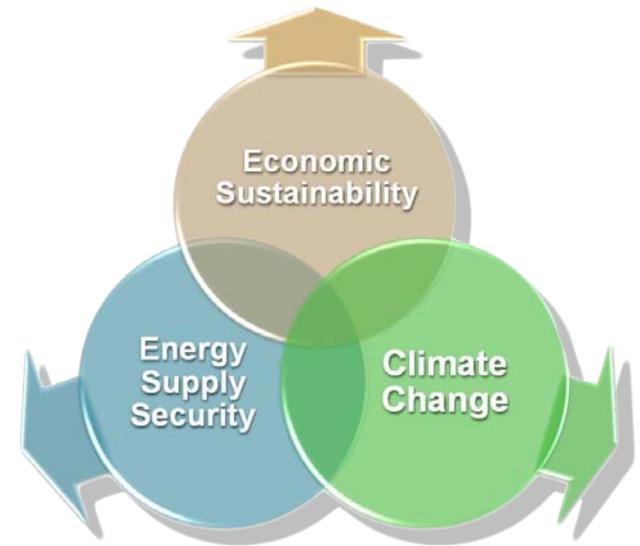


# Economic Comparison of IGCC to PC and Oxycombustion



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## National Rural Electric Cooperative Association

Generation, Fuels and Environment - Membership Advisory Group Meeting

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# Overview

- **Comparison of carbon capture technologies for coal-fired power plants**
  - Pre-combustion (IGCC), Post Combustion (PC with Amine capture), and Oxy-combustion
  - Bituminous coal
  - Today's or near term technology

# Information Source for Comparison of Carbon Capture Technologies

- **NETL's "Cost and Performance Baselines for Fossil Energy Plants"**
  - **Bituminous Coal and Natural Gas to Electricity; Rev 1 August 2007, Rev 2 to be issued this summer**
  - **Pulverized Coal (Bituminous) Oxycombustion Power Plants; Rev 2, August 2008 (Updated economic parameters for this presentation)**

# General Objectives of Baseline Studies

- **What - Determine cost and performance estimates of near-term commercial offerings**
  - Consistent design basis
  - Consistent performance and capital cost estimate methodology
  - Technologies built now and deployed in the near term
- **Why - Provide baseline costs and performance to:**
  - Compare technologies
  - Provide basis for sensitivity analyses
  - Provide basis for screening studies
  - Develop pathway studies to guide R&D for advancing technologies within the FE Program

# Design Basis

	Bituminous Baseline
Location	Mid-west
Elevation (ft)	0
Barometric Pres. (psia)	14.7
Temp (F)	59
Coal Type	Illinois #6
Coal HHV (Btu/lb)	11,666
Coal (\$/MMBtu)	\$1.64
Natural Gas (\$/MMBtu)	\$6.55
Cooling System	Evaporative

# Study Assumptions

- **Capacity Factor assumed to equal Availability**
  - IGCC capacity factor = 80% w/ no spare gasifier
  - PC, Oxycombustion, and NGCC capacity factor = 85%
- **In CO<sub>2</sub> capture cases, CO<sub>2</sub> compressed to 2200 psig, transported 50 miles, sequestered in saline formation at depth of 4,065 feet and monitored for 80 years**
- **Owners costs and CO<sub>2</sub> transport, storage and monitoring (TS&M) costs included in the levelized cost of electricity (LCOE)**



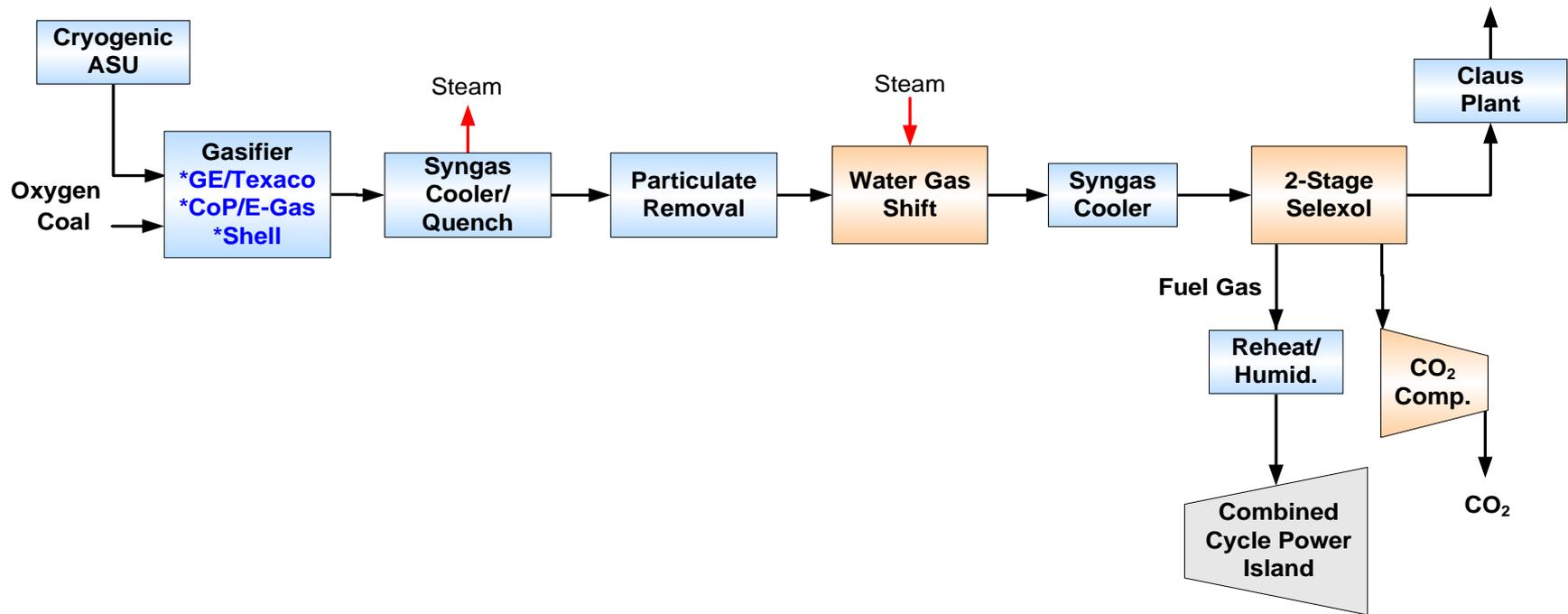
# Study Matrix

## Bituminous Coal and Natural Gas to Power

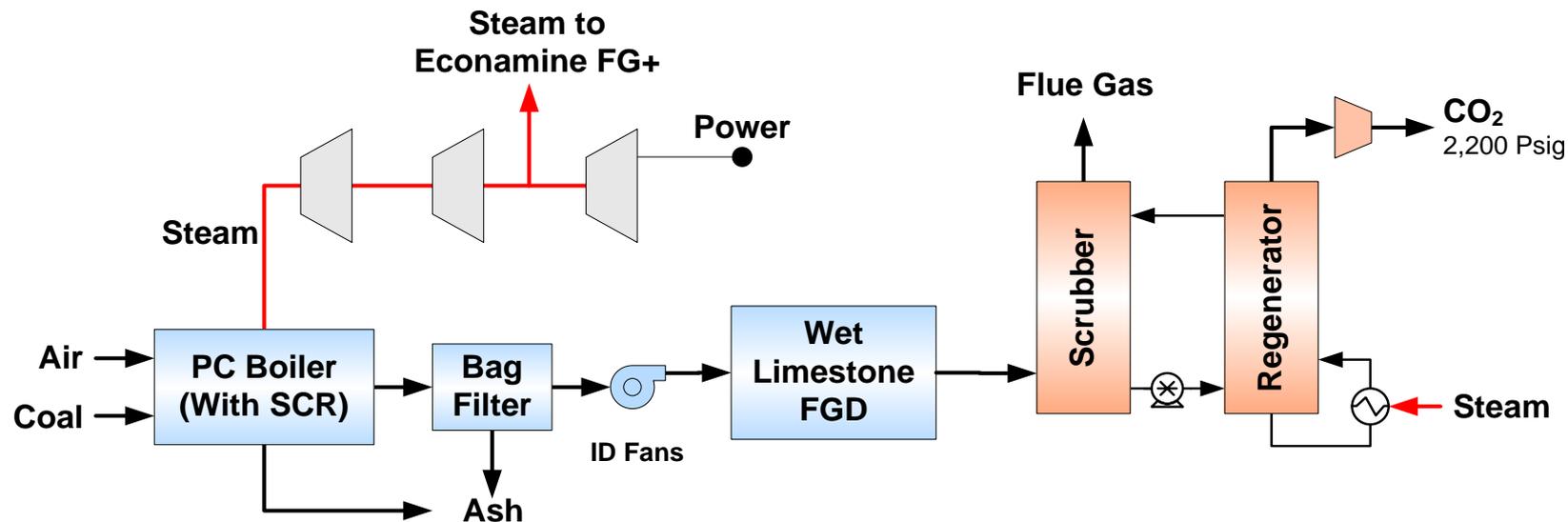
Plant Type	ST Cond. (psig/°F/°F)	GT	Gasifier/Boiler	Acid Gas Removal/ CO <sub>2</sub> Separation / Sulfur Recovery	CO <sub>2</sub> Cap
IGCC	1800/1050/1050 (non-CO <sub>2</sub> capture cases)	F Class	GEE	Selexol / - / Claus	
				Selexol / Selexol / Claus	90%
	1800/1000/1000 (CO <sub>2</sub> capture cases)		CoP E-Gas	MDEA / - / Claus	
				Selexol / Selexol / Claus	90%
	Shell		Sulfinol-M / - / Claus		
			Selexol / Selexol / Claus	90%	
PC	2400/1050/1050		Subcritical	Wet FGD / - / Gypsum	
				Wet FGD / Econamine / Gypsum	90%
	3500/1100/1100		Supercritical	Wet FGD / - / Gypsum	
				Wet FGD / Econamine / Gypsum	90%
NGCC	2400/1050/1050	F Class	HRSG		
				- / Econamine / -	90%

GEE – GE Energy  
CoP – Conoco Phillips

# IGCC Power Plant with CO<sub>2</sub> Capture



# Pulverized Coal Power Plant with CO<sub>2</sub> Capture



# Study Matrix

## Bituminous Oxycombustion

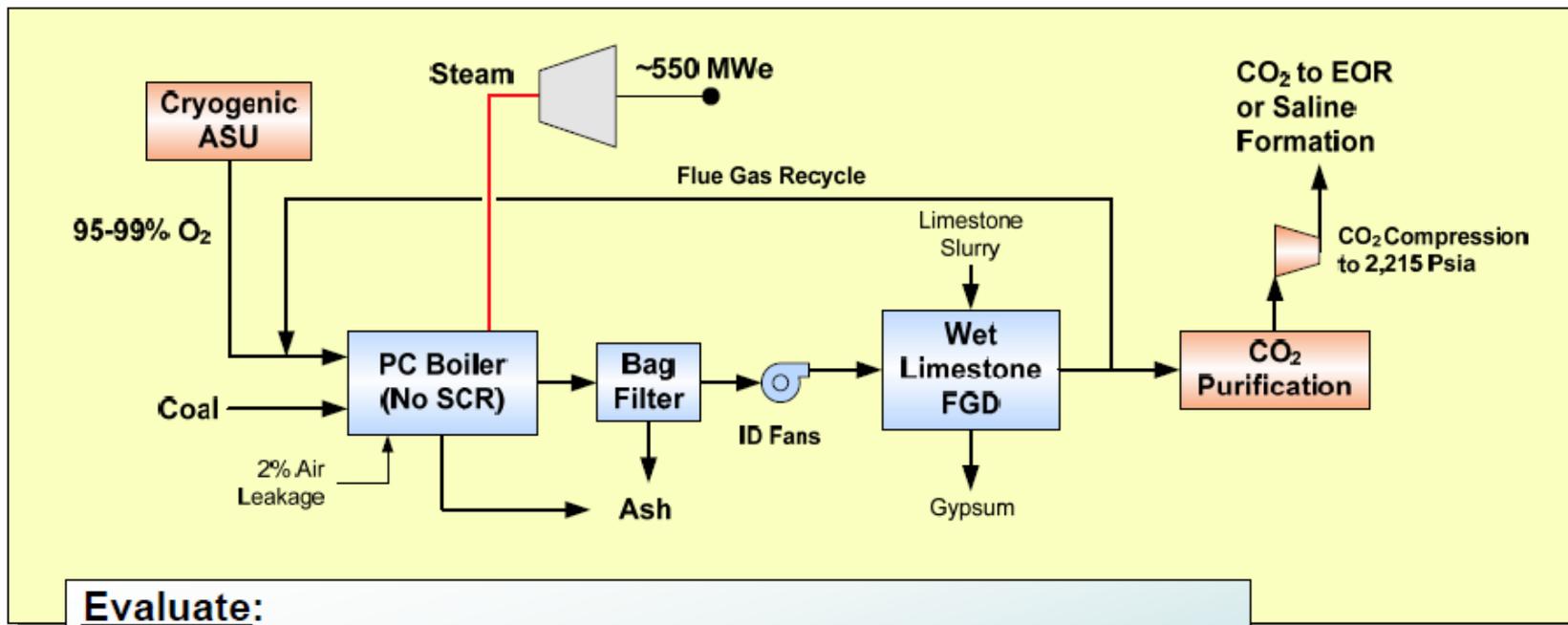
Case	Plant Design	Steam Cycle	Oxidant	Pipeline Specification
1	Air Fired	SC	Air	N/A
2	No CO <sub>2</sub> Capture	USC		N/A
3	Air Fired	SC		UR Saline Formation
4	MEA CO <sub>2</sub> Capture	USC		UR Saline Formation
5	Oxycombustion	SC	95%	UR Saline Formation
5A			99%	UR Saline Formation
5B			95%	Match 5A
5C			95%	URSF and >95% CO <sub>2</sub>
6		USC	95%	UR Saline Formation
6A			95%	URSF and >95% CO <sub>2</sub>
7		SC	~100% ITM	UR Saline Formation
7A			~100% ITM	URSF and >95% CO <sub>2</sub>

URSF: Unrestricted Saline Formation Specification

Supercritical (SC): 3,500 psig/1,100 F/1,150 F – Current state-of-art

Ultra-supercritical (USC): 4,000 psig/1,350 F/1,400 F – Advanced material program

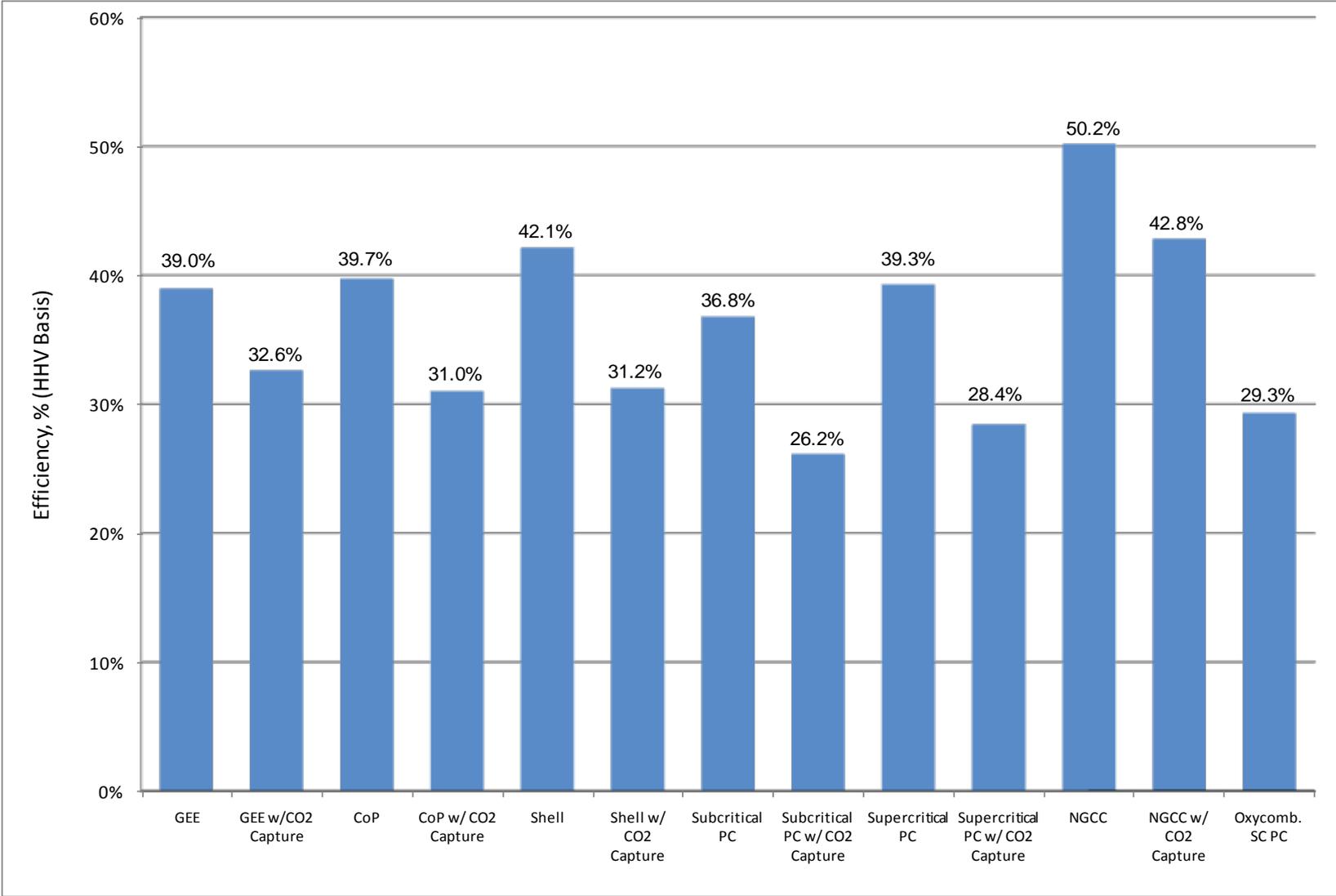
# Oxycombustion Pulverized Coal Power Plant



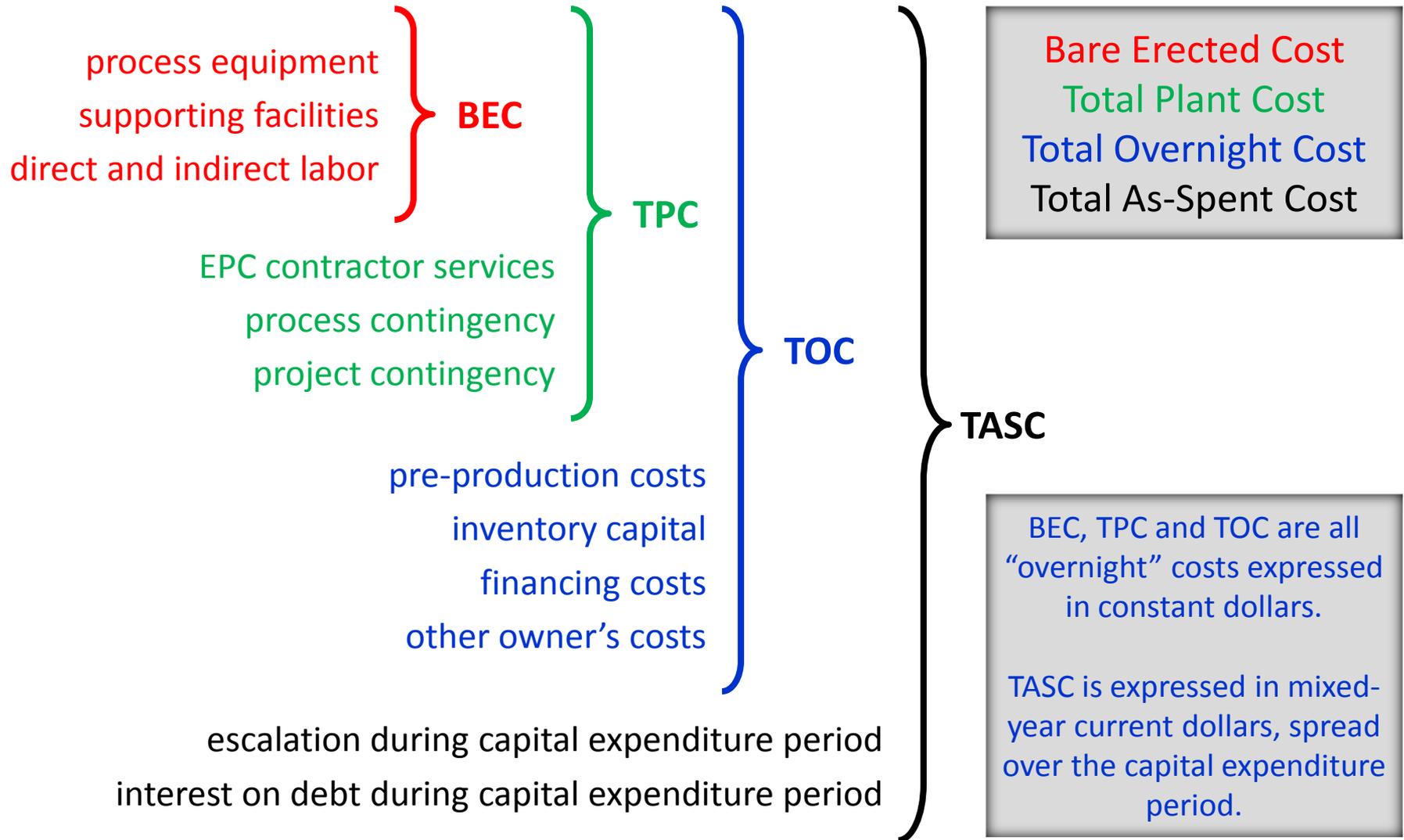
## Evaluate:

1. Impact 95 versus 99% oxygen purity has on the CO<sub>2</sub> purification/compression process
2. Minimum CO<sub>2</sub> recycle rate
3. Co-sequestration (CO<sub>2</sub>/NO<sub>x</sub>/SO<sub>x</sub>) feasibility

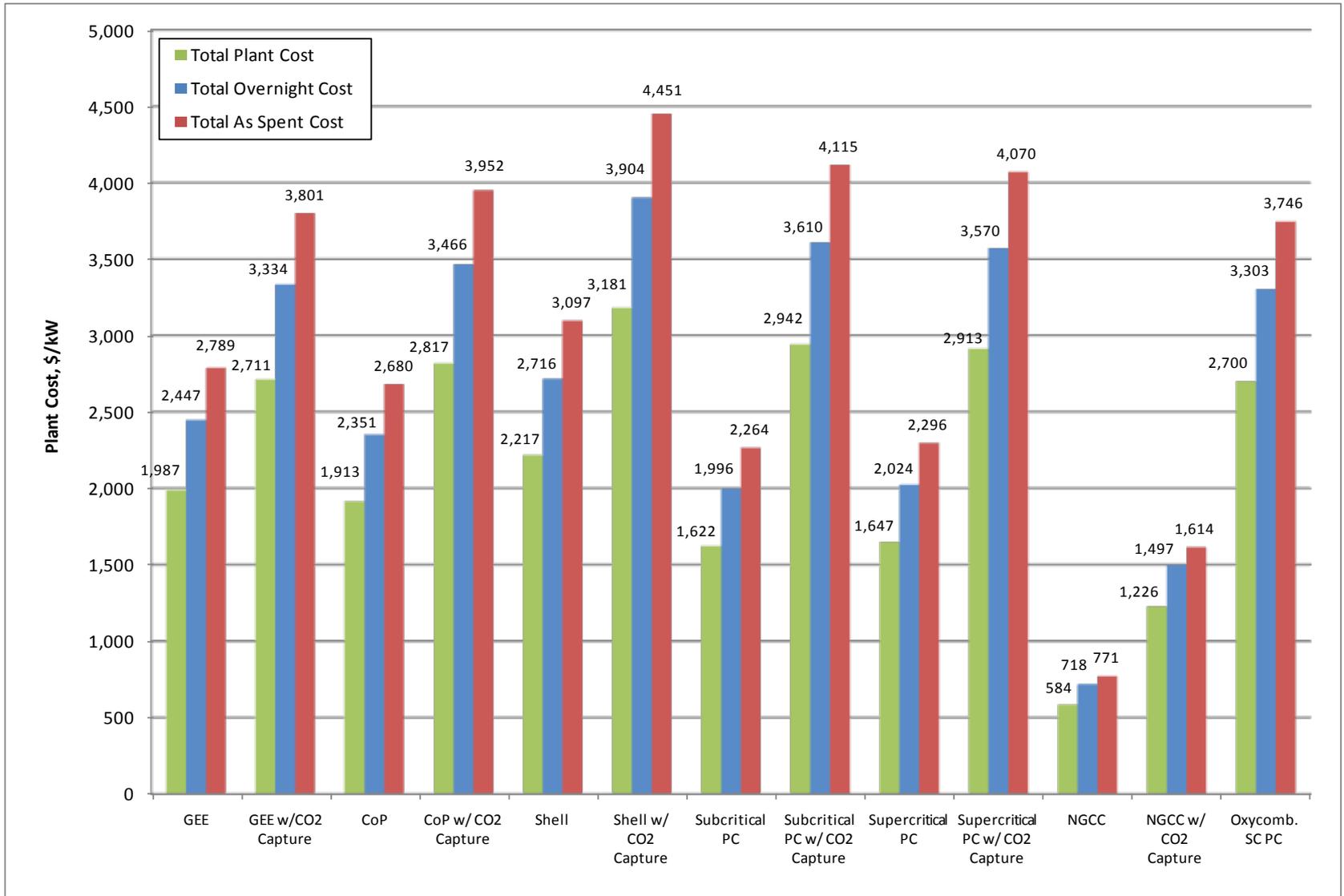
# Plant Efficiency



# Levels of Capital Cost



# Plant Costs



# Finance Structure

		Investor Owned Utility (IOU)		Independent Power Projects (IPP)	
		Low-Risk	High-Risk	Low-Risk	High-Risk
<i>Capital Structure</i>	<i>Percent Debt</i>	50%	45%	70%	60%
	<i>Percent Equity</i>	50%	55%	30%	40%
<i>Interest Rate</i>		4.5% (LIBOR plus 1%)	5.5% (LIBOR plus 2%)	6.5% (LIBOR plus 3%)	8.5% (LIBOR plus 5%)
<i>IRROE</i>		12%	12%	20%	20%
<i>Before Tax Weighted Cost of Capital</i>		8.25%	9.08%	10.55%	13.10%
<i>After Tax Weighted Cost of Capital (ATWCC)</i>		7.39%	8.13%	8.82%	11.16%

# Assumptions for DCF Analysis

## (resulting CCF is dependent on these assumptions)

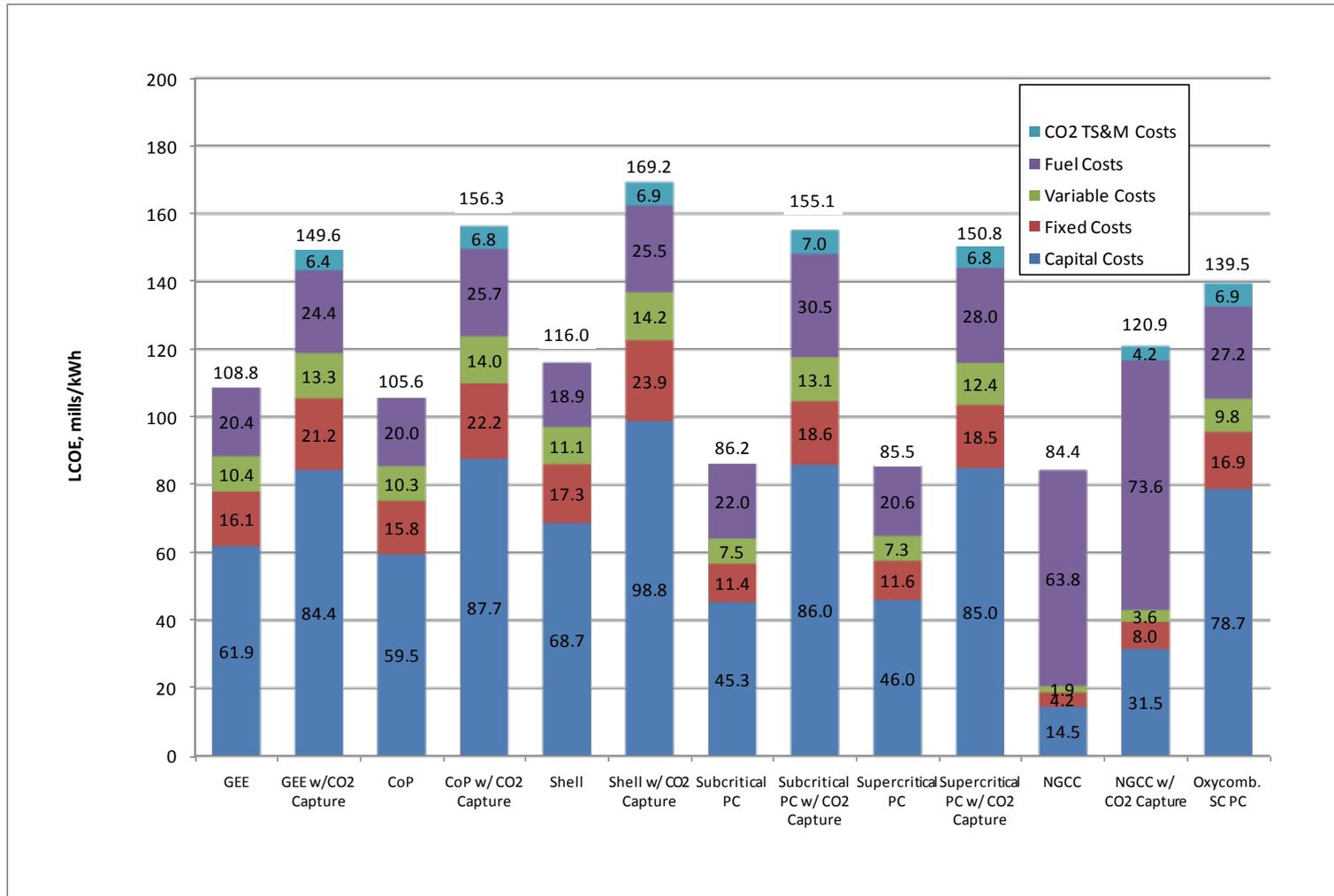
Parameter	Value
<b>TAXES</b>	
Income Tax Rate	38% (Effective 34% Federal, 6% State)
Capital Depreciation	20 years, 150% declining balance
Investment Tax Credit	0%
Tax Holiday	0 years
<b>FINANCING TERMS</b>	
Repayment Term of Debt	15 years
Grace Period on Debt Repayment	0 years
Debt Reserve Fund	None
<b>TREATMENT OF CAPITAL COSTS</b>	
Capital Cost Escalation During Construction (nominal annual rate)	3.6%
Distribution of Total Overnight Capital over the Capital Expenditure Period (before escalation)	3-Year Period: 10%, 60%, 30% 5-Year Period: 10%, 30%, 25%, 20%, 15%
Working Capital	zero for all parameters
% of Total Overnight Capital that is Depreciated	100% ( <i>this assumption introduces a very small error even if a substantial amount of TOC is actually non-depreciable</i> )
<b>INFLATION</b>	
LCOE, O&M, Fuel Escalation (nominal annual rate) Escalation rates must be the same for LCOE approximation to be valid	3.0% COE, O&M, Fuel

[1] A nominal average annual rate of 3.6% is assumed for escalation of capital costs during construction. This rate is equivalent to the nominal average annual escalation rate for process plant construction costs between 1941 and 2008 according to the *Chemical Engineering Plant Cost Index*.

[2] An average annual escalation rate of 3.0% is assumed. This rate is equivalent to the average annual escalation rate between 1947 and 2008 for the U.S. Department of Labor's Producer Price Index for Finished Goods, the so-called "headline" index of the various Producer Price Indices. (The Producer Price Index for the Electric Power Generation Industry may be more applicable, but that data does not provide a long-term historical perspective since it only dates back to December 2003.)

# Levelized Cost of Electricity

## 30-Year, Current-Dollar



Coal cost \$1.64/MMBtu, Gas cost \$6.55/MMBtu

# Highlights

## Efficiency & Capital Cost

- **Using today's technology, coal-based plants are efficient and clean**
  - PC and IGCC: 39-42%, HHV (without CCS)
  - Emissions meet or exceed current environmental requirements
  - 90% of CO<sub>2</sub> can be removed, but at significant increase in COE

Total Overnight Cost, \$/kW June-2007 (equiv. to Jan-2010)		
No CCS	NGCC	718
	Supercritical PC	2,024
	CoP IGCC	2,351
With CCS	NGCC	1,497
	Supercritical PC	3,570
	GE IGCC	3,334
	SC PC Oxycombustion	3,303

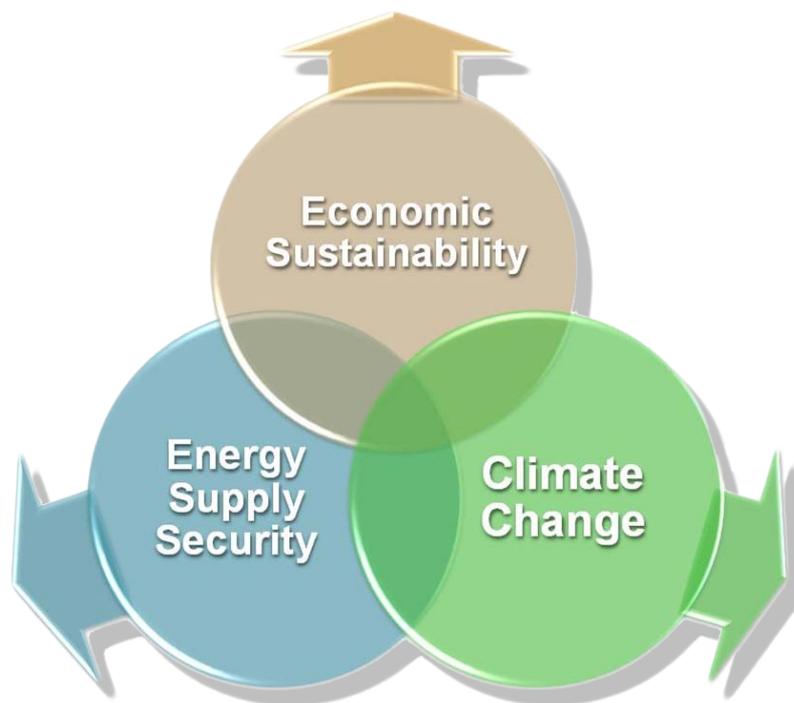
~ 2/3 to 3/4 more than  
PC w/o CCS

# Highlights

## LCOE

LCOE, \$/MWh		
No CCS	NGCC	84
	Supercritical PC	86
	CoP IGCC	106
With CCS	NGCC	121
	Supercritical PC	151
	GE IGCC	150
	SC PC Oxycombustion	140

~  $\frac{2}{3}$  to  $\frac{3}{4}$  more than  
PC w/o CCS



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