

Describing of drying curves of green coffee beans using mathematical model

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Abstract. The most important processes in food processing include drying. Generally it is the removal of water from the material for further processing or storage. This study was focused on the analysis of drying process of green coffee beans (*Coffea arabica*). The green beans, originally from Indonesia, were used in this experiment. Moisture content of beans $M_c = 28.1 \pm 1.7$ % (w.b.) were determined. The beans were dried at different air temperatures $T_d = 40, 60, 80, 100$ and 120 ± 1 °C. Drying tests were carried out on drying scales (Radwag, MA 50.R, Poland). The test was repeated three times for each temperature. Measured data were analysed by computer software Mathcad 14. Experimental drying curves at different temperatures were determined. The measured values of the drying curves of green coffee beans were fitted and a mathematical model was created. Model coefficients were determined and the proposed model was statistically analysed.

1. Introduction

Coffee is one of the most commonly consumed beverages in the world. Drying coffee plays a very important role in its processing. Drying is one of the oldest methods of agriculture products preservation and improves the shelf life of agriculture products [1]. Without drying, it is not possible to process or store fresh coffee. For storage of coffee beans is necessary to reduce their moisture content. Due to the drying requirements, it is necessary to keep coffee moisture around 11% [2]. Drying coffee is a very sensitive process that can affect quality [3]. For example, drying has an effect on the sugar content of coffee beans [4]. Removing the water is very energy intensive and therefore it is necessary to find optimal point drying [5]. One of the most important parameters in the design of drying lines is energy and time efficiency [6], [7], [8]. When designing dryers, it is necessary to know drying curves for different drying temperatures. The aim of this study is to determine the mathematical model describing the coffee bean drying curves for different drying temperatures.

2. Materials and Methods

2.1. Materials

Samples of coffee beans (*Coffea arabica* L.), obtained from Nord Sumatra region, Indonesia were used for this experiment. The moisture content $M_c = 28.1 \pm 1.7$ % (w.b.) of



the freshly coffee beans was determined using standard oven method, ASAE method (ASAE S410.1 DEC97, ASAE, 1998). Samples of 100 g mass from a batch of coffee beans were randomly selected for the moisture content determination. For measuring of mass of each sample $m_s(g)$ an electronic balance (Kern 440–35, Kern & Sohn GmbH, Balingen, Germany) was used. All the obtained results were expressed as mean of three replicates. Beans samples were packaged by vacuum atmosphere in polyethylene (PE) bag. Packed samples of coffee beans were transported using air transport to the laboratory of CULS Prague. All the beans were stored in a refrigerator at 5 ± 1 °C prior to the experiments.

2.2. *Drying experiments*

Drying experiments were carried out using drying moisture balance (Radwag, MA 50.R, Poland). Moisture balance is equipped with IR emitter heating module 400 W and was set to a standard drying profile. Samples of coffee beans weighing 15g were inserted into drying balance and air-dried at temperatures of 40, 60, 80, 100 and 120 ± 1 °C. The weight loss changes per minute were recorded in the memory. The test was repeated three times for each temperature.

2.3. Mathematical modelling of drying curves

The measured values of weight loss of coffee beans for different drying temperatures were analysed with computer program Mathcad 14 (MathCAD 14, PTC Software, Needham, MA, USA), (Pritchard, 1998) uses Levenberg-Marquardt algorithm for data fitting (Marquardt 1963). ANOVA was used for statistical verification of the obtained models.

3. Results and discussion

The figure (Fig. 1) shows the drying curves of coffee beans for different drying temperatures in range of 40 – 120 °C. The initial moisture content of freshly harvested coffee beans was observed to be $Mc = 28.1 \pm 1.7\%$ (w.b.), which is normal value for coffee beans [9]. Drying continued until the final moisture content was ca. 11% (w.b.). The appropriate moisture content for storing the coffee is around 11% (w.b.) [10] Fig. 1 shows that, as expected, drying rate increases significantly as the drying air temperature increases. However, it is necessary to use the appropriate temperature when drying the coffee beans. It has been found that when drying above 45 °C the coffee beans may be damaged [11]. Therefore optimum drying temperature is required for the highest quality coffee. The results indicate that increasing drying air temperature can extensively enhance drying process. This is due to the fact that high temperature could enhance heat transfer between drying air and coffee beans [12].

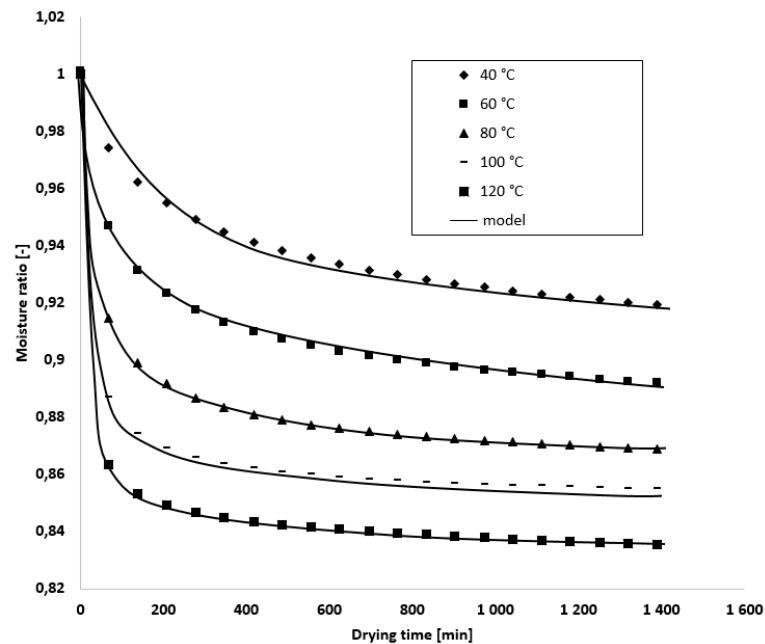


Figure 1. Measured values of moisture ratio of coffe beans and fitted models in the air temperature range of 40 – 120 °C

Individual measured drying values are shown in figure 1. Measured values for different drying air temperatures were fitted by exponential curve using Marguardt Levenberg algorithm and it is described by Eq. 1.

$$\vartheta(d, t) = d_0 + d_1(e^{d_2 \cdot t}) + d_3(e^{d_4 \cdot t}) \quad (1)$$

where: d_0, d_1, d_2, d_3, d_4 – coefficients of equation; t – drying time.

The values of coefficients d_0, d_1, d_2, d_3, d_4 from Eq. 1 are presented in Table 1.

Table 1. Estimated values of coefficients for Eq. 1

Temperature of drying (°C)	d_0 (-)	d_1 (-)	d_2 (min ⁻¹)	d_3 (-)	d_4 (min ⁻¹)
40	0.914	0.031	-0.014	0.054	-0.00167
60	0.89	0.06	-0.022	0.05	-0.00219
80	0.869	0.091	-0.029	0.04	-0.0028
100	0.855	0.117	-0.037	0.028	-0.00321
120	0.835	0.142	-0.04	0.023	-0.00224

In table 2 a statistical evaluation of the obtained model was determined. From statistical analysis ANOVA (table 2) follows, that measured amounts of drying curves at different temperatures and results from the general exponential model (Eq. 1) were statistically significant at significance level 0.05, that is, the values of F_{crit} (critical value comparing a pair of models) were higher than the F_{rat} values (value of the F – test) for all the measured coffee

beans and values of P_{value} (significance level at which it can be rejected the hypothesis of equality of models) (table 2) were higher than 0.05 which is also confirmed by very high coefficients of determination R^2 .

Table 2. Statistical analysis of general model

Temperature of drying (°C)	F_{rat} (-)	F_{crit} (-)	P_{value} (-)	R^2 (-)
40	$1.703 \cdot 10^{-11}$	4.085	1	0.998
60	$1.223 \cdot 10^{-11}$	4.085	1	0.999
80	$1.811 \cdot 10^{-11}$	4.085	1	0.999
100	$-7.214 \cdot 10^{-12}$	4.085	1	0.993
120	$-5.857 \cdot 10^{-12}$	4.085	1	0.996

F_{rat} - value of the F test, F_{crit} - critical value that compares a pair of models, P_{value} - hypothesis of the study outcomes significant level, R^2 – coefficient of determination

From the Fig. 1 is also visible that drying rate decrease showed no constant drying rate period for coffee beans. This fact is caused by the structure of the sample being dried and the mechanism of internal liquid migration [13]. Some previous authors found that moisture diffusion represents the dominant physical mechanism affecting drying rate decrease during the drying of natural products [14], [15]. Drying is a very energy-intensive process and has a significant effect on the quality of the final product [16]. It is necessary to know the mathematical description of drying curves for the construction of coffee dryers. Modelling of the drying process is examined by a number of authors [17], [18], [19].

4. Conclusion

This study was focussed on the drying process of green coffee beans. A change in weight was determined depending on the drying time and the drying temperature. This dependence was transformed into general mathematical model describing hot air drying of green coffee beans. The model of Eq. 1 provides valuable information about the moisture ratio during drying. This model may be used in the optimal design of coffee dryers.

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References

- [1] Larrauri J A, 1999 New approaches in the preparation of high dietary fibre powders from fruit by-products. Trends in Food Science & Technology 10 pp 3-8
- [2] Burmester K, Eggers R, 2010 Heat and mass transfer during the coffee drying process. Journal of Food Engineering 99 pp 430-436
- [3] Dong W, Hu R, Chu Z, Zhao J, Tan L, 2017 Effect of different drying techniques on bioactive components, fatty acid composition, and volatile profile of robusta coffee beans. Food Chemistry 234 PP 121-130
- [4] Kleinwächter M, Selmar D, 2010 Influence of drying on the content of sugars in wet processed green Arabica coffees. Food Chemistry 119 pp 500-504
- [5] Agrawal S G, Methekar R N, 2017 Mathematical model for heat and mass

- transfer during convective drying of pumpkin. *Food and Bioproducts Processing* 101 pp 68-73
- [6] Mongpraneet S, Abe T, Tsurusaki A, 2002 Accelerated drying of welsh onion by far infrared radiation under vacuum conditions. *Journal of Food Engineering* 55 pp 147-156
 - [7] Sharma G P, Verma R C, Pathare P B, 2005 Thin-layer infrared radiation drying of onion slices. *Journal of Food Engineering* 67 pp 361-366
 - [8] Adak N, Heybeli N, Ertekin C, 2017 Infrared drying of strawberry. *Food Chemistry* 219 pp 109-116
 - [9] Gautz L D, Smith V E, Bittenbender H C, 2008 Measuring Coffee Bean Moisture Content. Cooperative Extension service
 - [10] Coradi P C, Borém F H, Saath R, Marques E R, 2015 Effect of drying and storage conditions on the quality of natural and washed coffee. *Coffee Science, Lavras* 2 pp 38-47
 - [11] Sfredo M A, Finzer J R D, Limaverde J R, 2002 . Study of the drying process of Arabica coffee cherries using vibrated trays driers in the fine drink attainment. In *Proceedings of the 13th International Drying Symposium (IDS 2002)*, Beijing China. B, pp 1342–1351
 - [12] Wang J, Fang X M, Mujumdar A S, Qian J Y, Zhang Q, Yang X H, Liu Y H, Gao Z J, Xiao H W, 2017 Effect of high-humidity hot air impingement blanching (HHAIB) on drying and quality of red pepper (*Capsicum annuum* L.). *Food Chemistry* 220 pp 145-152
 - [13] Simović D Š, Šereš Z, Maravić N, Djordjević M, Djordjević M, Luković J, Tepić A, 2016 Enhancement of physicochemical properties of sugar beet fibres affected by chemical modification and vacuum drying. *Food and Bioproducts Processing* 100 pp 432-439
 - [14] Singh B, Gupta A K, 2007 Mass transfer kinetics and determination of effective diffusivity during convective dehydration of pre-osmosed carrot cubes. *Journal of Food Engineering* 79 pp 459-470
 - [15] Xiao H W, Pang C L, Wang L H, Bai J W, Yang W X, Gao Z J, 2010 Drying kinetics and quality of Monukka seedless grapes dried in an air-impingement jet dryer. *Biosystem Engineering* 105 pp 233-240.
 - [16] Mohanty A K, Misra M, Drzal L T, 2005 Natural fibers, biopolymers, and biocomposites. Taylor & Francis Group, USA
 - [17] Varadharaju N, Karunanidhi C, Kailappan R, 2001 Coffee cherry drying: a two layer model. *Drying Technology* 19 pp 709-715
 - [18] Hernández-Díaz W N, Ruiz-Lopez I I, Salgado-Cervantes M A, Rodríguez-Jimenes G C, García-Alvarado M A, 2008 Modeling heat and mass transfer during drying of green coffee beans using prolate spheroidal geometry. *Journal of Food Engineering* 86 pp 1-9
 - [19] Pérez-Alegria L R, Ciro-Vela'squez H J, 2001 Mathematical simulation of parchment coffee drying in a deep bed with airflow reversal. *Transactions of ASAE* 44 pp 1229-1234