

Magnetic composites Fe₃O₄@SiO₂@PILs as sorbents for efficient denitrogenation of fuel oil

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In this work, the study of synthesis and denitrogenation of magnetic polymeric ionic liquids (PILs) for N-compounds in simulated oils and diesel are reported. Three functionalised magnetic particles, Fe₃O₄@SiO₂@PILs with side alkyl chain of C2, C4 and C6, respectively, were prepared by grafting PILs on the surface of silica-coated Fe₃O₄. Fourier transform infrared spectra, thermogravimetric analysis, X-ray diffraction and scanning electron microscopy were carried out to characterise the structure of Fe₃O₄@SiO₂@PILs. It has shown that Fe₃O₄@SiO₂@PILs possess precious merits for sorbents, such as regular morphology, good stability and magnetic properties. Denitrogenation experiments of simulated oils demonstrate that Fe₃O₄@SiO₂@PILs show better denitrogenation efficiency of basic N-compounds than neutral N-compounds. The effects of temperature, reaction times, ratio of reagent to oil on denitrogenation for simulated oils were explored, and 92.1% denitrogenation efficiency was obtained to remove quinoline from simulated oils. Denitrogenation of Fe₃O₄@SiO₂@PILs in diesel leads to 84.3% denitrogenation efficiency, and it can remain 82.5% denitrogenation efficiency after five times of recycles. Compared with other similar sorbents, Fe₃O₄@SiO₂@PILs show competitive performances to eliminate organic N-compounds. It is hopeful that Fe₃O₄@SiO₂@PILs can be promising sorbents for purification of liquid fuel by adsorptive denitrogenation.

1. Introduction: N-compounds in fuel can be changed into NO_x during combustion which has an incalculable impact on the environment [1–3]. In addition, in the process of hydrodesulphurisation, N-compounds will reduce the thermal and oxidative stability of diesel. Therefore, denitrogenation from oils have attracted extensive attentions of both academic and industrial communities.

Hydrodenitrogenation (HDN) is an effective and widely used technology for the elimination of N-compounds in petroleum refining processes [4, 5]. However, HDN process requires tough operating conditions (such as noble catalyst, high pressure and high temperature). Adsorptive denitrogenation (ADN) [6–8] is the alternative method to the elimination of N-compounds from oils with high removal capacity, convenient operation, low cost and possibility of materials recycling. Activated carbon [9, 10], molecular surface imprinted polymers [11, 12], microporous or mesoporous materials [13–15] and metal–organic frameworks materials [16–18] are reported as ADN sorbent in recent years.

Ionic liquids (ILs) [19, 20] which are composed of an organic cation and an inorganic or organic anion were applied in the area of denitrogenation. Wang and co-workers [21] utilised [Bmim]Cl/ZnCl₂ in extraction of denitrogenation with an efficiency of 93.8% (carbazole) and 98% (pyridine), respectively. Maschmeyer and his co-workers [22] applied various ILs based on common cations and anions as extractants to study the denitrogenation of pyridine and indole from a simulated oil. The results demonstrated that the sizes of cation and anion are the major factors to the efficiency of N-compound extraction. Liu *et al.* [23] researched the denitrogenation efficiency of H₂PO₄⁻-based IL to the simulated oils, and the mechanism of denitrification ascertained that a liquid–liquid extraction as well as the acidity of ILs both contribute to denitrogenation. Polymeric ionic liquids (PILs) [24–26], assembled by connecting IL species in their repeated units of polymer chains, can be functionalised with unique properties, such as designable structure, strong polarity, adjustable physico-chemical properties, thermal and chemical stability, which is suitable for the promising candidates as sorbents of denitrogenation. However, it is difficult to recycle the powdered adsorbents after treatment.

Magnetic solid phase adsorption (MSPA) [27, 28] is a novel simple and effective method for sample purification due to their properties of easy automatic operation and low consumption of organic reagents. Sun and co-workers [29] prepared magnetic HKUST-1/Fe₃O₄ composites to remove the N-compounds in fuel, which showed that the adsorbents had a high adsorptive capacity of 0.89 mmol/g N in indole. Afzalnia and his colleagues [30] synthesised Fe₃O₄@TMU-17-NH₂ as sorbent for highly efficient ultrasonic-assisted denitrogenation of fossil fuel. The maximum adsorption capacity of the synthesised composite to indole and quinoline is calculated by 375.93 and 310.18 mg/g at 25°C, respectively.

In this work, magnetic sorbents, MSPA-coupled PILs, were proposed for the denitrogenation of N-compounds. PILs were prepared on the surface of silica-core shell Fe₃O₄ which was modified by 3-mercaptopropyltrimethoxysilane (MPTMS) for MSPA. The sorbents were applied for rapid separation of N-compounds from the simulated oils and real oils.

2. Experimental section

2.1. Materials: All chemical reagents were used without any further purification (Table 1). 1-Vinylimidazole, 1,2-dibromoethane, 1,4-dibromobutane, 1,6-dibromohexane, quinoline, indole, sodium acetate and acetonitrile were purchase from Shanghai Aladdin. FeCl₃·6H₂O, ethyl acetate, azobisisobutyronitrile (AIBN), carbazole, FeCl₂·4H₂O, MPTMS, tetraethoxysilane (TEOS) and pyridine were purchased from Macklin Reagent.

2.2. Characterisation: ¹H NMR and ¹³C NMR spectra were recorded by a Varian MERCURY Plus-400 MHz spectrometer. Fourier transform infrared spectra were carried out on Nicolet 6700 spectrometer. X-ray diffractometer with Cuka radiation was used to record the structural characteristics of the adsorbents. Thermal gravimetric analysis (TG) was performed with a SII TG/DTA 6300. The microstructure of nanomaterials was observed by scanning electron microscopy (SEM, Hitachi TM 3000). Magnetic hysteresis was carried out on a quantum design

Table 1 Reagents and chemicals

Chemicals	Purity level, %	CAS number
1-vinylimidazole	99.9	1072-63-5
1,2-dibromoethane	99	1106-93-4
1,4-dibromobutane	98	1110-52-1
1,6-dibromohexane	97	6629-03-8
indole	99.5	775-05-8
MPTMS	95	4420-74-0
quinoline	99	91-22-5
AIBN	99	78-67-1
FeCl ₃ ·6H ₂ O	98	10025-77-1
FeCl ₂ ·4H ₂ O	99.9	13478-10-9
TEOS	98	681-84-5
carbazole	99	127-09-3
pyridine	99.5	67-64-1

superconducting quantum interference device magnetometer. Nitrogen content was measured by TN-3000 series nitrogen analyser.

2.3. Preparation of Fe₃O₄@SiO₂@PILs

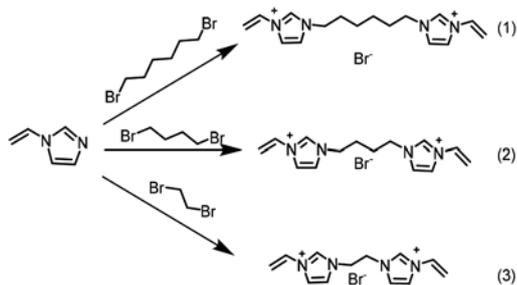
2.3.1. Synthesis of bis-vinyl imidazolium dibromide salts: The bis-vinyl imidazolium dibromide salts were synthesised via the reaction of 1-vinylimidazole (0.5 mol) and 1,2-dibromoalkane (0.25 mol) dissolved in 100 ml acetonitrile at 80°C for 48 h (Fig. 1). The product was washed with diethyl ether and ethyl acetate three times and then dried under dynamic vacuum at room temperature for 24 h at 40°C.

1,6-bis(1-vinylimidazolium)hexane bromide (1): ¹H-NMR (400 MHz, D₂O) δ 7.66 (d, 2H), 7.47 (d, 2H), 7.03 (dd, 2H), 5.69 (dd, 2H), 5.31 (dd, 2H), 4.13 (t, 4H), 1.79 (p, 4H), 1.26 (p, 4H). ¹³C-NMR (101 MHz, D₂O) δ 134.29, 128.23, 122.84, 119.48, 109.31, 49.79, 28.89, 24.85.

1,4-bis(1-vinylimidazolium)butane bromide (2): ¹H-NMR (400 MHz, D₂O) δ 7.64 (d, 2H), 7.44 (d, 2H), 6.99 (dd, 2H), 5.71–5.61 (m, 2H), 5.32–5.24 (m, 2H), 4.16 (d, 4H), 1.82 (q, 4H). ¹³C-NMR (101 MHz, D₂O) δ 134.39, 128.10, 122.64, 119.60, 109.41, 49.01, 25.99.

1,2-bis(1-vinylimidazolium)ethane bromide (3): ¹H-NMR (400 MHz, D₂O) δ 7.74 (d, 2H), 7.47 (d, 2H), 7.03 (dt, 2H), 5.71 (dd, 2H), 5.39–5.31 (m, 2H), 4.74 (d, J = 1.9 Hz, 4H). ¹³C-NMR (101 MHz, D₂O) δ 134.89, 127.95, 122.74, 120.43, 110.42, 48.85.

2.3.2. Preparation of Fe₃O₄: Fe₃O₄ was prepared as reported method [27]. In short, 5.41 g FeCl₃·6H₂O and 1.98 g FeCl₂·4H₂O were dissolved in 50 ml deionised water, then 2 ml of hydrazine hydrate and 10 ml of 30% ammonia were successively added to the system. The mixture was heated to 90°C by stirring for 1 h, and 4.2 g of sodium acetate was added for further stirring for

**Fig. 1** Synthesis routes of bis-vinyl imidazolium dibromide salts

10 min. The product was collected via magnetic separation and washed with water and acetone for several times.

2.3.3. Preparation of Fe₃O₄@SiO₂-SH: Fe₃O₄@SiO₂-SH was prepared by sequential silylanisation on the surface of Fe₃O₄. The mixture of 5 g Fe₃O₄, 10 ml TEOS and 20 ml MPTMS was stirred for 8 h at room temperature. The Fe₃O₄@SiO₂-SH was collected by a magnet, and the residual reactants were removed by ultrasonic washing with water for several times and then dried under vacuum at 40°C overnight.

2.3.4. Preparation of Fe₃O₄@SiO₂@PILs: Fe₃O₄@SiO₂@PILs were prepared as the method reported in the literature [31]. Shortly, Fe₃O₄@SiO₂-SH (5 g), the bis-vinyl imidazolium salt (27.5 mmol), AIBN (0.2 g) and 200 ml of ethanol were added in a three-necked round bottom flask. The mixture was stirred for 48 h at 80°C under nitrogen atmosphere. The obtained composite was washed with methanol and diethyl ether, respectively.

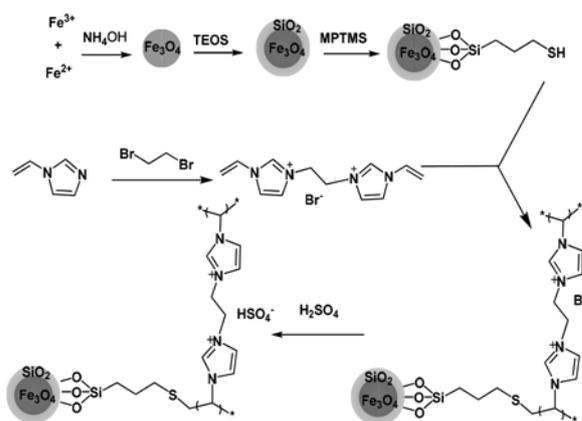
The above composite was dispersed in 10 ml of water, and 2 ml of H₂SO₄ was added into the mixtures by keeping the mixture in a low temperature. The reaction was carried on for 24 h by stirring at room temperature. Then Fe₃O₄@SiO₂@PILs were separated and washed by water to remove H₂SO₄, dried in an oven at 60°C overnight (Fig. 2).

2.4. Adsorption procedure: In adsorption study, simulated oils were composed by dissolving a certain amount of N-compound (such as quinoline, pyridine, indole and carbazole) in a mixing solution of toluene (80 wt. %) and n-heptane (20 wt. %), respectively. Real fuel was provided by Sinopec Zhenhai Refining & Chemical Company, with a content of 250 ppm nitrogen element (wt.).

About 0.5 g of Fe₃O₄@SiO₂@PILs was added to 5.0 ml of simulated oils, and the mixture was stirred to reach adsorption balance. After the adsorption completed, the Fe₃O₄@SiO₂@PILs was separated from oils solution by an external magnetic field and the nitrogen content of the simulated oils was measured by TN-3000 series nitrogen analyser. The efficiency of extraction *E*(%) was determined according to (1), where *c_i* and *c_f* are the abbreviation of initial and final concentrations in the studied molecule, respectively

$$E(\%) = \frac{c_i - c_f}{c_i} \times 100 \quad (1)$$

The regeneration of Fe₃O₄@SiO₂@PILs can be managed in the common regeneration process of ILs. In brief, after completion of denitrogenation, Fe₃O₄@SiO₂@PILs were separated by magnet and then washed by ethyl acetate and water, each for five times,

**Fig. 2** Preparation process of Fe₃O₄@SiO₂@PILs

respectively. Finally, $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PILs}$ were added to the aqueous solution of sulphuric acid for regeneration.

3. Results and discussion

3.1. Characterisation of $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PILs}$: Fig. 3 demonstrated the FTIR spectra of Fe_3O_4 , $\text{Fe}_3\text{O}_4@\text{SiO}_2\text{-SH}$ and $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PILs}$. The peaks at 590 and 1086 cm^{-1} are attributed to the stretching vibrations of Fe–O bond and Si–O bond, respectively. The peak of 2420 cm^{-1} corresponds to the SH stretching vibration. The acidic counter-anion HSO_4^- appears at the position of 1203 and 1149 cm^{-1} , respectively, verifying the asymmetric and symmetric stretching vibration of O=S=O [32]. The peak of 850 cm^{-1} assigned to the C–H in-plane vibration of imidazolium ring. The C–H bond of the alkyl chain in the imidazolium ring appears at 2800–3000 cm^{-1} for $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_2$, $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_4$ and $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_6$, respectively, indicating that, with the increase of the base chain, the stretching vibration peak of methylene of alkyl chain appears gradually obvious.

The thermogravimetric analysis (TGA) curves are illustrated in Fig. 4. The weight loss process can be classified into three stages: the first stage was from 30 to 200°C, mainly resulted from the moisture evaporation on the surface of the hygroscopicity of these composites. The second stage was in the range of 200–380°C, where the weight loss may be caused by the decomposition of the ILs with the sulfhydryl group and double bond polymerisation, therefore the loading capacity of PILs in $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PILs}$ is calculated by 15–20% which is in line with the estimated value according to the reactions. The third stage was from 380 to 800°C, which can be attributed to the Fe_3O_4 changes to Fe_2O_3 in phase transfer and the decomposition of SiO_2 . The TGA analysis demonstrates that the synthesised $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PILs}$ can be stable at normal circumstances for practical application.

Fig. 5 shows the magnetisation curves of Fe_3O_4 , $\text{Fe}_3\text{O}_4@\text{SiO}_2\text{-SH}$ and $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PILs}$. The saturation magnetisation of Fe_3O_4 is

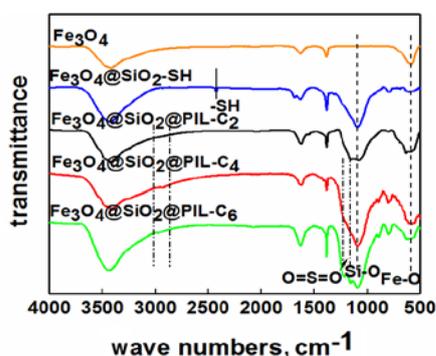


Fig. 3 FTIR spectra of Fe_3O_4 , $\text{Fe}_3\text{O}_4@\text{SiO}_2\text{-SH}$ and $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PILs}$

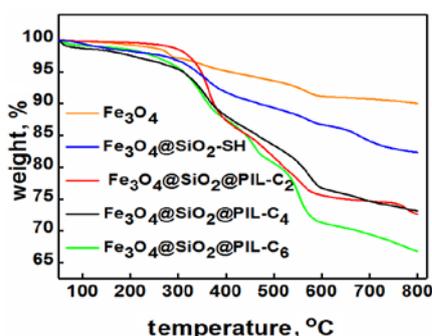


Fig. 4 TGA curves of Fe_3O_4 , $\text{Fe}_3\text{O}_4@\text{SiO}_2\text{-SH}$ and $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PILs}$

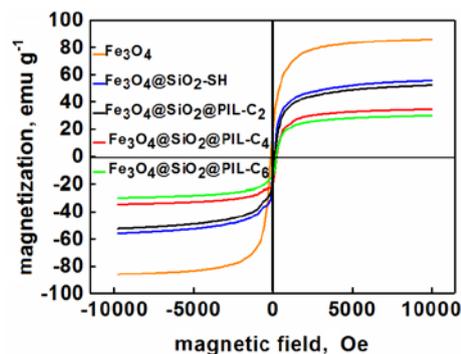


Fig. 5 Magnetic hysteresis curves of Fe_3O_4 , $\text{Fe}_3\text{O}_4@\text{SiO}_2\text{-SH}$, $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PILs}$

86.1 emu g^{-1} , and saturation magnetisation decreases with the increase of the modified molecules. The saturation magnetisation of $\text{Fe}_3\text{O}_4@\text{SiO}_2\text{-SH}$, $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_2$, $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_4$ and $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_6$ were 55.8, 52.4, 34.6 and 30.0 emu g^{-1} , respectively, which reveals that the magnetism of the magnetic composites is sufficient for the magnetic separation.

The X-ray diffraction (XRD) patterns of Fe_3O_4 , $\text{Fe}_3\text{O}_4@\text{SiO}_2\text{-SH}$ and MP were illustrated in Fig. 6. All the diffraction peaks verify the cubic inverse spinel Fe_3O_4 , which indicates that the Fe_3O_4 particles are encapsulated in cages of PILs. Therefore, the preparation of the expected composite was confirmed by XRD studies.

The SEM images were used to illustrate the morphologies of the prepared composites. As shown in Fig. 7, both Fe_3O_4 and $\text{Fe}_3\text{O}_4@\text{SiO}_2\text{-SH}$ have spherical nanoparticles structure in average size of 40 and 230 nm, respectively, while $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PILs}$ are ultrafine particles in diameter of 30–50 μm . The size of the three composites is in the order of $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_4 > \text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_6 > \text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_2$, which complies to the fact that the PILs size changes slightly with the increasing of the alkyl chain length connected on the imidazole ring.

3.2. Denitrogenation efficiency of different N-compounds: The comparison of denitrogenation efficiency to different N-compounds in simulated oils is shown in Table 2. It can be seen from Table 2 that the synthesised adsorbents perform better denitrogenation efficiency of basic N-compounds than that of neutral N-compounds.

The possible mechanism (Fig. 8) is assumed that H^+ from the ionisation of HSO_4^- anions ILs can attack lone pair of electrons of N in the quinoline molecule to form charged ions to accelerate the transfer of quinoline from oil phase into aqueous phase, which agrees to the denitration mechanism of H_2PO_4^- anion imidazolium-based ILs in the literature [22, 23, 30]. On the other hand, the π - π interactions between quinoline and PILs may also

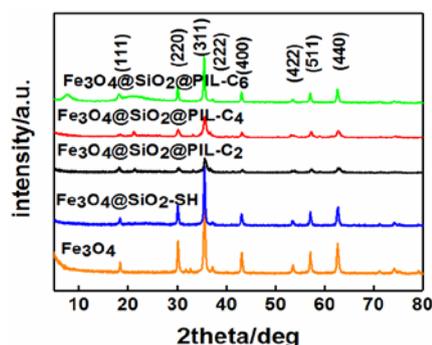


Fig. 6 XRD spectra of Fe_3O_4 , $\text{Fe}_3\text{O}_4@\text{SiO}_2\text{-SH}$ and $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PILs}$

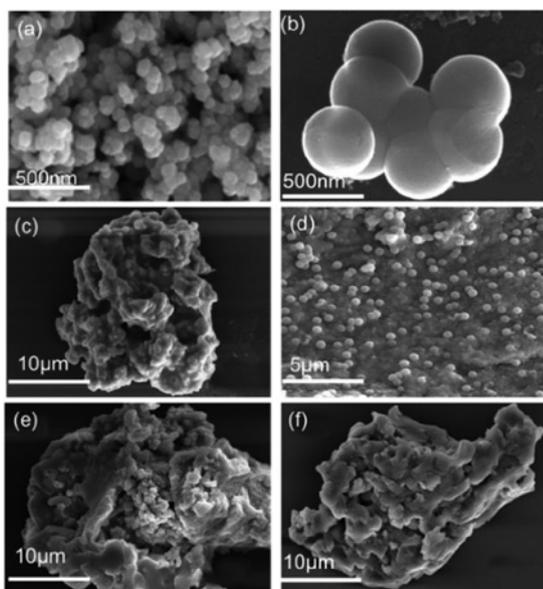


Fig. 7 SEM images of
 a Fe_3O_4
 b $\text{Fe}_3\text{O}_4@\text{SiO}_2\text{-SH}$
 c $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_2$
 d Section of $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_2$
 e $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_4$
 f $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_6$

Table 2 Denitrogenation efficiency of different N-compounds in simulated oils

Sorbent	Denitrogenation efficiency, %			
	Quinoline	Pyridine	Indole	Carbazole
$\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_2$	84.45	80.28	32.48	28.47
$\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_4$	84.16	79.16	30.87	24.15
$\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_6$	83.73	77.18	27.04	22.08

Denitrogenation conditions: adsorbent concentration 250 ppm, ratio of adsorbent to oil 1:10 (w/w), reaction time 5 min, temperature 25°C.

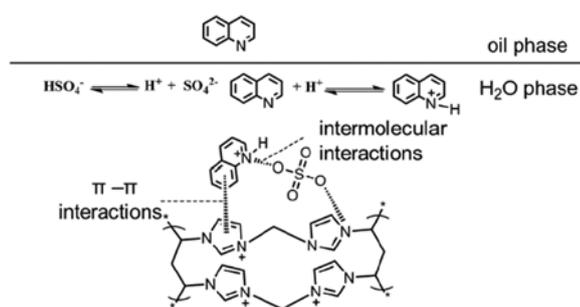


Fig. 8 Possible mechanism of adsorption denitrification of simulated oil with $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PILs}$

play a positive role in the denitrogenation efficiency. A possible denitrogenation mechanism is shown in Fig. 8.

3.3. Effect of temperature on denitrogenation: The effect of adsorption temperature on the denitrification rate, with 1:10 of the ratio of reagent to oil (w: w) for 5 min, is described in Fig. 9.

Fig. 9 demonstrates that $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_2$ has the highest denitrogenation efficiency in the three synthesised sorbents, and

that the denitrogenation efficiency can be reduced with the increase of reaction temperature, ranging from 84.5 to 82.1% with the temperature rising from 30 to 70°C. The results interpret that the denitrogenation progress of ILs is an exothermic reaction, and high temperature will impact the activity of sorbent.

3.4. Effect of the ratio of sorbent on denitrogenation: The results of the ratio of sorbent to oil at 30°C and 5 min of reaction time are shown in Fig. 10. We can see that the denitrogenation efficiency of $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_2$ decreases from 92.1 to 78.9% with the ratio decreased from 1:5 to 1:25, respectively. Similar results are observed for $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_4$ and $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_6$. This can be contributed by the increase of $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PILs}$ adsorption capacity to the N-compounds in diesel with the enhancement of the ratio of sorbent to oil.

3.5. Effect of reaction time on denitrogenation: Fig. 11 shows the effect of reaction time on denitrogenation at 30°C with a ratio of 1:5 sorbent to oil (w: w). The results in Fig. 11 indicate that the denitrogenation efficiency of $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_2$ increases from 88.7 to 92.1% when the reaction time increases from 5 to 20 min, and that the denitrogenation rate may not show any obvious improvement for further adsorption time. Hence, a preferable adsorption time is 10 min.

As reported results in the literature, 95.9% of denitrogenation efficiency to quinoline was achieved by a non-magnetic IL formulated as $[\text{C}_4\text{mim}]\text{HSO}_4$ [33], while the denitrogenation efficiency of $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PIL-C}_2$ to quinoline in this work is equally high up to 92.1%. Nevertheless, the magnetic composite proposed in this work possesses the advantage of simple and speed operation, and it can be easy to realise automation. It is obvious that a promising sorbent for denitrogenation to the N-compounds was developed in this work, especially for the basic N-compounds.

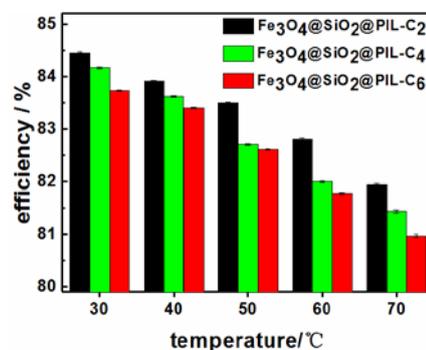


Fig. 9 Effect of isotherms on denitrogenation rate over $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PILs}$

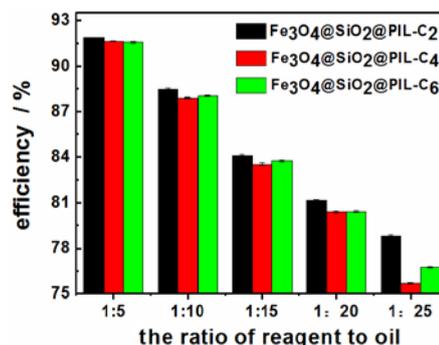


Fig. 10 Effect of the ratio of sorbent to oil on denitrogenation rate over $\text{Fe}_3\text{O}_4@\text{SiO}_2@\text{PILs}$

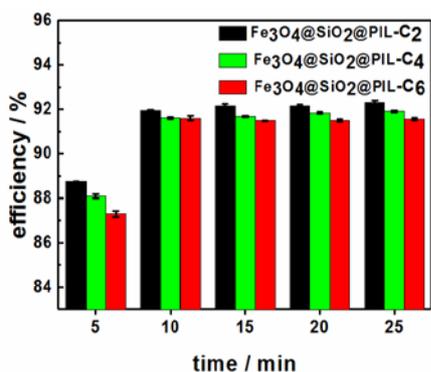


Fig. 11 Effect of reaction time on denitrogenation rate over $Fe_3O_4@SiO_2@PILs$

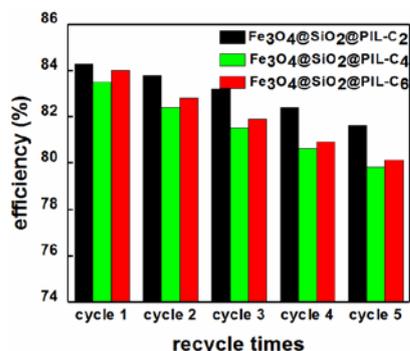


Fig. 12 Effect of recycle times on denitrogenation rate over $Fe_3O_4@SiO_2@PILs$

3.6. Effect of recycle times on denitrogenation of diesel: Based on the denitrogenation efficiency to quinoline in simulated oils, the denitrogenation experiments of the synthesised sorbents to diesel were carried out in the optimum denitrogenation conditions. Under the condition of temperature 30°C, the ratio of sorbent to oil (w: w) 1:5 with 5 min reaction time, the effect of recycle times on denitrogenation efficiency of diesel is shown in Fig. 12.

Fig. 12 demonstrated that with the cycle time increased, the denitrogenation efficiency of $Fe_3O_4@SiO_2@PIL-C_2$ slightly decreased from 84.3 to 82.5%, which is much lower than the results of simulated oils in 92.1% denitrogenation efficiency. Both $Fe_3O_4@SiO_2@PIL-C_4$ and $Fe_3O_4@SiO_2@PIL-C_6$ show the same consequence with the cycle times. This can be explained by two reasons, one is that there are some amounts of neutral N-compounds in the diesel which cannot be adsorbed well by the sorbents, and the other is the complexity composition of real oils which may be adsorbed on the surface of $Fe_3O_4@SiO_2@PILs$ leading to decrease the sorbents effect.

4. Conclusions: The synthesis and denitrogenation of magnetic PILs to N-containing oils were investigated. $Fe_3O_4@SiO_2@PILs$ were synthesised by grafting PILs on the surface of silica-coated Fe_3O_4 . Structural characterisation shows that $Fe_3O_4@SiO_2@PILs$ possess regular morphology, good stability and magnetic properties. $Fe_3O_4@SiO_2@PILs$ perform better denitrogenation efficiency of basic N-compounds than that of neutral N-compounds, and the shorter side alkyl chain in $Fe_3O_4@SiO_2@PILs$ will benefit the denitrogenation efficiency than the longer ones. The effects of temperature, reaction times, ratio of reagent to oil on denitrogenation for simulated oils and diesel were discussed. Denitrogenation efficiency of 92.1% to the simulated oils and 84.3% to diesel were achieved under the optimum condition. In

addition, $Fe_3O_4@SiO_2@PILs$ can be used at least for five times without significant decreased of denitrogenation efficiency, which provides a more convenient recycling method with low consumption. It is suggested that magnetic PILs have a potential application in denitrogenation process as environment-friendly sorbent.

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