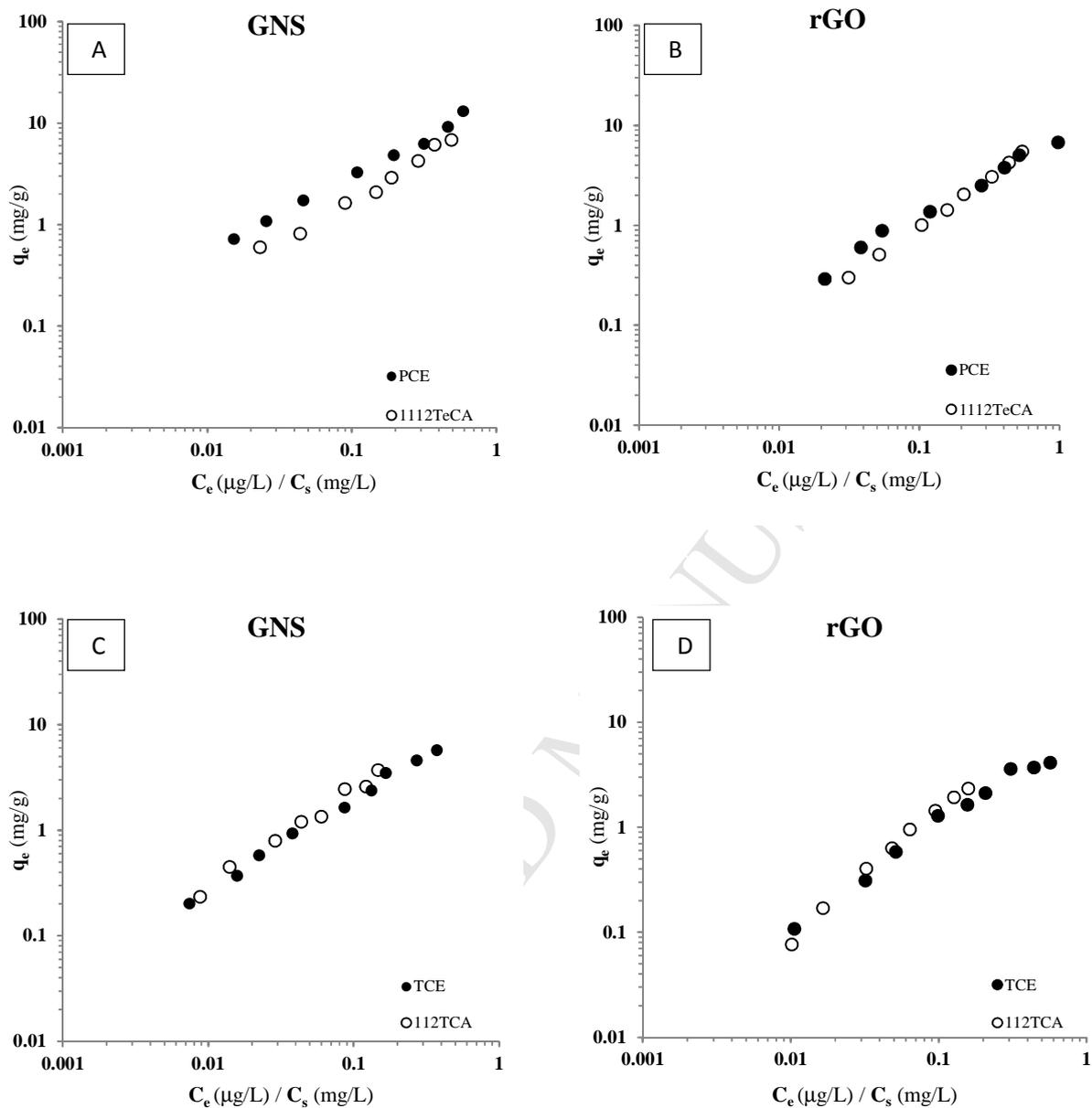
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553 **Figure 4.** Comparison of 111TCA and 112TCA solubility-normalized adsorption isotherms on GNS and  
554 rGO in DDW.

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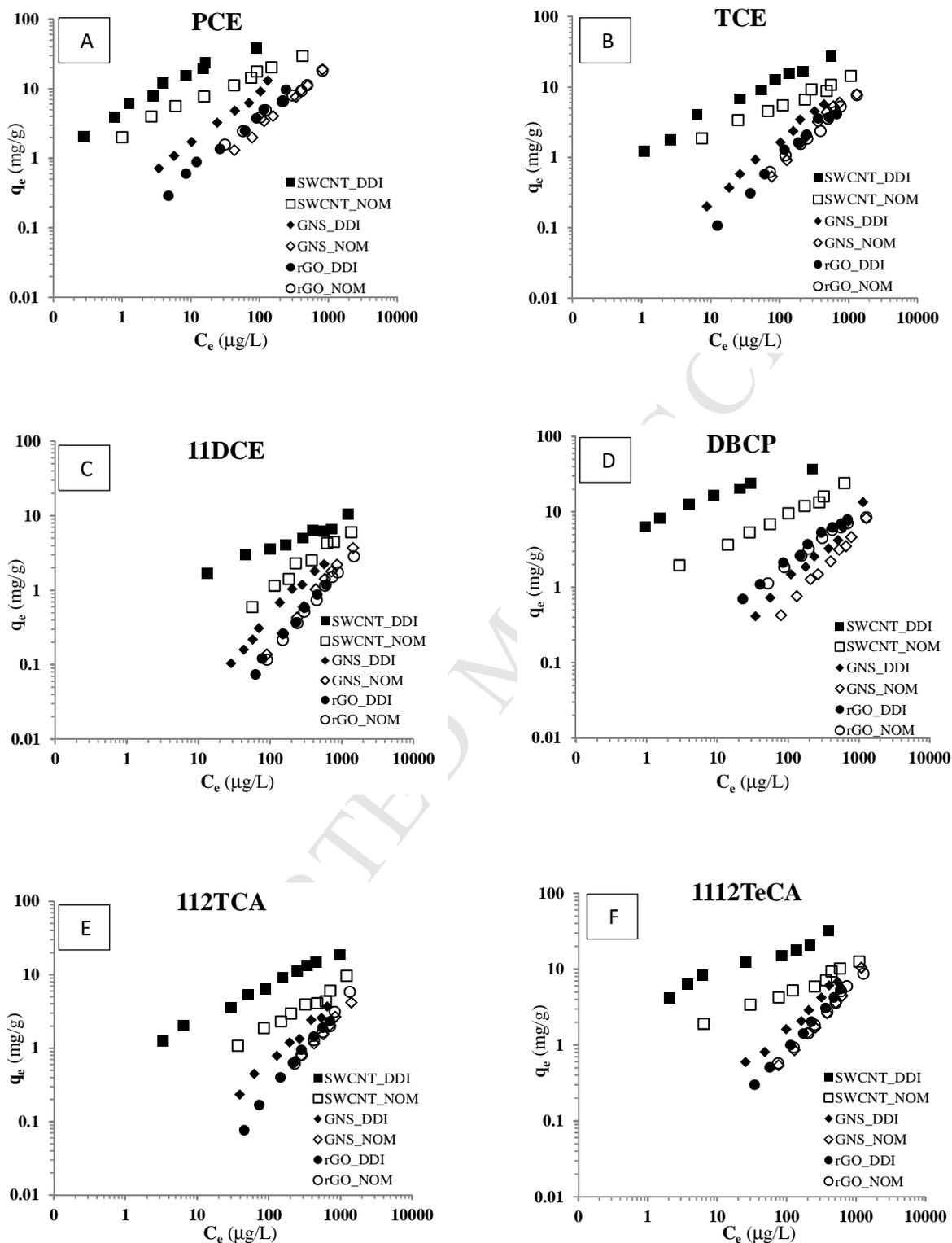


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561 **Figure 5.** Comparison of PCE vs. 1112TeCA and TCE vs. 112TCA solubility normalized adsorption  
 562 isotherms on GNS and rGO in DDW (A) PCE vs. 1112TeCA-GNS, (B) PCE vs. 1112TeCA-rGO, (C)  
 563 TCE vs. 112TCA-GNS, and (D) TCE vs. 112TCA- rGO.



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569 **Figure 6.** Adsorption isotherms in DDW and under NOM preloading conditions (A) PCE, (B) TCE, (C)  
 570 11DCE, (D) DBCP, (E) 112TCA, and (F) 1112TeCA.

**Highlights**

- Graphene nanomaterials adsorb halogenated aliphatic SOC<sub>s</sub>
- The effect of NOM was smaller on adsorption capacity of graphenes than CNT<sub>s</sub>
- rGO showed comparable adsorption capacities in NOM solution and DDW
- Hydrophobicity was the dominant factor in the adsorption of tested aliphatic SOC<sub>s</sub> by graphenes
- CNT<sub>s</sub> and GAC exhibited higher adsorption capacities for aliphatic SOC<sub>s</sub> than graphenes

1 SUPPORTING INFORMATION

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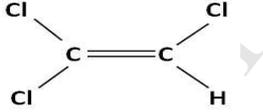
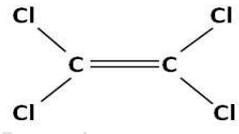
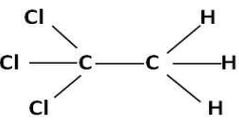
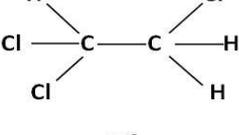
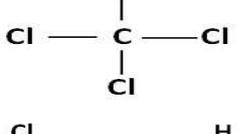
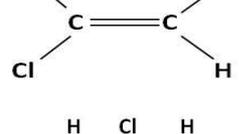
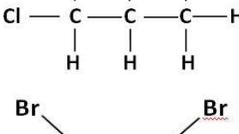
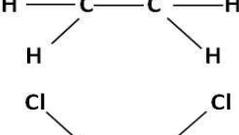
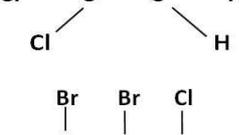
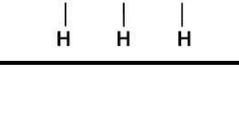
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7 **Adsorption of Halogenated Aliphatic Contaminants by Graphene**  
8 **Nanomaterials**

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12  
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24 \*Corresponding author: email: tkaranf@clemson.edu; phone: +1-864-656-1005; fax: +1-864-656-0672

**Table S1.** Molecular structures of selected aliphatic SOC's

SOC	Abbreviation	Molecular Structures
trichloroethylene	TCE	
tetrachloroethylene	PCE	
1,1,1-trichloroethane	111TCA	
1,1,2-trichloroethane	112TCA	
carbon tetrachloride	CCl <sub>4</sub>	
1,1-dichloroethylene	11DCE	
1,2-dichloropropane	12DCP	
1,2-dibromoethane	12DBE	
1,1,1,2-tetrachloroethane	1112TeCA	
1,2-dibromo-3-chloropropane	DBCP	

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**Table S2.** Nonlinear model fits for adsorption of ten aliphatic SOCs on GNS

SOC	Langmuir				Freundlich				Langmuir-Freundlich					Polanyi-Manes models				
	$q_m$	$K_L$	$r^2$	RMSE	$K_F$	n	$r^2$	RMSE	$q_m$	$K_S$	n	$r^2$	RMSE	$q_m$	a	b	$r^2$	RMSE
TCE	16.8	0.001	0.993	0.17	0.032	0.86	0.996	0.20	17.4	0.001	0.991	0.993	0.19	9.8	-24.7	1.26	0.993	0.19
CCl <sub>4</sub>	13.7	0.002	0.999	0.08	0.039	0.82	0.984	0.14	13.8	0.002	0.996	0.999	0.08	7.3	-29.1	1.28	0.999	0.08
PCE	129.2	0.001	0.976	0.74	0.287	0.75	0.995	0.65	<u>1370.4</u>	<u>4E-05</u>	<u>0.877</u>	0.981	0.72	65.5	-5.3	0.45	0.995	0.38
111TCA	13.2	0.001	0.989	0.15	0.005	1.09	0.982	0.17	7.1	0.002	1.223	0.991	0.14	5.3	-66.9	1.57	0.991	0.14
11DCE	10.1	0.001	0.994	0.06	0.003	1.05	0.990	0.08	5.1	0.001	1.180	0.996	0.06	4.1	-43.3	1.59	0.996	0.05
112TCA	35.5	2E-04	0.971	0.22	0.009	0.93	0.987	0.22	110.6	4E-05	0.948	0.972	0.24	48.6	-10.9	0.74	0.973	0.23
12DBE	<u>424.1</u>	<u>2E-05</u>	0.982	0.37	0.002	1.15	0.983	0.36	<u>424.1</u>	<u>2E-05</u>	<u>1.054</u>	0.984	0.38	13.1	-120.7	1.83	0.993	0.24
12DCP	<u>951.1</u>	<u>5E-06</u>	0.980	0.34	0.003	1.10	0.997	0.10	<u>951.2</u>	<u>1E-05</u>	<u>1.195</u>	0.998	0.12	27.2	-13.2	0.78	0.999	0.06
1112TeCA	45.8	3E-04	0.985	0.31	0.035	0.84	0.987	0.31	49.2	3E-04	0.993	0.985	0.34	12.7	-22.5	1.07	0.985	0.34
DBCp	<u>1905.4</u>	<u>6E-06</u>	0.974	0.68	0.017	0.92	0.985	0.48	<u>1905.5</u>	<u>1E-05</u>	<u>1.172</u>	0.987	0.52	20.0	-6.3	0.53	0.996	0.33

27  $q_m$  (mg/g): maximum adsorption capacity;  $K_L$ (L/ $\mu$ g): adsorption affinity coefficient;  $r^2$ : coefficient of determination; RMSE: residual root mean square error;  $K_F$  [(mg/g)/( $\mu$ g/L)<sup>n</sup>]:  
 28 adsorption affinity coefficient; n: nonlinear index;  $K_S$  [(L/ $\mu$ g)<sup>n</sup>]: adsorption affinity coefficient; a and b: fitting parameters; underlined numbers represent the unreasonable values of  
 29 the models.

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**Table S3.** Nonlinear model fits for adsorption of ten aliphatic SOC's on rGO

SOC	Langmuir				Freundlich				Langmuir-Freundlich					Polanyi-Manes models				
	$q_m$	$K_L$	$r^2$	RMSE	$K_F$	$n$	$r^2$	RMSE	$q_m$	$K_S$	$n$	$r^2$	RMSE	$q_m$	$a$	$b$	$r^2$	RMSE
<b>TCE</b>	8.7	0.001	0.974	0.26	0.011	0.95	0.984	0.34	5.5	0.003	1.430	0.981	0.24	4.6	-112.4	1.84	0.980	0.25
<b>CCl<sub>4</sub></b>	<u>93.0</u>	<u>6E-05</u>	0.992	0.09	0.014	0.82	0.992	0.08	<u>93.0</u>	<u>5E-05</u>	<u>0.961</u>	0.993	0.09	5.6	-8.3	0.70	0.998	0.04
<b>PCE</b>	38.8	0.001	0.963	0.66	0.096	0.82	0.989	0.64	<u>398.1</u>	<u>5E-05</u>	<u>0.860</u>	0.966	0.69	6.9	-26.4	1.19	0.995	0.28
<b>111TCA</b>	29.6	9E-05	0.972	0.10	0.001	1.13	0.991	0.10	2.1	0.003	1.860	0.982	0.09	2.0	-208.1	1.87	0.981	0.09
<b>11DCE</b>	<u>203.3</u>	<u>9E-06</u>	0.991	0.04	0.001	1.18	0.992	0.02	<u>203.3</u>	<u>2E-05</u>	<u>1.122</u>	0.997	0.03	3.8	-26.1	1.21	0.998	0.02
<b>112TCA</b>	<u>178.1</u>	<u>2E-05</u>	0.994	0.07	0.001	1.24	0.994	0.05	<u>178.1</u>	<u>3E-05</u>	<u>1.075</u>	0.997	0.06	5.9	-79.6	1.70	0.999	0.02
<b>12DBE</b>	<u>998.3</u>	<u>8E-06</u>	0.973	0.57	0.001	1.30	0.991	0.47	<u>998.3</u>	<u>1E-05</u>	<u>1.132</u>	0.982	0.50	17.7	-123.4	1.82	0.990	0.38
<b>12DCP</b>	<u>303.3</u>	<u>7E-06</u>	0.991	0.11	0.001	1.07	0.998	0.05	<u>303.3</u>	<u>1E-05</u>	<u>1.114</u>	0.998	0.05	7.5	-18.4	0.95	0.998	0.05
<b>1112TeCA</b>	<u>607.4</u>	<u>1E-05</u>	0.997	0.12	0.009	1.00	0.999	0.09	<u>607.4</u>	<u>2E-05</u>	<u>1.059</u>	0.998	0.10	13.4	-13.7	0.82	0.999	0.07
<b>DBCP</b>	13.6	0.002	0.993	0.23	0.078	0.72	0.990	0.34	14.0	0.002	0.981	0.993	0.25	8.7	-40.8	1.38	0.993	0.26

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**Table S4.** Nonlinear model fits for adsorption of ten aliphatic SOC<sub>s</sub> on HD3000

SOC	Langmuir				Freundlich				Langmuir-Freundlich					Polanyi-Manes models				
	q <sub>m</sub>	K <sub>L</sub>	r <sup>2</sup>	RMSE	K <sub>F</sub>	n	r <sup>2</sup>	RMSE	q <sub>m</sub>	K <sub>S</sub>	n	r <sup>2</sup>	RMSE	q <sub>m</sub>	a	b	r <sup>2</sup>	RMSE
<b>TCE</b>	32.0	0.017	0.982	0.91	1.300	0.61	0.994	0.53	<u>541.8</u>	<u>7E-05</u>	<u>0.641</u>	0.994	0.59	<u>193.1</u>	<u>-8.3</u>	<u>0.79</u>	0.994	0.56
<b>CCl<sub>4</sub></b>	14.6	0.011	0.960	0.88	0.680	0.51	0.986	0.88	21.6	0.004	0.678	0.970	0.83	14.1	-21.1	1.00	0.970	0.83
<b>PCE</b>	34.7	0.103	0.993	0.59	3.721	0.68	0.998	0.21	135.3	0.007	0.705	0.999	0.18	86.3	-17.3	1.65	0.999	0.17
<b>111TCA</b>	14.8	0.004	0.994	0.24	0.178	0.69	0.996	0.18	32.5	0.001	0.755	0.998	0.15	17.1	-20.2	1.25	0.998	0.15
<b>11DCE</b>	11.4	0.006	0.969	0.46	0.508	0.46	0.967	0.52	13.4	0.004	0.821	0.972	0.50	11.1	-36.3	1.86	0.971	0.50
<b>112TCA</b>	23.0	0.007	0.949	1.16	0.712	0.55	0.990	0.76	<u>311.7</u>	<u>3E-05</u>	<u>0.615</u>	0.977	0.87	<u>1244</u>	<u>-6.4</u>	<u>0.45</u>	0.942	1.39
<b>12DBE</b>	43.1	0.004	0.988	1.01	0.858	0.58	0.995	0.72	87.2	0.001	0.705	0.997	0.58	65.1	-16.7	1.36	0.996	0.62
<b>12DCP</b>	25.0	0.003	0.967	0.99	0.539	0.52	0.967	0.71	79.9	2E-04	0.607	0.984	0.76	29.5	-13.3	1.15	0.984	0.76
<b>1112TeCA</b>	36.4	0.009	0.980	1.39	1.444	0.52	0.995	0.82	65.4	0.002	0.633	0.999	0.27	37.8	-20.5	1.35	0.999	0.29
<b>DBCP</b>	51.2	0.078	0.984	1.62	6.118	0.53	0.994	1.52	78.7	0.025	0.704	0.995	0.96	76.7	-40.9	1.81	0.995	1.02

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**Table S5.** Nonlinear model fits for adsorption of ten aliphatic SOCs on SWCNT

SOC	Langmuir				Freundlich				Langmuir-Freundlich				Polanyi-Manes models					
	$q_m$	$K_L$	$r^2$	RMSE	$K_F$	$n$	$r^2$	RMSE	$q_m$	$K_S$	$n$	$r^2$	RMSE	$q_m$	$a$	$b$	$r^2$	RMSE
<b>TCE</b>	31.7	0.007	0.962	1.77	1.275	0.50	0.987	0.80	133.8	1E-04	0.499	0.993	0.82	35.2	-9.4	1.11	0.993	0.82
<b>CCl<sub>4</sub></b>	17.2	0.085	0.856	2.76	3.155	0.30	0.939	0.78	93.2	2E-05	0.297	0.988	0.86	21.8	-4.8	1.00	0.988	0.84
<b>PCE</b>	42.6	0.076	0.976	1.91	4.795	0.52	0.970	2.14	55.8	0.034	0.699	0.991	1.27	42.9	-31.6	1.65	0.991	1.27
<b>111TCA</b>	10.5	0.066	0.886	1.01	2.865	0.22	0.983	0.49	19.5	0.004	0.356	0.980	0.48	12.2	-8.6	1.38	0.980	0.05
<b>11DCE</b>	10.7	0.004	0.811	1.22	0.672	0.36	0.967	0.72	68.4	2E-05	0.456	0.927	0.82	60.0	-2.6	0.31	0.967	0.55
<b>112TCA</b>	21.8	0.005	0.983	0.81	0.751	0.48	0.993	0.71	34.2	0.001	0.654	0.996	0.40	25.5	-20.3	1.53	0.996	0.44
<b>12DBE</b>	20.2	0.034	0.862	2.85	2.461	0.36	0.942	0.96	141.8	2E-05	0.357	0.983	1.08	47.6	-4.9	0.93	0.984	1.04
<b>12DCP</b>	15.0	0.003	0.977	0.59	0.218	0.60	0.946	0.91	15.0	0.003	0.994	0.977	0.63	13.0	-88.2	1.99	0.976	0.64
<b>1112TeCA</b>	27.4	0.027	0.775	4.66	3.913	0.33	0.964	2.15	<u>250.4</u>	<u>1E-05</u>	<u>0.383</u>	0.947	2.47	<u>424.1</u>	<u>-3.2</u>	<u>0.27</u>	0.983	1.39
<b>DBCP</b>	35.3	0.102	0.918	3.30	7.373	0.32	0.971	1.66	54.9	0.019	0.493	0.998	0.51	42.2	-23.0	1.70	0.999	0.48

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**Table S6.** Freundlich isotherm parameters of aliphatic SOC's adsorption in DDW

SOC	Adsorbent	$K_{F\mu}^a$	$K_{Fm}^a$	$Q^b$	n	$r^2$
		(mg/g)/( $\mu$ g/L) <sup>n</sup>	(mg/g)/(mg/L) <sup>n</sup>	mg/m <sup>2</sup>		
<b>TCE</b>	SWCNT	1.2748	39.6	0.074	0.50	0.987
	HD3000	1.3002	87.9	0.137	0.61	0.994
	GNS	0.0320	12.3	0.018	0.86	0.996
	rGO	0.0110	7.7	0.015	0.95	0.984
<b>CCl<sub>4</sub></b>	SWCNT	3.1549	25.9	0.048	0.30	0.939
	HD3000	0.6800	22.6	0.035	0.51	0.986
	GNS	0.0392	11.5	0.017	0.82	0.984
	rGO	0.0139	4.1	0.008	0.82	0.992
<b>PCE</b>	SWCNT	4.7953	172.5	0.321	0.52	0.970
	HD3000	3.7205	416.1	0.648	0.68	0.998
	GNS	0.2871	52.8	0.079	0.75	0.995
	rGO	0.0955	27.2	0.055	0.82	0.989
<b>111TCA</b>	SWCNT	2.8651	13.2	0.025	0.22	0.983
	HD3000	0.1775	21.0	0.033	0.69	0.996
	GNS	0.0047	9.1	0.014	1.09	0.982
	rGO	0.0012	2.9	0.006	1.13	0.991
<b>11DCE</b>	SWCNT	0.6721	8.4	0.016	0.36	0.967
	HD3000	0.5080	12.2	0.019	0.46	0.967
	GNS	0.0033	4.7	0.007	1.05	0.990
	rGO	0.0006	2.2	0.004	1.18	0.992
<b>112TCA</b>	SWCNT	0.7508	21.1	0.039	0.48	0.993
	HD3000	0.7122	32.1	0.050	0.55	0.990
	GNS	0.0086	5.2	0.008	0.93	0.987
	rGO	0.0008	4.0	0.008	1.24	0.994
<b>12DBE</b>	SWCNT	2.4611	29.9	0.056	0.36	0.942
	HD3000	0.8581	47.8	0.074	0.58	0.995
	GNS	0.0023	6.6	0.010	1.15	0.983
	rGO	0.0012	9.0	0.018	1.30	0.991
<b>12DCP</b>	SWCNT	0.2183	13.7	0.025	0.60	0.946
	HD3000	0.5394	19.5	0.030	0.52	0.967
	GNS	0.0026	5.0	0.008	1.10	0.997
	rGO	0.0013	2.2	0.004	1.07	0.998
<b>1112TeCA</b>	SWCNT	3.9129	37.5	0.070	0.33	0.964
	HD3000	1.4443	51.1	0.080	0.52	0.995
	GNS	0.0350	11.2	0.017	0.84	0.987
	rGO	0.0085	8.8	0.018	1.00	0.999
<b>DBCP</b>	SWCNT	7.3732	69.3	0.129	0.32	0.971
	HD3000	6.1177	234	0.364	0.53	0.994
	GNS	0.0165	9.8	0.015	0.92	0.985
	rGO	0.0781	11.4	0.023	0.72	0.990

40 <sup>a</sup> Mass-basis adsorption affinity expressed in different units; <sup>b</sup> Surface area normalized adsorption capacity.

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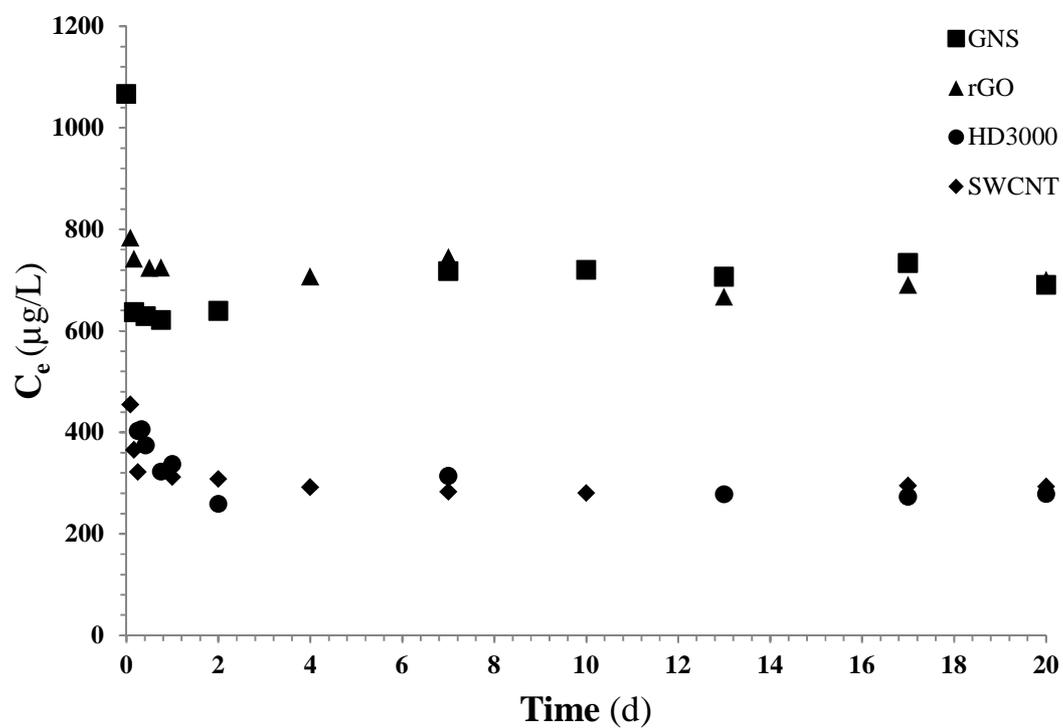
42 **Table S7.** Freundlich isotherm parameters of aliphatic SOCs adsorption in NOM preloading conditions

<b>SOC</b>	<b>Adsorbent</b>	<b><math>K_{F\mu}^a</math></b> (mg/g)/( $\mu$ g/L) <sup>n</sup>	<b><math>K_{Fm}^a</math></b> (mg/g)/(mg/L) <sup>n</sup>	<b><math>R_u^b</math></b>	<b><math>R_m^c</math></b>	<b>n</b>	<b>r<sup>2</sup></b>
<b>TCE</b>	SWCNT-DDW	1.2748	39.6	--	--	0.50	0.987
	SWCNT-NOM	0.8801	13.2	0.69	0.33	0.39	0.981
	GNS-DDW	0.0320	12.3	--	--	0.86	0.996
	GNS-NOM	0.0076	7.9	0.24	0.64	1.01	0.976
	rGO-DDW	0.0110	7.7	--	--	0.95	0.984
	rGO-NOM	0.0152	6.2	1.38	0.81	0.87	0.993
<b>PCE</b>	SWCNT-DDW	4.7953	172.5	--	--	0.52	0.970
	SWCNT-NOM	2.3521	45.5	0.49	0.26	0.43	0.990
	GNS-DDW	0.2871	52.8	--	--	0.75	0.995
	GNS-NOM	0.0446	21.8	0.16	0.41	0.90	0.990
	rGO-DDW	0.0955	27.2	--	--	0.82	0.989
	rGO-NOM	0.1377	19.5	1.44	0.72	0.72	0.993
<b>11DCE</b>	SWCNT-DDW	0.6721	8.4	--	--	0.36	0.967
	SWCNT-NOM	0.0341	5.4	0.05	0.64	0.73	0.976
	GNS-DDW	0.0033	4.7	--	--	1.05	0.990
	GNS-NOM	0.0006	2.6	0.18	0.55	1.21	0.997
	rGO-DDW	0.0006	2.2	--	--	1.18	0.992
	rGO-NOM	0.0006	2.0	1.00	0.91	1.17	0.997
<b>112TCA</b>	SWCNT-DDW	0.7508	21.1	--	--	0.48	0.993
	SWCNT-NOM	0.1372	7.1	0.18	0.34	0.57	0.967
	GNS-DDW	0.0086	5.2	--	--	0.93	0.987
	GNS-NOM	0.0022	2.9	0.26	0.56	1.04	0.995
	rGO-DDW	0.0008	4.0	--	--	1.24	0.994
	rGO-NOM	0.0007	3.6	0.88	0.90	1.24	0.983
<b>1112TeCA</b>	SWCNT-DDW	3.9129	37.5	--	--	0.33	0.964
	SWCNT-NOM	0.9489	11.4	0.24	0.30	0.36	0.977
	GNS-DDW	0.0350	11.2	--	--	0.84	0.987
	GNS-NOM	0.0050	7.7	0.14	0.68	1.06	0.994
	rGO-DDW	0.0085	8.8	--	--	1.00	0.999
	rGO-NOM	0.0074	7.4	0.87	0.84	1.00	0.994
<b>DBCP</b>	SWCNT-DDW	7.3732	69.3	--	--	0.32	0.971
	SWCNT-NOM	1.1402	27.0	0.15	0.39	0.46	0.994
	GNS-DDW	0.0165	9.8	--	--	0.92	0.985
	GNS-NOM	0.0048	6.0	0.29	0.61	1.03	0.996
	rGO-DDW	0.0781	11.4	--	--	0.72	0.990
	rGO-NOM	0.1008	8.8	1.29	0.77	0.65	0.975

43 <sup>a</sup> Mass-basis adsorption affinity expressed in different units; <sup>b</sup>  $K_F$  ratio of SOCs in NOM preloading adsorption to that in  
44 DDW at equilibrium concentration of 1 $\mu$ g/L; <sup>c</sup>  $K_F$  ratio of SOCs in NOM preloading adsorption to that in DDW at  
45 equilibrium concentration of 1mg/L.

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**Figure S1.** Adsorption kinetics of TCE onto GNS, rGO, HD3000 and SWCNT in DDW.

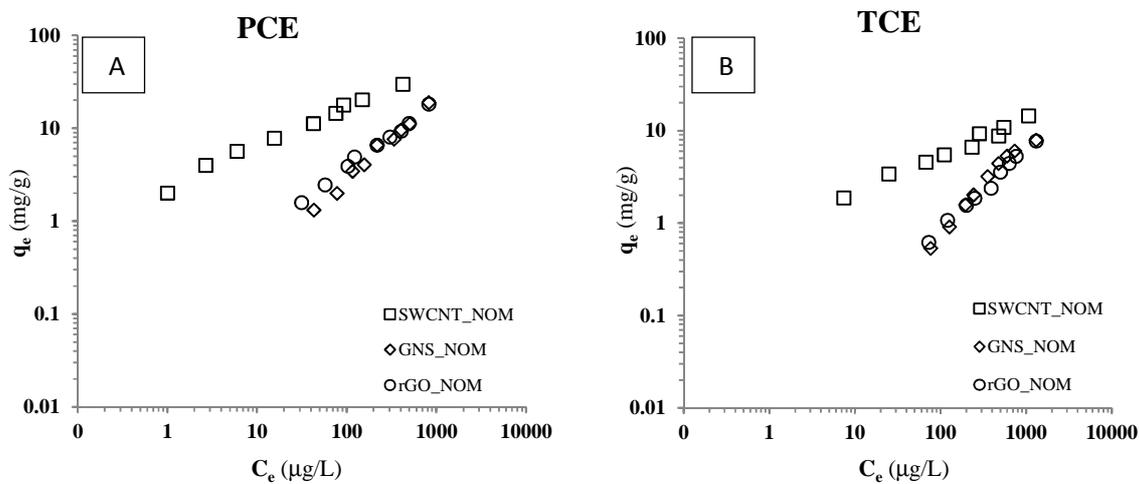
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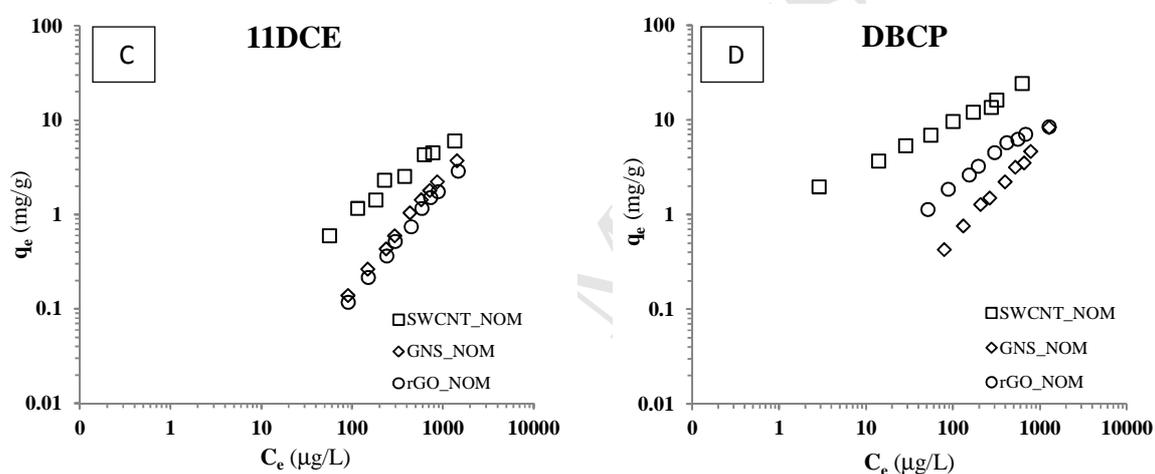
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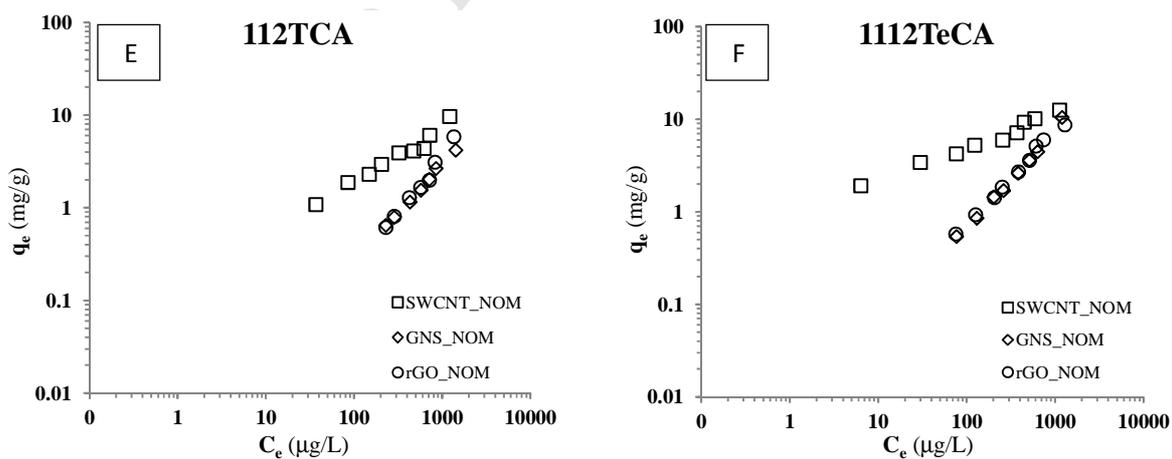
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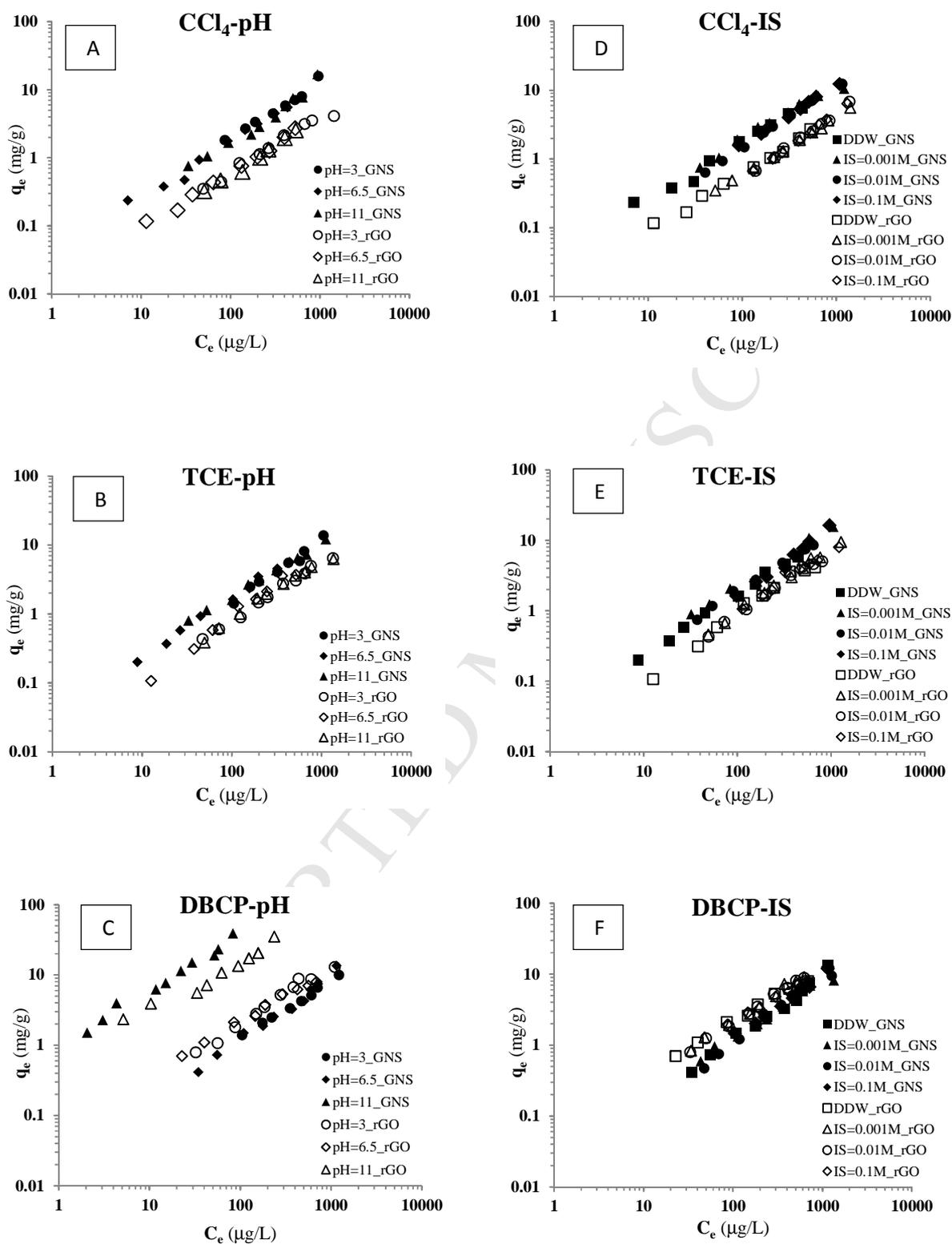
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58 **Figure S2.** Adsorption isotherms under NOM preloading conditions (A) PCE, (B) TCE, (C) 11DCE, (D)  
 59 DBCP, (E) 112TCA, and (F) 1112TeCA.

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66 **Figure S3.** Adsorption isotherms in different solution pH and IS (A)  $\text{CCl}_4$ -pH, (B) TCE-pH, (C) DBCP-  
 67 pH, (D)  $\text{CCl}_4$ -IS, (E) TCE-IS, and (F) DBCP-IS.