

Article

Entropy Generation in Flow of Highly Concentrated Non-Newtonian Emulsions in Smooth Tubes

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Abstract: Entropy generation in adiabatic flow of highly concentrated non-Newtonian emulsions in smooth tubes of five different diameters (7.15–26.54 mm) was investigated experimentally. The emulsions were of oil-in-water type with dispersed-phase concentration (ϕ) ranging from 59.61–72.21% vol. The emulsions exhibited shear-thinning behavior in that the viscosity decreased with the increase in shear rate. The shear-stress (τ) versus shear rate ($\dot{\gamma}$) data of emulsions could be described well by the power-law model: $\tau = K\dot{\gamma}^n$. The flow behavior index n was less than 1 and it decreased sharply with the increase in ϕ whereas the consistency index K increased rapidly with the increase in ϕ . For a given emulsion and tube diameter, the entropy generation rate per unit tube length increased linearly with the increase in the generalized Reynolds number (Re_n) on a log-log scale. For emulsions with $\phi \leq 65.15$ % vol., the entropy generation rate decreased with the increase in tube diameter. A reverse trend in diameter-dependence was observed for the emulsion with ϕ of 72.21% vol. New models are developed for the prediction of entropy generation rate in flow of power-law emulsions in smooth tubes. The experimental data shows good agreement with the proposed models.

Keywords: emulsion; non-Newtonian; power law; entropy generation; pipeline flow; exergy destruction

PACS Codes: 5; 47; 82

1. Introduction

According to the Gouy-Stodola theorem, the rate of loss of work or available energy in a process is directly proportional to the total rate of entropy generation within and outside the control volume. The Gouy-Stodola theorem is expressed mathematically as [1]:

$$\dot{W}_{lost} = T_o \dot{S}_{G,total} \quad (1)$$

where \dot{W}_{lost} is the rate of lost work, T_o is the surroundings temperature, and $\dot{S}_{G,total}$ is the total rate of entropy generation within and outside the control volume. The greater the rate of entropy generation due to internal and external irreversibilities, the greater is the amount of energy that becomes unavailable for work [2–4]. Thus, it is important from a practical point of view to estimate the rate of entropy generation in a process in order to determine the thermodynamic efficiency of the process.

This article is related to entropy generation in flow of highly concentrated non-Newtonian emulsions of oil-in-water type in smooth tubes. The oil-in-water (designated as O/W) emulsions consist of oil droplets dispersed in a continuum of aqueous phase. Such emulsions are very important industrially [5]. For example, a large number of skincare and makeup creams marketed today are in the form of O/W emulsions. One important function of these creams is to prevent dryness of skin by replacing lost moisture and by keeping the skin hydrated over a period of time. The O/W emulsions are of considerable importance in the food industry as well. Examples of food emulsions (O/W type) are: milk, mayonnaise, coffee whiteners, and salad dressings. The dispersed-phase (oil droplets) concentration of food emulsions could range from low to very high. For example, milk consists of 3–4 volume percent of dispersed-phase whereas mayonnaise consists of more than 65 volume percent dispersed phase (oil droplets). The pipeline transportation of highly viscous crude oils in the form of O/W emulsions has also received special attention in recent years [6–8]. The transportation of highly viscous crude oils, such as bitumen and heavy oils, by pipelines is difficult, especially during cold weather. To facilitate the flow of highly viscous crude oils in pipelines, it is necessary to reduce their viscosity. This can be achieved by forming emulsions of O/W type with crude oil as the dispersed phase. The concept of crude oil transportation in the form of O/W emulsion has already been utilized commercially in a pipeline 21 km in length and 20 cm in diameter in California, and in a pipeline 238 km in length and 51 cm in diameter in Indonesia [7]. For emulsion pipelining to be economical, it is important to keep the dispersed-phase (oil) concentration of the emulsion as high as possible and, at the same time, maintain the emulsion viscosity at a reasonable level. However, concentrated O/W emulsions are known to exhibit non-Newtonian shear-thinning behavior.

In light of the industrial applications of emulsions just mentioned, it is of practical significance to investigate the production of entropy in emulsion flow in pipelines and other process equipment. In the past, a number of research articles have been published on simultaneous flow of oil and water in pipelines [7,9–22]. The published studies deal with topics such as: phase inversion in emulsion flow [9–12], droplet size and droplet size distribution in emulsion flow [13,14], flow patterns in concurrent flow of oil and water in pipelines [15–17], and pressure drop in pipeline flow of emulsions [7,16–22]. However, little or no attention has been given to the second law analysis and entropy generation in emulsion flows despite the practical significance of the problem.

This work is in continuation of our earlier study on the production of entropy in flow of emulsions in smooth tubes [23]. Our earlier study was restricted to entropy generation in flow of dilute to moderately concentrated water-in-oil (W/O) emulsions. The emulsions were Newtonian in nature. The key objective of the present work is to experimentally investigate the generation of entropy in flow of highly concentrated surfactant-stabilized oil-in-water (O/W) emulsions in different diameter tubes. These emulsions exhibited non-Newtonian shear-thinning behavior. Models are also developed for the prediction of entropy generation rate in flow of power-law emulsions in smooth tubes.

It should be pointed out that a number of interesting research articles have been published recently on heat transfer and entropy generation in flow of Newtonian and non-Newtonian fluids [24–33]. Several published articles also deal with the fluid mechanics, thermodynamics, and stability of non-Newtonian fluids in different configurations [34–36]. However, the published studies mostly deal with analytical solutions and simulations related to homogeneous fluids. To our knowledge, little or no experimental and theoretical work has been reported on entropy generation in flow of concentrated non-Newtonian emulsions in tubes.

2. Theoretical Background

Consider a control volume with multiple inlets and outlets. Let the control volume be in contact with N heat reservoirs at temperatures T_i 's and the environment at T_o . Let the rates of heat transfer from heat reservoirs to the control volume be \dot{Q}_i 's and from environment to the control volume be \dot{Q}_o . Let the temperatures of the control volume boundary portions in contact with the heat reservoirs and the environment be T_{bi} 's and T_{bo} , respectively. Entropy balance on the control volume gives:

$$\sum_{In} \dot{m}s + \frac{\dot{Q}_o}{T_{bo}} + \sum_N \frac{\dot{Q}_i}{T_{bi}} - \sum_{Out} \dot{m}s + \dot{S}_{G,CV} = \frac{\partial S_{CV}}{\partial t} \quad (2)$$

where \dot{m} is the mass flow rate, s is the specific entropy, \dot{S}_G is the rate of entropy generation, “In” refers to inlets, “Out” refers to outlets, and subscript “CV” refers to control volume. Doing entropy balance on the surroundings, one can write:

$$-\frac{\dot{Q}_o}{T_{bo}} - \sum_N \frac{\dot{Q}_i}{T_{bi}} + \dot{S}_{G,surr} = \frac{\partial S_{surr}}{\partial t} = -\frac{\dot{Q}_o}{T_o} - \sum_N \frac{\dot{Q}_i}{T_i} \quad (3)$$

This equation could be re-cast as:

$$\dot{S}_{G,surr} = \frac{\dot{Q}_o}{T_{bo}} \left[1 - \frac{T_{bo}}{T_o} \right] + \sum_N \frac{\dot{Q}_i}{T_{bi}} \left[1 - \frac{T_{bi}}{T_i} \right] \quad (4)$$

Adding the entropy balances for control volume and surroundings, the following result is obtained:

$$\dot{S}_{G,total} = \frac{\partial S_{CV}}{\partial t} + \sum_{Out} \dot{m}s - \frac{\dot{Q}_o}{T_{bo}} - \sum_N \frac{\dot{Q}_i}{T_{bi}} - \sum_{In} \dot{m}s + \frac{\dot{Q}_o}{T_{bo}} \left[1 - \frac{T_{bo}}{T_o} \right] + \sum_N \frac{\dot{Q}_i}{T_{bi}} \left[1 - \frac{T_{bi}}{T_i} \right] \quad (5)$$

This equation could be re-cast as:

$$\dot{S}_{G,total} = \frac{\partial S_{CV}}{\partial t} + \sum_{Out} \dot{m}s - \frac{\dot{Q}_o}{T_o} - \sum_N \frac{\dot{Q}_i}{T_i} - \sum_{In} \dot{m}s \quad (6)$$

The thermodynamic efficiency η of a flow process is defined as the ratio of actual shaft work (\dot{W}_{sh}) produced to the maximum shaft work ($\dot{W}_{sh,ideal}$) obtainable from a given change in the properties of the flow streams [2,4]. Thus:

$$\eta = \frac{\dot{W}_{sh}}{\dot{W}_{sh,ideal}} = \frac{\dot{W}_{sh,ideal} - \dot{W}_{lost}}{\dot{W}_{sh,ideal}} \quad (7)$$

Using the Gouy-Stodola theorem, the thermodynamic efficiency of a process can be expressed as:

$$\eta = 1 - \frac{T_o \dot{S}_{G,total}}{\dot{W}_{sh,ideal}} \quad (8)$$

According to the second law of thermodynamics, $\dot{S}_{G,total} > 0$ for any irreversible process and therefore, the efficiency of a process expressed in Equation (8) is always less than one. Only in the limiting case of complete reversibility where the process is completely reversible without any internal and external irreversibilities, $\dot{S}_{G,total} = 0$ and the thermodynamic efficiency of the process is one.

Consider now the steady and adiabatic flow of fluid in a pipe. According to Equation (2):

$$\dot{S}_{G,CV} = \dot{m}(s_2 - s_1) = \dot{m}\Delta s \quad (9)$$

For adiabatic incompressible flow in a horizontal pipe in the absence of any shaft work, the enthalpy change is zero ($\Delta h = h_2 - h_1 = 0$) according to the first law for open systems. Using the following fundamental thermodynamic relation:

$$dh = Tds + \frac{dP}{\rho} \quad (10)$$

it follows that:

$$T \frac{ds}{dx} = \frac{1}{\rho} \left(-\frac{dP}{dx} \right) \quad (11)$$

where T is temperature, P is pressure, ρ is density, and dP/dx is pressure gradient in the direction of flow. Combining Equations (9) and (11), we obtain:

$$\dot{S}'_G = \dot{m} \frac{ds}{dx} = \frac{\dot{m}}{\rho T} \left(-\frac{dP}{dx} \right) \quad (12)$$

where \dot{S}'_G is the rate of entropy generation per unit pipe length.

The Fanning friction factor f in pipe flow is defined as:

$$f = \frac{(-dP/dx)(D/4)}{\rho \bar{V}^2 / 2} \quad (13)$$

where D is the pipe diameter and \bar{V} is the average fluid velocity in pipe. From Equations (12) and (13), it follows that:

$$\dot{S}'_G = \frac{\pi}{2T} (f \rho D \bar{V}^3) \quad (14)$$

In pipeline flow of non-Newtonian power-law fluids, friction factor is related to the generalized Reynolds number Re_n defined as:

$$Re_n = \frac{\rho D^n \bar{V}^{2-n}}{K 8^{n-1} \left[\frac{3n+1}{4n} \right]^n} \quad (15)$$

where K and n are the power-law parameters which appear in the following power-law model of the fluid:

$$\tau = K \dot{\gamma}^n \quad (16)$$

In this power law model, τ is the shear stress and $\dot{\gamma}$ is the shear rate. The power-law parameter K is often referred to as “consistency index” and n is called “flow behavior index”. For Newtonian fluids, $n=1$ and $K=\mu$ (μ is the viscosity) and the generalized Reynolds number Re_n reduces to the conventional Reynolds number. For pseudo-plastic (shear-thinning) fluids, $n < 1$ and for dilatant (shear-thickening) fluids, $n > 1$.

From Equations (14) and (15), it can be readily shown that:

$$\dot{S}'_G = \left(\frac{\pi}{2T} \right) \left[\frac{(a_n)^{3/(2-n)}}{\rho^{(1+n)/(2-n)} D^{(4n-2)/(2-n)}} \right] (f) (Re_n)^{3/(2-n)} \quad (17)$$

where a_n is given as :

$$a_n = K 8^{n-1} \left[\frac{3n+1}{4n} \right]^n \quad (18)$$

When the fluid is Newtonian, $n=1$, $K=\mu$, $a_n=\mu$, and the expression for entropy generation rate per unit pipe length reduces to :

$$\dot{S}'_G = \left(\frac{\pi}{2T} \right) \left[\frac{\mu^3}{\rho^2 D^2} \right] (f Re^3) \quad (19)$$

where Re is the conventional Reynolds number defined as: $Re = \rho D \bar{V} / \mu$. Equation (19) was derived in our previous study [23] on entropy generation in pipeline flow of Newtonian emulsions.

For *laminar* flow of non-Newtonian power-law fluids in pipes, the friction factor is related to the generalized Reynolds number Re_n as follows:

$$f = \frac{16}{Re_n} \quad (20)$$

For *turbulent* flow of non-Newtonian power-law fluids in *hydraulically smooth* pipes, the friction factor is given by the following Dodge-Metzner equation [37]:

$$\frac{1}{\sqrt{f}} = \left(\frac{4}{n^{0.75}} \right) \log_{10} [f^{(1-0.5n)} Re_n] - \frac{0.4}{n^{1.2}} \quad (21)$$

The Dodge-Metzner equation reduces to the well-known Prandtl-von Karman law in the special case of Newtonian fluids ($n=1$, $K=\mu$):

$$\frac{1}{\sqrt{f}} = 4 \log_{10} [Re \sqrt{f}] - 0.4 \quad (22)$$

The disadvantage of Equation (21) is that it is not explicit in f and has to be solved numerically. Dodge and Metzner [37] also proposed a Blasius-type equation explicit in f for non-Newtonian fluids:

$$f = \frac{\alpha_n}{(\text{Re}_n)^{\beta_n}} \quad (23)$$

where α_n and β_n are functions of n reported graphically. The plots of α_n versus n and β_n versus n can be described accurately by the following expressions:

$$\alpha_n = 0.0077 \ln(n) + 0.078 \quad (24)$$

$$\beta_n = 0.25(n)^{-0.22} \quad (25)$$

The critical Reynolds number for transition from laminar to turbulent flow in power-law non-Newtonian fluids is given as [38]:

$$(\text{Re}_n)_{\text{critical}} = \frac{2100(4n+2)(5n+3)}{3(3n+1)^2} \quad (26)$$

Substitution of the friction factor expressions from Equations (20) and (23) into Equation (17) leads to the following relations for entropy production in pipeline flow of non-Newtonian power-law fluids:

$$\dot{S}'_G = \left(\frac{8\pi}{T} \right) \left[\frac{(a_n)^{3/(2-n)}}{\rho^{(1+n)/(2-n)} D^{(4n-2)/(2-n)}} \right] (\text{Re}_n)^{(1+n)/(2-n)} \quad \text{laminar flow} \quad (27)$$

$$\dot{S}'_G = \left(\frac{\pi}{2T} \right) \left[\frac{(a_n)^{3/(2-n)}}{\rho^{(1+n)/(2-n)} D^{(4n-2)/(2-n)}} \right] \alpha_n (\text{Re}_n)^{(3/(2-n))-\beta_n} \quad \text{turbulent flow} \quad (28)$$

where a_n is given by Equation (18), α_n by Equation (24), and β_n by Equation (25). Equations (27) and (28) are the new predictive models for entropy generation per unit length in pipeline flow of non-Newtonian power-law fluids. These models could be applied to non-Newtonian (power-law) pseudo-homogeneous mixtures of two phases such as emulsions of oil and water. When the fluid is Newtonian, $n=1$, $K=\mu$, these expressions reduce to:

$$\dot{S}'_G = \frac{\pi}{2T} \left(\frac{\mu^3}{\rho^2 D^2} \right) (16 \text{Re}^2) \quad \text{laminar flow} \quad (29)$$

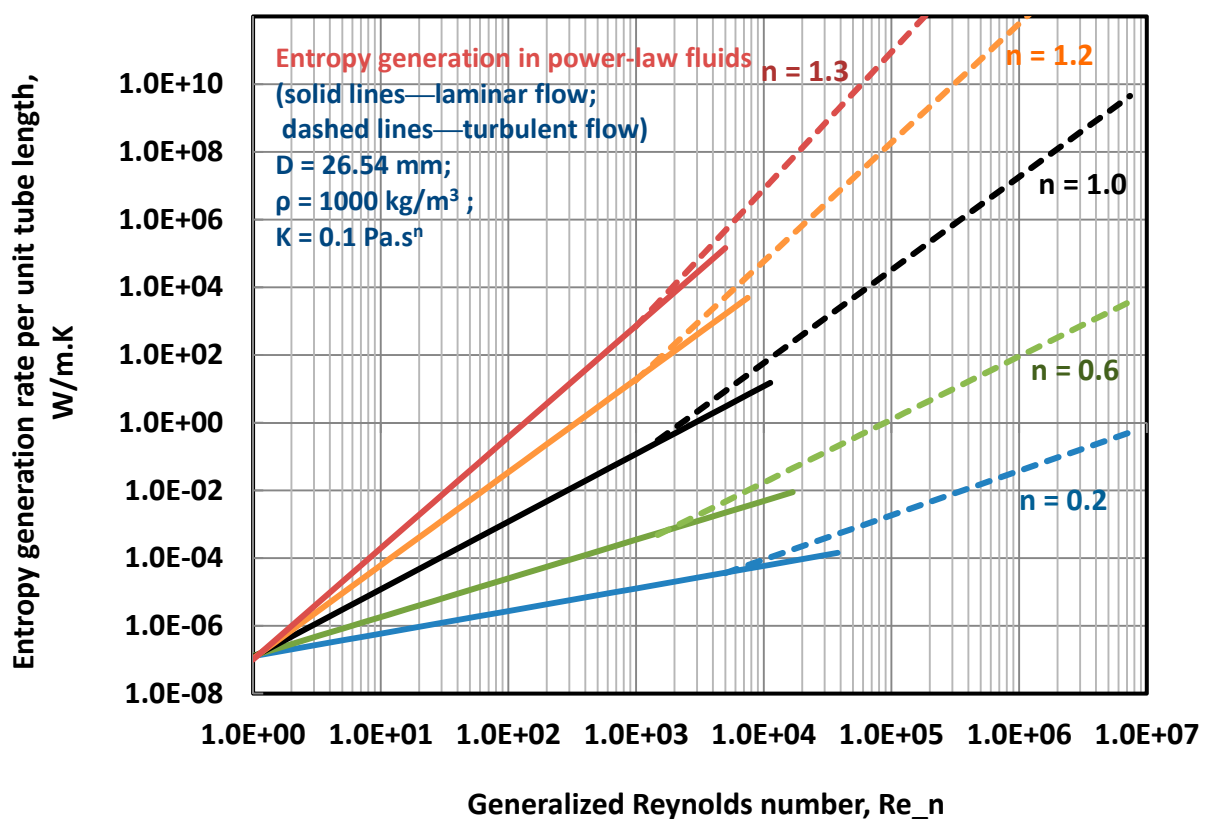
$$\dot{S}'_G = \frac{\pi}{2T} \left(\frac{\mu^3}{\rho^2 D^2} \right) (0.078 \text{Re}^{2.75}) \quad \text{turbulent flow} \quad (30)$$

Equations (29) and (30) were derived in our previous study [23] on entropy generation in pipeline flow of Newtonian emulsions.

3. Model Predictions

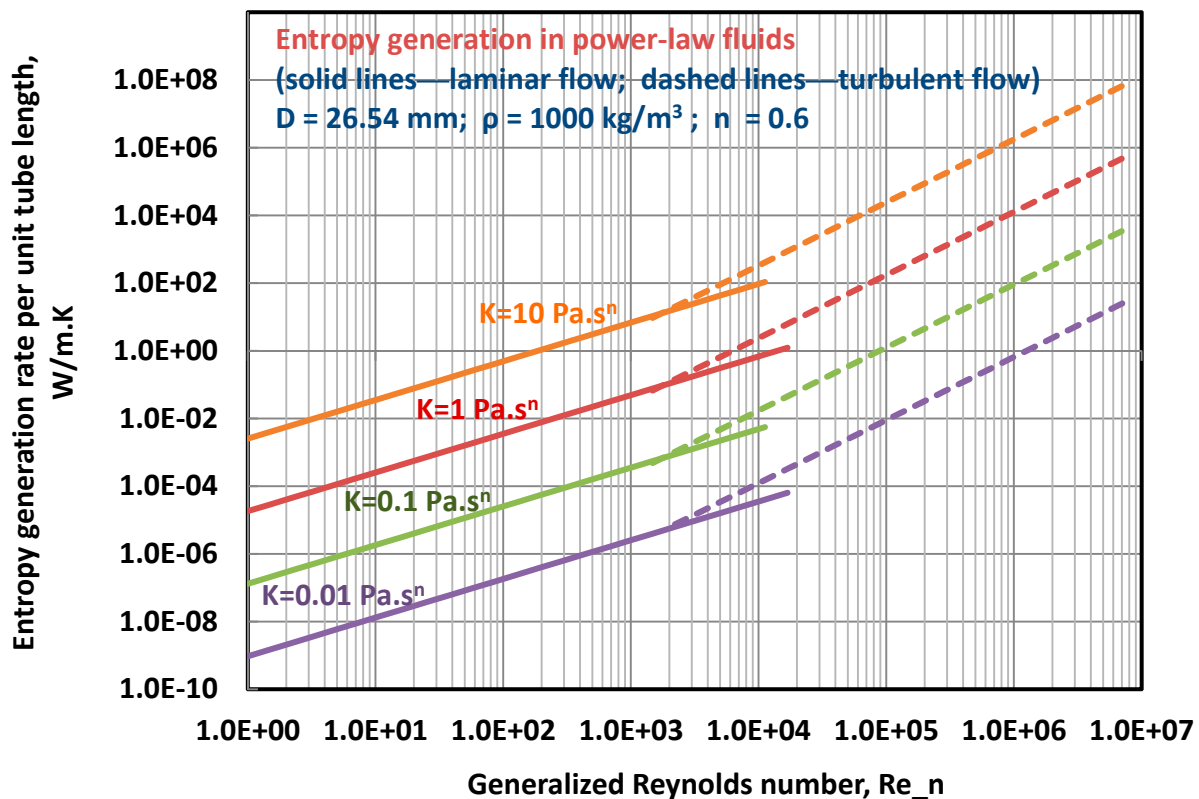
Figure 1 shows the effect of flow behavior index n on entropy generation rate in flow of non-Newtonian power-law fluids in a smooth tube. The plots of \dot{S}'_G versus Re_n are generated from model Equations (27) and (28) for different values of n . The tube diameter is 26.54 mm and the fluid properties are as follows: $\rho = 1000 \text{ kg/m}^3$ and $K = 0.1 \text{ Pa.s}^n$. The figure indicates that: (a) for a given value of n , the entropy generation rate \dot{S}'_G increases linearly with the increase in generalized Reynolds number on a log-log scale, in both laminar and turbulent regimes. However, the slope in the turbulent regime is higher; (b) for a given value of Re_n , the entropy generation rate per unit tube length increases with the increase in the value of the flow behavior index n . This indicates that flow of pseudo-plastic fluids ($n < 1$) is more efficient thermodynamically in comparison with dilatant fluids ($n > 1$).

Figure 1. \dot{S}'_G versus Re_n plots for non-Newtonian power-law fluids for different values of flow behavior index n .



The influence of consistency index K on entropy generation rate in flow of power-law fluids in a smooth tube is shown in Figure 2. The plots of \dot{S}'_G versus Re_n shown in the figure are generated from model Equations (27) and (28) for different values of K . The tube diameter is 26.54 mm and the fluid properties are as follows: $\rho = 1000 \text{ kg/m}^3$ and $n = 0.6$. With the increase in K , a constant upward shift is observed in the plot of \dot{S}'_G versus Re_n . This indicates that for a given value of Re_n , the entropy generation rate per unit tube length increases with the increase in K value.

Figure 2. \dot{S}'_G versus Re_n plots for non-Newtonian power-law fluids for different values of consistency index K .



4. Experimental Work

Figure 3 shows a schematic diagram of the flow rig that was designed and developed to experimentally investigate the rate of entropy generation in flow of emulsions in smooth tubes. Five different diameter tubes (stainless steel, seamless) were installed horizontally. The various dimensions of the test sections are summarized in Table 1. The emulsions were prepared in a large mixing tank (capacity about 1 m^3) equipped with baffles, two high shear mixers, heating/cooling coil, and a temperature controller. The emulsion from the mixing tank was circulated to the tube test sections, one at a time, by a centrifugal pump. From the tube test section, the emulsion was allowed to return to the mixing tank via the metering section where its flow rate was measured.

The pressure drops in various tubes were measured by means of pressure transducers. The output signals from the pressure transducers were recorded by a microcomputer data-acquisition system. Further details about the flow rig can be found in our earlier publication [23].

The emulsions were prepared using 1% by wt. surfactant solution in tap water and a refined mineral oil (Bayol-35). Triton X-100 (isooctylphenoxypolyethoxy ethanol) was used as a surfactant. This is a water soluble non-ionic surfactant. The oil had a density of 780 kg/m^3 and a viscosity of 2.41 mPa.s at 25°C . The oil-in-water emulsions of three different dispersed phase (oil) concentrations were prepared; the dispersed phase concentrations were 59.61%, 65.15%, and 72.21% by volume. The emulsions produced were highly stable with respect to coalescence.

A Fann coaxial cylinder viscometer was used to determine the rheological behavior (shear stress versus shear rate) of emulsions. The droplet size information of emulsion was obtained by taking photomicrographs with a Zeiss optical microscope.

The experimental work was conducted at a constant temperature of 25 °C. The temperature was maintained constant in the flow loop with the help of a temperature controller installed in the mixing tank.

Figure 3. Schematic diagram of the flow rig.

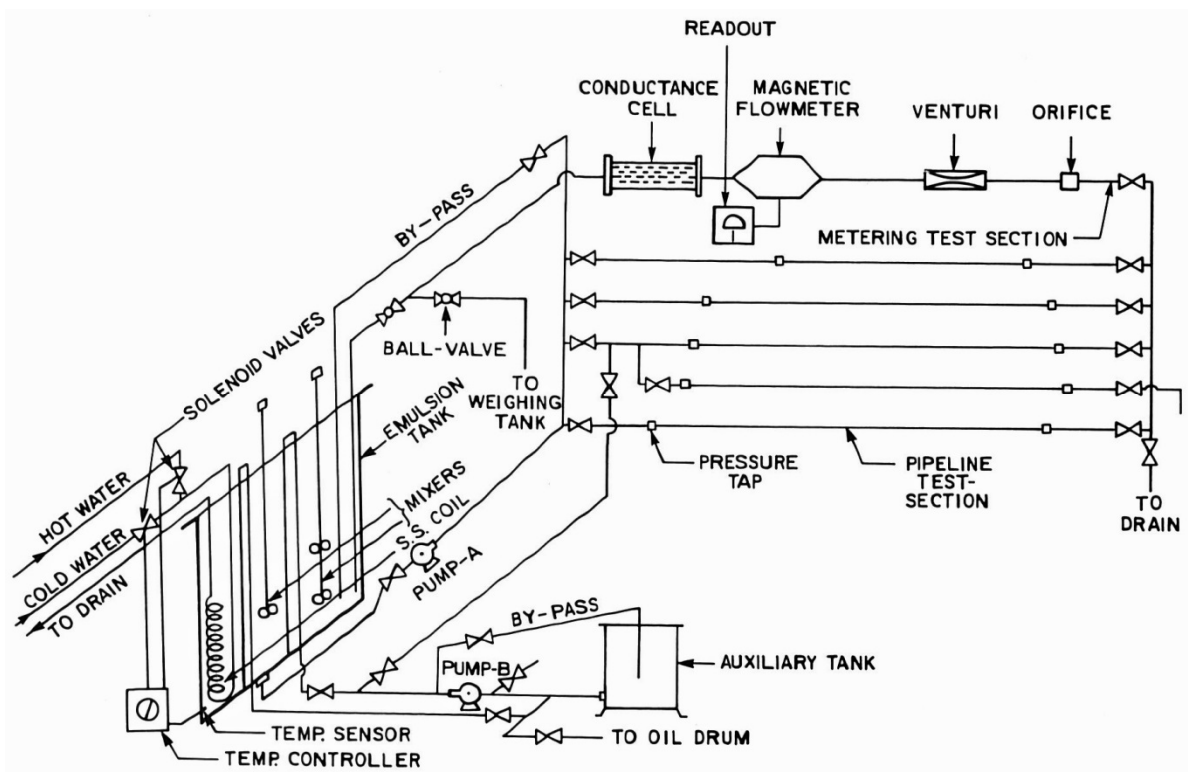


Table 1. Various dimensions of tube test sections.

Tube inside diameter [mm]	Entrance length [m]	Length of test section [m]	Exit length [m]
7.15	1.07	3.05	0.46
8.89	0.89	3.35	0.48
12.60	1.19	2.74	0.53
15.80	1.65	2.59	0.56
26.54	3.05	1.22	0.67

5. Experimental Results and Discussion

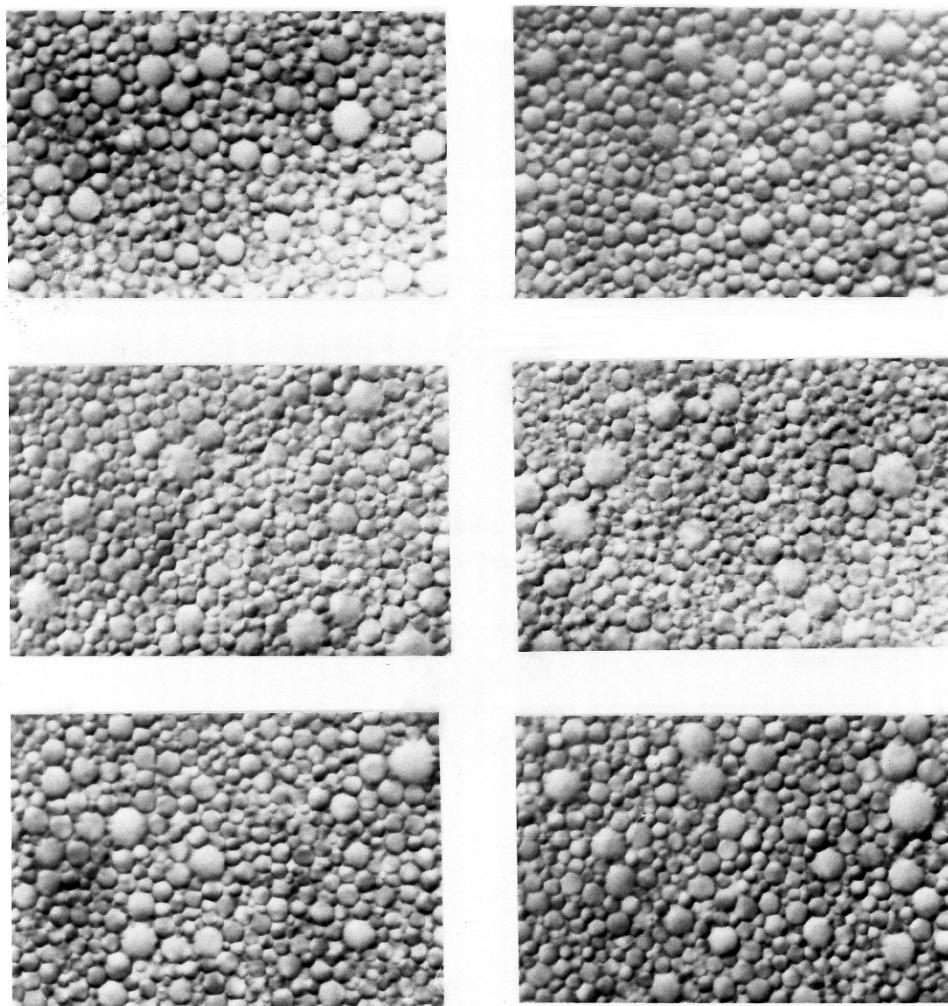
Figure 4 shows typical photomicrographs of oil droplets of an emulsion. The droplets are smaller than 12 μm in diameter. The viscosity *versus* shear rate plots of emulsions are shown in Figures 5–7.

The apparent viscosity μ , defined as the ratio of shear stress (τ) to shear rate ($\dot{\gamma}$), decreases with the increase in shear rate indicative of shear-thinning non-Newtonian behavior of emulsions. The plots of μ *versus* $\dot{\gamma}$ follow a linear relationship on a log-log scale indicating that emulsions follow a power-law model (Equation (16)). Note that the power-law model (Equation (16)) could be expressed as:

$$\log \mu = \log K - (1 - n) \log \dot{\gamma} \quad (31)$$

Thus, the slope of μ versus $\dot{\gamma}$ plot is negative, equal to $-(1-n)$. According to plots of Figures 5–7, the power-law index n decreases and the consistency index K increases with the increase in dispersed-phase (oil) concentration. The variations of n and K with the dispersed-phase concentration of emulsion can be seen more clearly in Figures 8 and 9. Interestingly, the power law constants n and K undergo dramatic changes when the oil concentration of the emulsion is increased from 65.15–72.21% vol.

Figure 4. Typical photomicrographs of emulsion.



12 μm

Figure 5. Apparent viscosity *versus* shear rate plot for 59.61% vol. O/W emulsion.

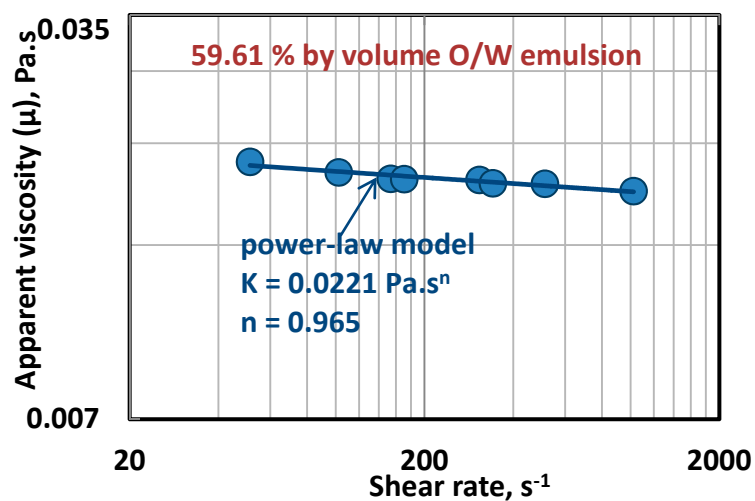


Figure 6. Apparent viscosity *versus* shear rate plot for 65.15% vol. O/W emulsion.

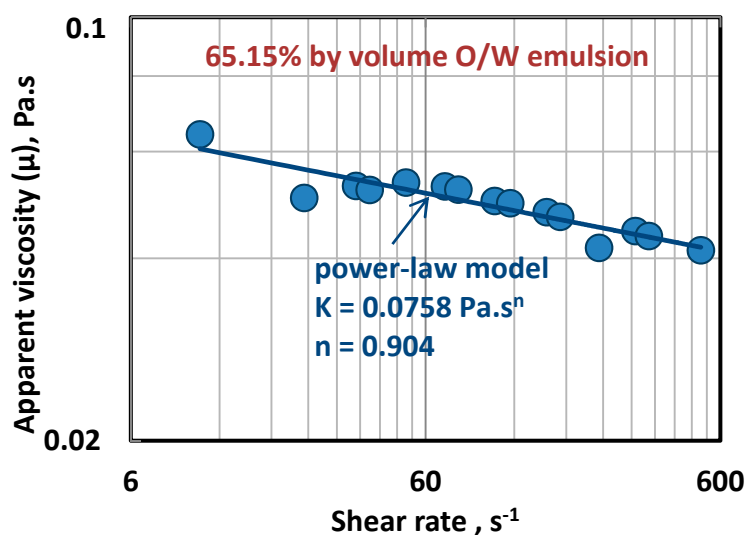


Figure 7. Apparent viscosity *versus* shear rate plot for 72.21% vol. O/W emulsion.

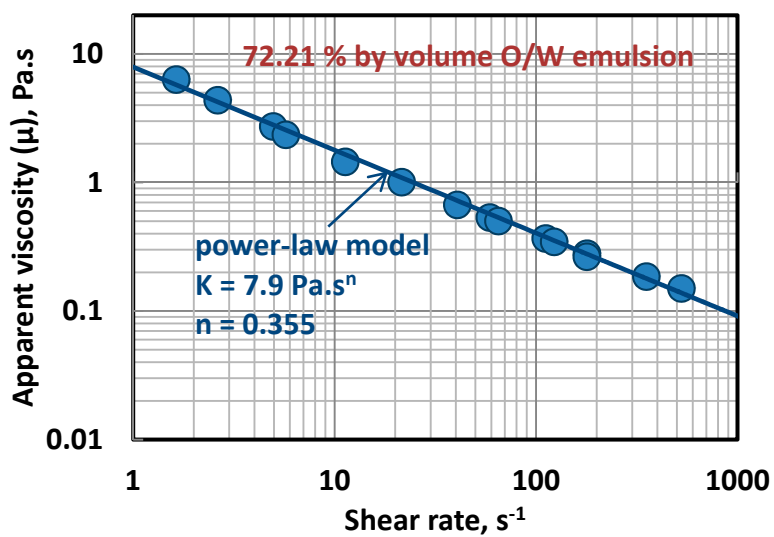


Figure 8. Variation of flow behavior index n with the increase in dispersed phase concentration of O/W emulsion.

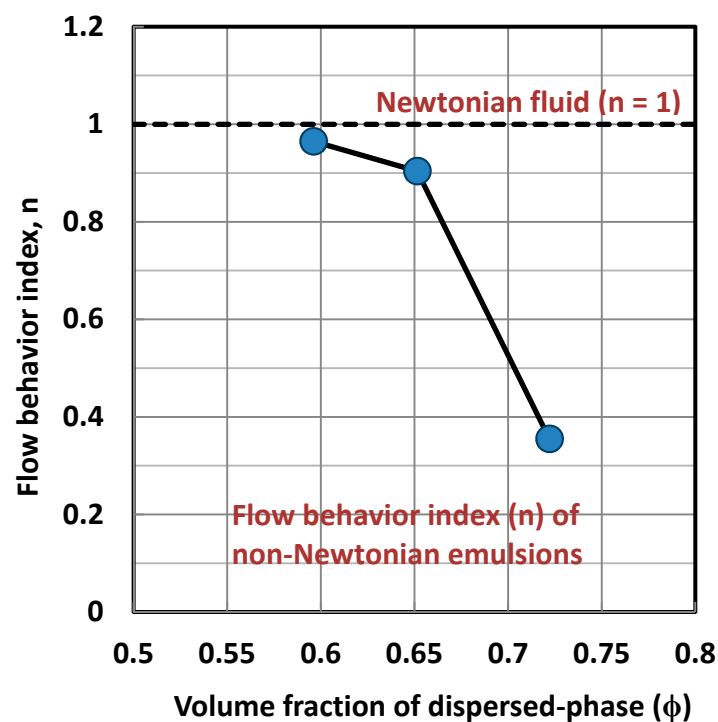


Figure 9. Variation of consistency index K with the increase in dispersed phase concentration of O/W emulsion.

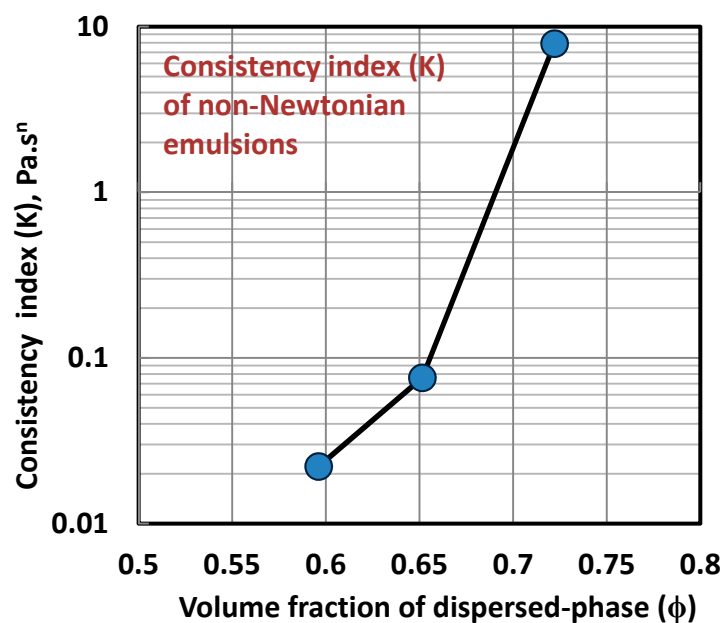
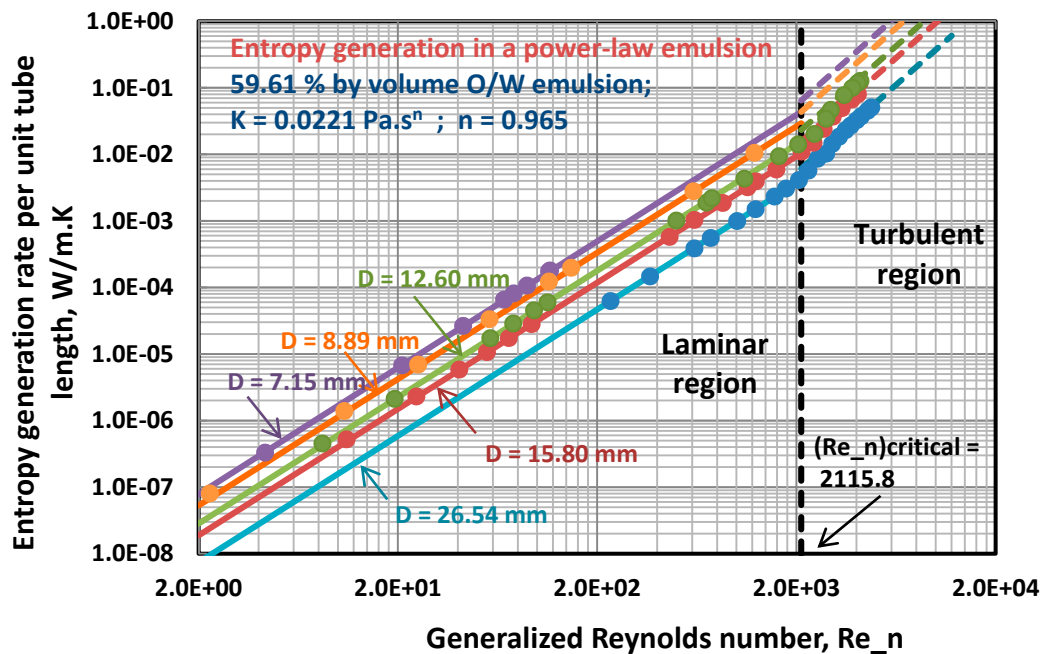


Figure 10 shows the plots of \dot{S}'_G versus Re_n data for 59.61% vol. O/W emulsion in different diameter tubes. For a given diameter tube, the entropy generation rate \dot{S}'_G increases linearly with the increase in the generalized Reynolds number (Re_n) on a log-log plot. As expected, the slope of \dot{S}'_G versus Re_n plot is higher in the turbulent regime. With the increase in tube diameter, the entropy generation rate per unit tube length decreases at any given value of the generalized Reynolds number.

Also, the experimental data shows excellent agreement with the predictions of the models. The solid lines shown in Figure 10 are the predictions of laminar model (Equation (27)) and the dashed lines represent the predictions of turbulent model (Equation (28)).

Figure 10. \dot{S}'_G versus Re_n plots for 59.61% vol. O/W emulsion flow in different diameter tubes. The solid lines in the laminar region represent Equation (27) and the dashed lines in the turbulent region represent Equation (28).



Figures 11 and 12 show the plots of \dot{S}'_G versus Re_n data for 65.15% and 72.21% vol. O/W emulsions, respectively. Due to the highly viscous nature of these emulsions, turbulent flow could not be achieved in our experiments and the data are restricted to laminar regime only. The plots of \dot{S}'_G versus Re_n data are linear (log-log scale) and the experimental data show good agreement with the predictions of the model, see Equation (27). It is interesting to note that in the case of 72.21% vol. O/W emulsion, the diameter dependence of entropy generation rate \dot{S}'_G is opposite to that of the other emulsions with lower volume fraction of dispersed-phase. The entropy generation rate \dot{S}'_G increases with the increase in tube diameter for 72.21% vol. O/W emulsion whereas the other emulsions with lower concentration exhibit a decrease in \dot{S}'_G with the increase in tube diameter at a given Re_n . According to the models, Equations (27) and (28):

$$\dot{S}'_G \propto D^{-(4n-2)/(2-n)} \quad (32)$$

When $n = 0.5$, Equation (32) predicts \dot{S}'_G to be independent of the tube diameter. When $n > 0.5$, \dot{S}'_G is expected to decrease with the increase in tube diameter as $(4n-2)/(2-n) > 0$; for Newtonian fluid ($n = 1$), $(4n-2)/(2-n) = 2$. When $n < 0.5$, \dot{S}'_G is expected to increase with the increase in tube diameter as $(4n-2)/(2-n) < 0$; for the case of extreme pseudo-plasticity ($n = 0$), $(4n-2)/(2-n) = -1$ and $\dot{S}'_G \propto D$, that is, \dot{S}'_G is directly proportional to the tube diameter.

Figure 11. \dot{S}'_G versus Re_n plots for 65.15% vol. O/W emulsion flow in different diameter tubes. The solid lines represent Equation (27).

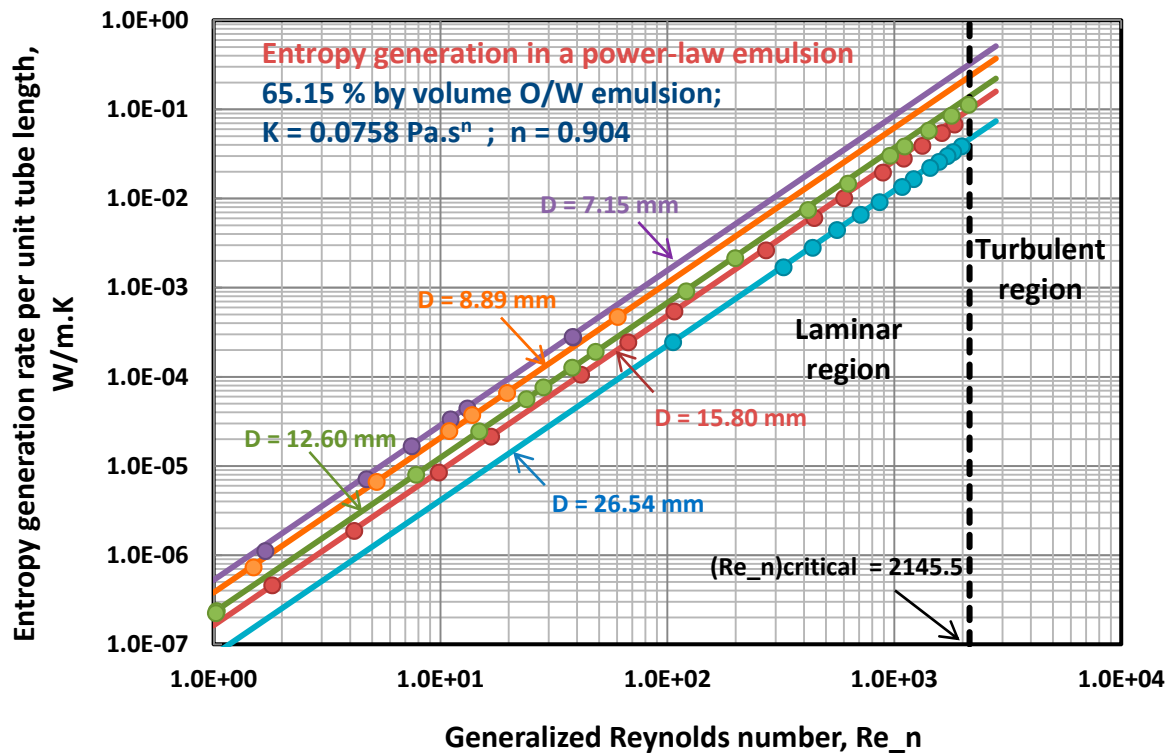
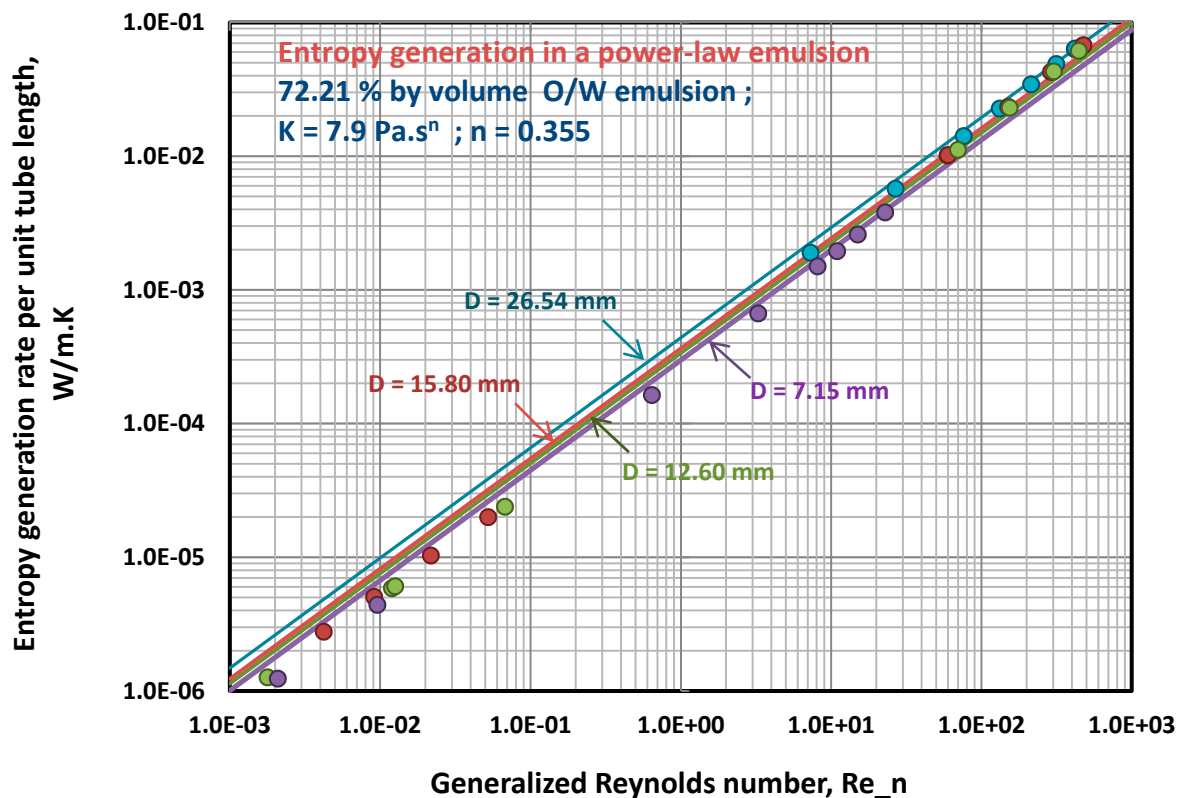


Figure 12. \dot{S}'_G versus Re_n plots for 72.21% vol. O/W emulsion flow in different diameter tubes. The solid lines represent Equation (27).



Figures 13–15 confirm the diameter-dependence of \dot{S}'_G expressed in Equation (32). The experimental data are now re-plotted as $D^{(4n-2)/(2-n)}\dot{S}'_G$ versus Re_n . As expected, the experimental data for a given emulsion from different diameter tubes fall on the same curve. The solid lines shown in the figures are generated from the model equations: Equations (27) for laminar flow and Equation (28) for turbulent flow. There is good agreement between experimental data and model predictions.

Figure 16 compares the plots of $D^{(4n-2)/(2-n)}\dot{S}'_G$ versus Re_n for different emulsions. The experimental data from all the tubes are included. At any given value of the generalized Reynolds number (Re_n), the diameter-scaled entropy generation rate ($D^{(4n-2)/(2-n)}\dot{S}'_G$) of O/W emulsion increases with the increase in the dispersed-phase (ϕ) concentration. While the increase in entropy generation rate is modest when ϕ increases from 59.61–65.15% vol., a large increase in entropy generation rate is observed when ϕ increases from 65.15–72.21% vol.

At a high dispersed-phase concentration of 72.21% vol., the dispersed (oil) droplets of emulsion are jam packed and consequently the emulsion behaves as a very viscous material with high rates of entropy generation. The theoretical value of the dispersed-phase concentration corresponding to hexagonal close packing of spheres is 74% vol. Thus, emulsions are expected to behave more like a semi-solid material with significant yield stress when ϕ is increased above 74% vol.

Figure 13. $D^{(4n-2)/(2-n)}\dot{S}'_G$ versus Re_n plot for 59.61% vol. O/W emulsion flow in different diameter tubes ($n = 0.965, K = 0.0221 \text{ Pa.s}^n$). The solid line in the laminar region represents Equation (27) and the solid line in the turbulent region represents Equation (28). The colored circles represent experimental data from different diameter tubes.

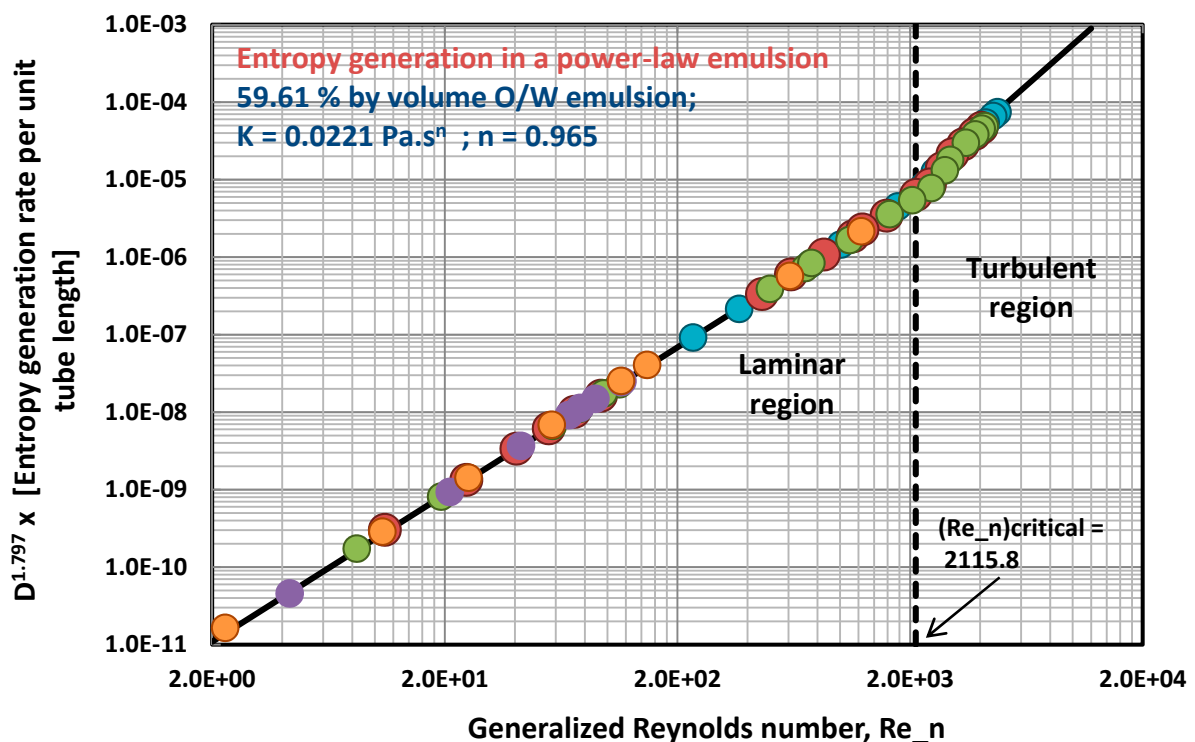


Figure 14. $D^{(4n-2)/(2-n)}\dot{S}'_G$ versus Re_n plot for 65.15% vol. O/W emulsion flow in different diameter tubes ($n = 0.904, K = 0.0758 \text{ Pa}\cdot\text{s}^n$). The solid line represents Equation (27). The colored circles represent experimental data from different diameter tubes.

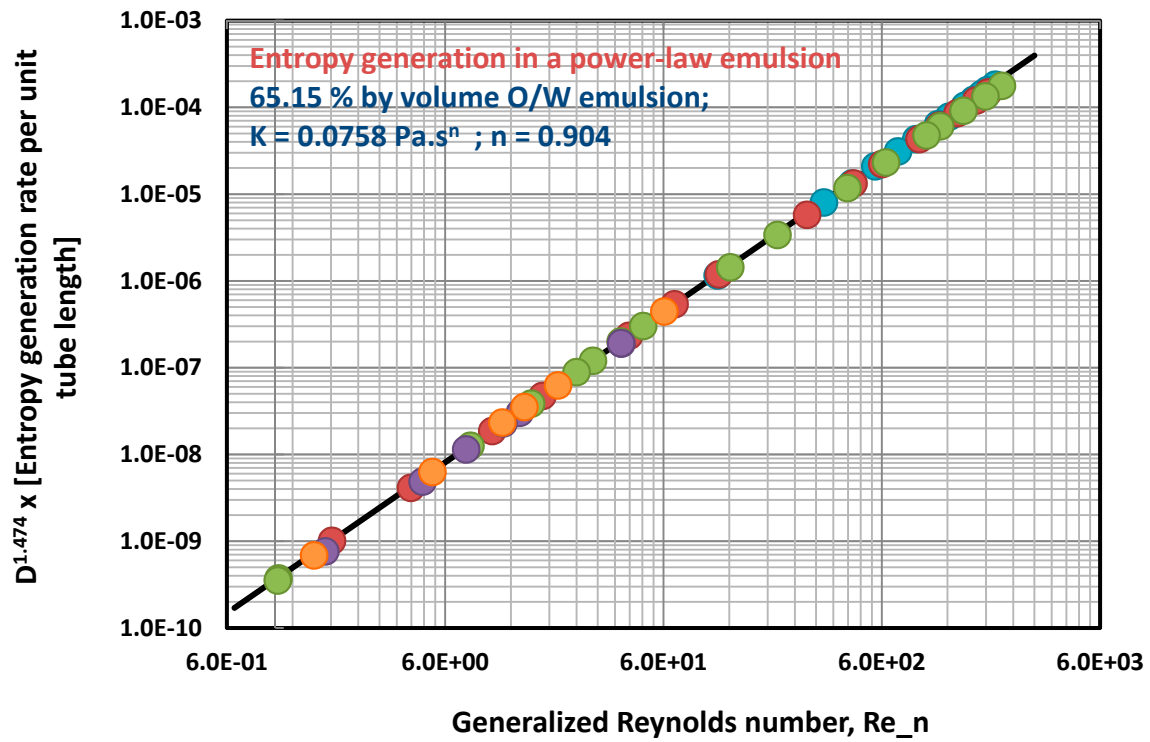


Figure 15. $D^{(4n-2)/(2-n)}\dot{S}'_G$ versus Re_n plot for 72.21% vol. O/W emulsion flow in different diameter tubes ($n = 0.355, K = 7.9 \text{ Pa}\cdot\text{s}^n$). The solid line represents Equation (27). The colored circles represent experimental data from different diameter tubes.

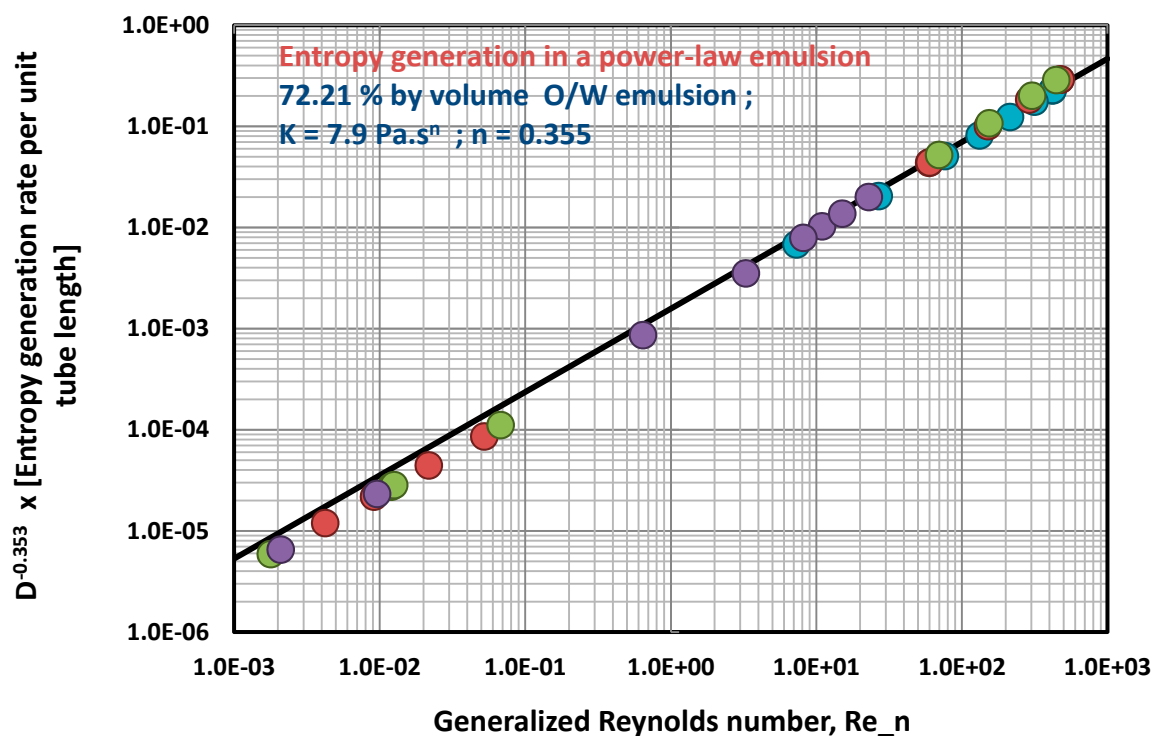
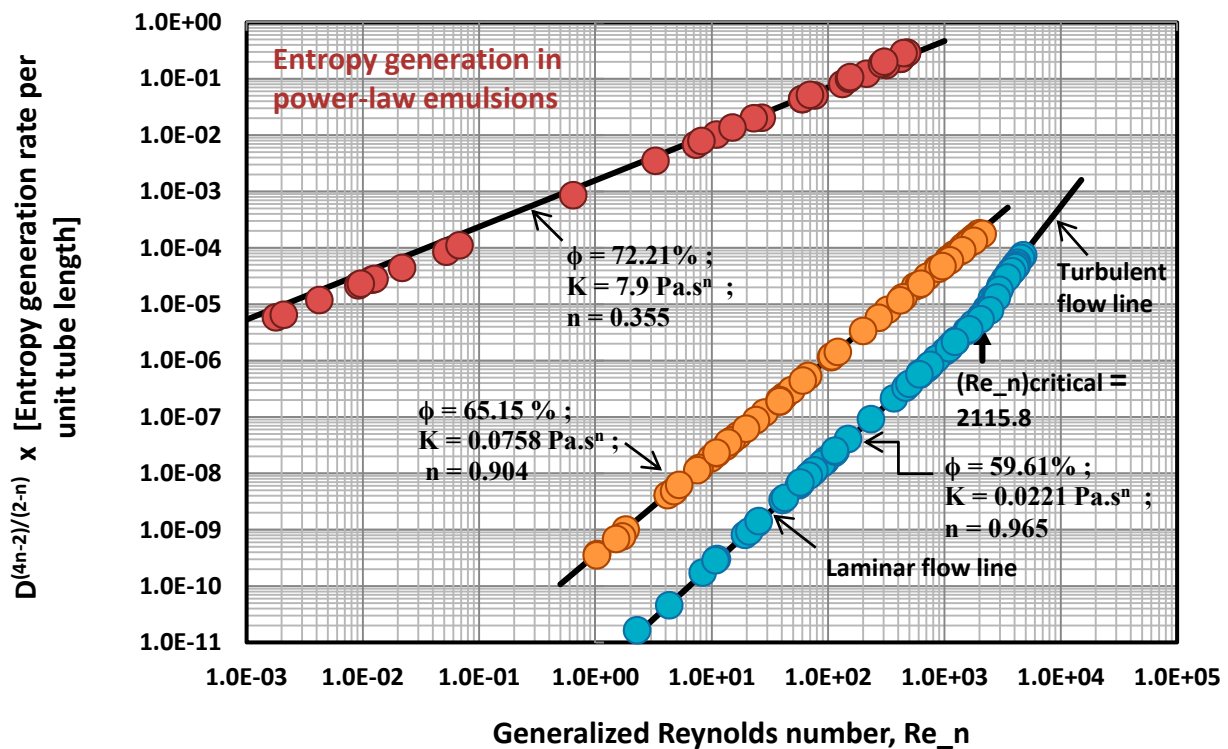


Figure 16. Comparison of $D^{(4n-2)/(2-n)} \dot{S}'_G$ versus Re_n plots for O/W emulsions with different dispersed-phase concentrations. The solid lines represent Equation (27) (laminar flow) and Equation (28) (turbulent flow). The colored circles represent experimental data.



6. Conclusions

Entropy production in adiabatic flow of non-Newtonian power-law emulsions of oil-in-water type in smooth tubes was investigated experimentally and theoretically. Based on this study, the following conclusions can be made: (a) for a given power-law emulsion (K and n fixed), the entropy generation rate \dot{S}'_G in a given diameter tube increases linearly with the increase in generalized Reynolds number on a log-log scale, in both laminar and turbulent regimes. However, the slope in the turbulent regime is higher; (b) at a given value of the generalized Reynolds number Re_n , the entropy generation rate per unit tube length increases with the increase in the value of the flow behavior index n , keeping other factors (K and D) constant; (c) at a given value of Re_n , the entropy generation rate per unit tube length increases with the increase in K value, keeping other factors (n and D) constant; (d) the power-law constants (n and K) undergo dramatic changes when the dispersed-phase concentration of the O/W emulsion is increased from 65.15%–72.21% vol.; n drops whereas K rises sharply; (e) emulsions with dispersed-phase concentration (ϕ) \leq 65.15% exhibit inverse diameter-dependency in that the entropy generation rate decreases with the increase in tube diameter whereas emulsion with $\phi = 72.21\%$ vol. shows direct diameter-dependency in that the entropy generation rate increases with the increase in tube diameter; (f) the diameter-scaled entropy generation rate increases sharply when ϕ is increased from 65.15%–72.21% vol.; and (g) the models proposed for entropy generation rate in flow of power-law fluids in tubes describe the experimental data for power-law emulsions reasonably well.

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Conflicts of Interest

The author declares no conflict of interest.

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